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## Fluorescence spectroscopy for wastewater monitoring

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Fluorescence spectroscopy for wastewater monitoring: A review

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1	Fluorescence spectroscopy for wastewater
2	monitoring: a review
3	
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15	
16	Abstract: Wastewater quality is usually assessed using
17	physical, chemical and microbiological tests, which are not
18	suitable for online monitoring, provide unreliable results, or use
19	hazardous chemicals. Hence, there is an urgent need to find a
20	rapid and effective method for the evaluation of water quality
21	in natural and engineered systems and for providing an early
22	warning of pollution events. Fluorescence spectroscopy has
23	been shown to be a valuable technique to characterize and
24	monitor wastewater in surface waters for tracking sources of
25	pollution, and in treatment works for process control and
26	optimization. This paper reviews the current progress in

27 applying fluorescence to assess wastewater quality. Studies 28 have shown that, in general, wastewater presents higher 29 fluorescence intensity compared to natural waters for the 30 components associated with peak T (living and dead cellular material and their exudates) and peak C (microbially 31 reprocessed organic matter). Furthermore, peak T fluorescence 32 33 is significantly reduced after the biological treatment process and peak C is almost completely removed after the chlorination 34 35 and reverse osmosis stages. Thus, simple fluorometers with appropriate wavelength selectivity, particularly for peaks T and 36 C could be used for online monitoring in wastewater treatment 37 38 works. This review also shows that care should be taken in any 39 attempt to identify wastewater pollution sources due to potential overlapping fluorophores. Correlations between 40 41 fluorescence intensity and water quality parameters such as 42 biochemical oxygen demand (BOD) and total organic carbon (TOC) have been developed and dilution of samples, typically 43 up to x10, has been shown to be useful to limit inner filter 44 effect. It has been concluded that the following research gaps 45 46 need to be filled: lack of studies on the on-line application of fluorescence spectroscopy in wastewater treatment works and 47 lack of data processing tools suitable for rapid correction and 48 49 extraction of data contained in fluorescence excitation-emission matrices (EEMs) for real-time studies. 50

52	Key words: fluorescence spectroscopy, wastewater, organic	
53	matter, monitoring	
54		
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#### 83 1 Introduction

Environmental monitoring is applied to determine the 84 85 compliance with ambient and discharge standards and to identify areas with persistent issues for timely and effective 86 87 remediation (Cahoon and Mallin 2013). Wastewater quality 88 assessment is an essential part of environmental monitoring due to the high anthropogenic impact of treated and untreated 89 discharges on water bodies (Suthar et al. 2010). There are two 90 91 important aspects of wastewater quality monitoring: the first concerns the detection of pollution events for early warning and 92 93 rapid remedial responses of water bodies, while the second aspect relates to wastewater treatment works where quality 94 95 monitoring is required for process control and compliance with regulations at the effluent discharge point (Bourgeois et al. 96 97 2001, Michael et al. 2015, Rehman et al. 2015).

The quality of wastewater is generally assessed using
physical, chemical and microbiological tests. Among these
techniques, reliance is often placed on biological oxygen
demand (BOD), chemical oxygen demand (COD) and total
organic carbon (TOC) (Bourgeois et al. 2001, Bridgeman et al.
2013). However, these global parameters depend on expensive

104	or time-consuming methods, offering only snapshots of
105	moments in time (Bourgeois et al. 2001, Chong et al. 2013,
106	Yang et al. 2015a), which makes them unsuitable for online
107	monitoring. Research conducted almost two decades ago
108	(Ahmad and Reynolds 1995, Tartakovsky et al. 1996, Reynolds
109	and Ahmad 1997, Ahmad and Reynolds 1999) has shown that
110	fluorescence spectroscopy could be used for wastewater quality
111	assessment as a tool for discharge detection in natural water
112	systems and for process control in wastewater treatment plants
113	(WwTPs). Fluorescence is the release of energy in the form of
114	light when molecules or moieties, named fluorophores, are
115	excited with a high-energy light source (Lakowicz 2006,
116	Reynolds 2014). The technique has been suggested for its
117	multiple advantages: it is fast, inexpensive, reagentless,
118	requires little sample preparation, is highly sensitive and non-
119	invasive (Reynolds 2003, Hudson et al. 2007, Cao et al. 2009,
120	Henderson et al. 2009, Hambly et al. 2010, Murphy et al. 2011,
121	Chong et al. 2013, Yang et al. 2015a). According to Reynolds
122	(2002) fluorescence monitoring could provide rapid feedback,
123	allowing dynamic, high spatial and temporal resolution studies.
124	In the past decades, more studies have proved the
125	potential of fluorescence spectroscopy as a monitoring and
126	detection tool in natural and engineered systems. This
127	technique has been used successfully to characterize organic
128	matter in seawater (Coble et al. 1990, Coble 1996, Conmy et al.

129	2004, Drozdowska 2007), freshwater (Baker 2001, McKnight
130	et al. 2001, Spencer et al. 2007b, Carstea et al. 2009) or
131	estuarine water (Huguet et al. 2009). Also, it has been used to
132	monitor riverine organic matter and diesel pollution (Downing
133	et al. 2009, Carstea et al. 2010), evaluate drinking water
134	treatment processes (Bieroza et al. 2009, Cumberland et al.
135	2012, Shutova et al. 2014) or detect pesticides (Ferretto et al.
136	2014). Fluorescence spectroscopy has been used to assess the
137	quality of raw sewage and effluents (Baker 2001, Boving et al.
138	2004, Pfeiffer et al. 2008), industrial (Santos et al. 2001,
139	Borisover et al. 2011, Li et al. 2015), or farm (Baker 2002b,
140	Old et al. 2012) discharges into natural systems. Moreover,
141	recent studies on short and long-term fluorescence monitoring
142	along the WwTPs process train have been undertaken, to
143	determine the potential of the technique for treatment processes
144	control (for example, (Murphy et al. 2011, Bridgeman et al.
145	2013, Cohen et al. 2014, Ou et al. 2014, Singh et al. 2015).
146	Although considerable work has been done so far in this field,
147	there are still issues with regard to the "matrix effects", as
148	reviewed by Henderson et al. (2009), or with fouling (Reynolds
149	2002) that must be overcome to allow application of the
150	technique in WwTPs.

Other reviews proved the potential of applying
fluorescence spectroscopy to water quality monitoring (<u>Hudson</u>
<u>et al. 2007</u>, <u>Henderson et al. 2009</u>, <u>Fellman et al. 2010</u>, <u>Ishii</u>

154 and Boyer 2012, Yang et al. 2015b). However, none of them focused only on wastewater, which requires a specific 155 156 discussion due to its complexity in composition and impact on 157 the environment. Moreover, a growing number of studies are published each year on the application of fluorescence 158 spectroscopy to wastewater quality evaluation, proving its 159 160 scientific and industrial importance. In this paper, we review the current progress in applying fluorescence spectroscopy to 161 162 assess wastewater quality. The technique's capabilities as a detection and early warning tool of pollution with treated or 163 raw wastewater from different sources are discussed. Also, its 164 165 potential for process control in WwTPs is presented.

166

#### 167 2 Fluorescence assessment of wastewater components

#### 168 2.1 Organic matter fluorescence assessment

The most common methods of recording fluorescence 169 spectra for wastewater are excitation - emission matrices 170 (EEM) and synchronous fluorescence spectra (SFS). EEMs 171 172 represent fluorescence contour maps, which comprise a series 173 of repeated emission scans recorded in a range of excitation 174 wavelengths (Coble 1996). SFS are obtained by scanning 175 simultaneously both excitation and emission monochromators 176 at a fixed wavelength interval between them (Patra and Mishra 177 2002, Reynolds 2003). For many years, since the mid-1970s, SFS were preferred as a multidimensional technique for the 178

179 analysis of complex solutions, because it provided better peak 180 resolution, compared to emission spectra, and faster recording 181 time than EEMs (Ryder 2005). However, the improvement of 182 instrumentation allowed researchers to obtain fast, highresolution EEM collection, which increased the method 183 popularity in the research community. In addition, EEMs offer 184 185 varied possibilities of data interpretation, from simple peakpicking and Fluorescence Regional Integration to the more 186 187 complex Parallel Factor Analysis (PARAFAC) and Self-188 Organizing Maps. Among these methods, peak-picking and PARAFAC are the most popular in the research community 189 190 and therefore only these two methods will be discussed in the 191 following sections.

The peak-picking method is a very simple tool to identify 192 193 their maximum intensity components based on and corresponding excitation and emission wavelength pairs (Coble 194 1996). An example of peak-picking analysis is shown in Figure 195 1 (a). According to Goldman et al. (2012), peak-picking is a 196 197 viable analysis technique and can be employed for the 198 development and use of a real-time tool and may be related to 199 custom sensors available today. However, its applicability may 200 be limited due to peak shifts, possible overlapping and 201 interferences between peaks (Yang et al. 2015b). Moreover, it 202 may lead to misleading observations by associating each peak

with a specific fluorophore, when two excitation wavelengthsare seen at fluorescent components (Fig. 1).

PARAFAC is a mathematical tri-liniar model that 205 206 deconvolutes EEMs into chemically meaningful components 207 (Fig. 1b). It separates the contribution of different fluorophores without additional assumptions about their excitation and 208 209 emission spectra (Cohen et al. 2014). A thorough description of PARAFAC method and components in wastewater is given by 210 211 Yang et al. (2015b). PARAFAC has become common practice 212 in water quality studies, over the past 10 years (Murphy et al. 213 2014). Yang et al. (2015b) proposed that PARAFAC be developed into a surrogate method for conventional water 214 215 quality parameters, treatability of organic matter (OM) and performance of treatment processes. Yu et al. (2014) suggested 216 217 that the PARAFAC tool, the EEMizer, developed by Bro and Vidal (2011), could be implemented to monitor on-line the 218 WwTPs performance. The studies of Yu et al. (2015a) implied 219 220 that PARAFAC is able to identify contamination events and 221 can be used for early warning, but the component that indicates 222 contamination must be spectrally different from the existing 223 components, without major spectral overlap, which may 224 undermine the online monitoring strategy. Similarly, Murphy et 225 al. (2011) showed that at times PARAFAC had difficulties distinguishing between components, returning hybridized 226 spectra. Also, in a comparison between chromatographic 227

228 fluorescence fingerprints and EEM-PARAFAC, Li et al. (2014) 229 showed that the latter method could not reflect the variety of 230 organic matter species with similar fluorescence, but different 231 physico-chemical properties. In addition, PARAFAC is 232 currently applied only as post-processing technique, making it unsuitable for continuous monitoring. Also, there is no 233 234 consensus regarding the optimum model in terms of sample 235 size and variability (Yu et al. 2015a).

All these techniques have been employed successfully to 236 237 analyse OM from various natural to engineered sources. A 238 thorough review on OM fluorescence is provided by Hudson et 239 al. (2007) and Fellman et al. (2010). Crude sewage is a 240 combination of domestic waste, industrial discharges, surface runoff and storm flow. Its composition varies depending on the 241 242 age and type of sewerage, time of day, weather conditions and type of incoming sewer (Ahmad and Reynolds 1995, Hudson et 243 al. 2007). Ellis (2004) showed that the general organic 244 composition of wastewater is 50 % proteins, 245 14 % 246 carbohydrates, 10 % fats and oils and trace amounts of priority 247 pollutants and surfactants, which are present in detergents, 248 soaps, shampoo and similar consumer products. More recently, 249 Huang et al. (2010) found that fibres, proteins and sugars are 250 the largest groups of OM in wastewaters, accounting for 20.64 %, 12.38 % and 10.65 %, respectively, of the total TOC. 251 According to the researchers, food related substances are the 252

253 main source of OM in wastewaters (Huang et al. 2010). Using 254 gas chromatography/mass spectrometry, Huang et al. (2010) detected 90 compounds from the groups of alkyls and aromatic 255 256 hydrocarbons, alkenes, alcohols, organic acids, ketones, 257 phenols, nitrogenous compounds, ethers, amines and esters. In addition, they found lipids, volatile fatty acids, humic acids, 258 259 DNA + RNA, tannic acids and linear alkylbenzene sulfonates. 260 Within the organic composition, there are numerous 261 overlapping fluorophores that contribute to the EEMs (Aiken 2014). Due to the difficulty of assigning specific fluorophores 262 to the peaks identified in EEMs, the fluorescence of wastewater 263 264 will be discussed as two regions based on the classification 265 provided by Li et al. (2014): the region Em < 380 nm is associated with fluorophores containing a limited number of 266 267 aromatic rings and the indole moiety of free tryptophan whilst the region > 380 nm is associated with polycyclic aromatic 268 fluorophores. 269

270 2.2 Region Em < 380 nm

Based on the peak-picking method, fluorescence in this region is represented by peak T ( $\lambda_{excitation} / \lambda_{emission} \sim 225 (\sim 280) /$  $\sim 350 \text{ nm}$ ) and peak B ( $\lambda_{excitation} / \lambda_{emission} \sim 225 (\sim 280) / \sim 305$ nm) (Fig. 1a). Peaks T and B have been observed in all studies that used the peak-picking method for EEM processing, irrespective of the wastewater source (Table SM1). These peaks have been associated with living and dead cellular

278 material and their exudates and indicate microbial activity 279 (Bridgeman et al. 2013) and material derived from anthropogenic activities (Yu et al. 2014). In PARAFAC, the 280 281 region Em < 380 nm is generally identified as components with 282 2 excitation wavelengths and 1 emission wavelength (Fig. 1b) in the same wavelength ranges as peaks T and B in the peak-283 284 picking method. These components are identified in both municipal and industrial wastewater samples; however, the 285 286 component similar to peak T is more common in wastewater 287 compared to other components in this region (Table SM2).

By examining the list of wastewater organic components 288 (Dignac et al. 2000, Huang et al. 2010, Navalon et al. 2011), 289 290 and the literature review of Aiken (2014), Stedmon and Cory (2014) and <u>Baker et al. (2014)</u>, the following components were 291 292 considered as contributors to the fluorescence in the region Em < 380 nm: phenols (for example cresols), indoles, mono and 293 polyaromatic hydrocarbons, DNA, aromatic amino acids 294 (phenylalanine, tyrosine), degradation products of lignin (lignin 295 296 phenols, vanillic acid, syringic acid etc.). These compounds are derived from domestic waste, chemical, pharmaceutical, 297 298 plastic, petrochemical, paper, leather or textile industries (del 299 Olmo et al. 1996, Pokhrel and Viraraghavan 2004, He et al. 300 2007, Tchaikovskaya et al. 2007, Tertuliani et al. 2008). The potential contributing fluorophores to this region are presented 301 302 in Table 1.

## **2.3 Region Em > 380 nm**

305	The peak-picking method classifies this region as
306	follows: Peak A ( $\lambda_{excitation} / \lambda_{emission} \sim 225 / 400$ - 500 nm), peak C
307	( $\lambda_{excitation}$ / $\lambda_{emission}$ 300 - 350 / 400 - 500 nm) and peak M
308	$(\lambda_{excitation} / \lambda_{emission} 310 - 320 / 380 - 420 nm)$ (Fig. 1a). All
309	studies done so far on wastewater OM have identified peak C
310	and most studies found peak A (Table 1); however, peak M
311	was analysed only by Yu et al. (2014) at municipal wastewater.
312	Most of the studies that employed PARAFAC for EEM
313	analysis identified a maximum of 4 components associated and
314	microbially and terrestrially derived DOM (example of two
315	components in Fig 1b). However, Ishii and Boyer (2012) have
316	identified the PARAFAC components common in natural and
317	engineered water systems: Component 1 similar to peak A with
318	excitation in the region $< 230 - 260 \text{ nm}$ and emission between
319	400 and 500 nm; Component 2 similar to peaks A + C found in
320	excitation region $< 240 - 275 (339 - 420 \text{ nm})$ and emission
321	within $434 - 520$ nm; and Component 3 similar to peak A + M
322	appearing in the excitation domain $<240 - 260 \text{ nm} (295 - 380)$
323	<i>nm</i> ) and within the $374 - 450$ <i>nm</i> emission range. According to
324	Ishii and Boyer (2012), component 1 is found mostly in OM
325	sources dominated by terrestrial precursor material. Component
326	2 was defined as reduced quinone-like and was identified in
327	OM from a wide variety of aquatic systems, including those

328 dominated by terrestrial and microbial inputs. While, component 3 fluorophores were defined as oxidised quinone-329 330 like and were similar to those with terrestrial and marine 331 precursors. Component 1 has not been reported in wastewater 332 studies, but components 2 and 3 were seen at studies made on municipal and industrial wastewater (Table SM2). Additional 333 334 components were observed in wastewater (Table SM2), but 335 they vary depending on source.

336 As shown in Table 1, there are several fluorophores that could contribute to the fluorescence of region Em > 380 nm: 337 lignins, PAHs, flavonoids, humic acids, quinones, aromatic 338 339 ketones, fluorescent whitening agents (FWAs), 340 pharmaceutically active compounds (Dignac et al. 2000, Huang et al. 2010, Aiken 2014, Baker et al. 2014, Stedmon and Cory 341 342 2014). Among these components, FWAs have been proposed as an indicator of human faecal contamination (Assaad et al. 343 2014), sewer misconnections (Chandler and Lerner 2015) and 344 presence of landfill leachates (Graham et al. 2015). FWAs are 345 346 highly soluble and poorly biodegraded, and therefore likely to 347 pass through biological treatment in WwTPs (Kramer et al. 348 1996, Poiger et al. 1998, Assaad et al. 2014). Research has shown that these components can be detected with handheld 349 350 fluorometers, which enhances the capability for in situ water monitoring (Hartel et al. 2007). Nevertheless, issues with 351 detecting FWAs in waters have been reported: the fluorescence 352

353	of other peak C fluorophores overlap the peaks of FWAs, these
354	components are easily photodegraded and DOM hinders the
355	reaction of FWAs (Kramer et al. 1996, Baker 2002a, Hartel et
356	al. 2007, Assaad et al. 2014). Solutions to overcome
357	fluorescence overlap have been proposed, yet the other issues
358	identified may limit the method's applicability in detecting
359	sewage. The following solutions have been proposed: a) to use
360	the photodegradation rate to separate FWAs from organic
361	matter (Hartel et al. (2007); b) to take into account the
362	differences in shape of the photodecay curve between FWAs
363	and natural organic matter (Cao et al. (2009)); c) to use a
364	baseline correction method to compare the differences in
365	fluorescence intensity of FWA, between the regions $320 \text{ nm}$ –
366	345 nm and 345 nm – 360 nm, with the same values for the
367	water samples (Takahashi and Kawamura (2006)); and d) to
368	apply three-way analysis of EEMs assisted by second-order
369	chemometric analyses (Gholami et al. 2015). Discrimination
370	between humic substances and FWAs was achieved by Boving
371	et al. (2004), who analysed FWAs in solution with humic acid
372	and tannic acid. FWAs were recorded at 344 nm and 422 nm
373	emission wavelength, and 250 nm excitation wavelength. The
374	authors found that the second peak of the FWAs was separated
375	from humic acids by 22 nm, but there was a 4 nm separation
376	from tannic acid. Therefore, the $\lambda_{excitation} / \lambda_{emission} = 250 / 422$

*nm* peak could be used for FWAs detection withoutinterference from humic acid.

379 As shown above, there are several fluorophores that 380 contribute to the < 380 nm > Em regions, but the list is not 381 exhaustive. More studies are needed to identify new fluorescent components and especially those specific to source with the 382 383 highest contribution to EEMs. Since the regions exhibit the 384 fluorescence of xenobiotic compounds, both can be used for 385 wastewater quality assessment. In particular, peaks T and C, 386 and the PARAFAC analogous components, are present in all wastewater studies (Tables SM1 and SM2) and may be applied 387 388 to the control of wastewater treatment processes. However, it 389 may be difficult to identify the source and type of sewage pollution in receiving water bodies. In this sense, Baker et al. 390 391 (2014) advise caution and stress the importance of using a good 392 framework combined sampling with appropriate an multivariate analysis of data for successful investigation of 393 water pollution. 394

395

## 396 3 Correlation of the fluorescence peaks with BOD, COD 397 and TOC

In order to assess the capability of fluorescence spectroscopy to act as a monitoring tool it is important to consider the correlations between fluorescence peaks and BOD, COD and TOC, commonly used indicators of OM

402 concentration in natural waters and wastewater. As reviewed by 403 Bourgeois et al. (2001) and (Jouanneau et al. 2014), BOD is a 404 desirable measurement in treatment processes, it presents 405 several disadvantages, which make this technique unsuitable 406 for on-line monitoring and process control: it is slow to yield information, it is labour intensive, toxic substances affect 407 408 bacteria, it may not reflect conditions in the treatment processes, it is insensitive and imprecise at low concentrations 409 410 and has an uncertainty of 15-20% in the results. COD takes less 411 time to give a result than BOD (2-4 h) and is not affected by 412 toxic substances. However, it is still not suitable for on-line 413 monitoring and process control due to the measuring time and 414 because it requires hazardous chemicals. Also, COD is able to discriminate between biodegradable and biologically inert 415 416 organic matter only in conjunction with BOD and not on its own (Bourgeois et al. 2001, Chen et al. 2014). TOC is very 417 fast, as triplicates can be analyzed in minutes. However, it 418 differentiate 419 cannot between biodegradable and 420 nonbiodegradable OM (Orhon et al. 2009). Also, conflicting results have been reported between different techniques of 421 measuring TOC (Bourgeois et al. 2001). 422

423 Correlation between fluorescence and standard
424 parameters revealed that peaks T and C relate to BOD, COD
425 and TOC, as reviewed by (<u>Henderson et al. 2009</u>). Slightly
426 better correlation with BOD is seen at peak T compared to peak

427 C. An exception to the above observation is found at the study 428 of Wang et al. (2007) who obtained better correlation with the 429 PARAFAC component exhibiting fluorescence in the peak C 430 region, compared to the peak T component (Table 2). They 431 observed the best correlation with BOD at the component similar to peak M (0.73). The researchers concluded that this 432 433 component contributed the most to BOD for wastewater-434 impacted lakes. Nevertheless, these results highlight the 435 complexity of the source and that there are potentially several 436 fluorophores, which display fluorescence in the peak T/C 437 regions. It also shows that both regions could contribute to 438 BOD. The difference in correlation coefficients could also be 439 determined by the low sample sizes in some studies, which might under or overestimate the relationship between 440 441 fluorescence and BOD, COD and TOC (Table 2). Another cause of the difference could be the method used for data 442 processing, as PARAFAC offers better separation of 443 444 overlapping components compared to peak-picking.

Based on the correlation between BOD and peak T fluorescence, <u>Hur and Kong (2008)</u> tried to estimate, using SFS and first derivative spectra, the concentration of BOD of samples from urban rivers affected by treated sewage. They found that the relative fluorescence intensity, at *283 nm* to *245 nm* from SFS, is the optimum estimation index as it has the best positive correlation with BOD values (0.91). It has been

452 reported that the multiple regression method, using the light 453 scattering intensity at 633 nm or turbidity, greatly enhances the 454 correlation between measured and predicted BOD values. Hur 455 and Kong (2008) also observed that filtered samples presented 456 enhanced correlation; however, Bridgeman et al. (2013) reported slightly higher correlation coefficient between BOD 457 458 and fluorescence at unfiltered samples compared to filtered with 0.45 or 0.2  $\mu$ m. These differences could be site specific 459 460 and may depend on the sizes of OM components.

As reviewed by Baker et al. (2014), the correlation 461 462 between BOD and peak T fluorescence suggests a direct link 463 with microbiological activity in this region of fluorescence, 464 although the source of peak T fluorescence is generally unknown. It was also implied that handheld instruments could 465 466 be used in the future to investigate the temporal variability of 467 BOD (Baker et al. 2014). Due to the relation with microbiological activity, peak T fluorescence was suggested as 468 indicator of the presence / absence faecal coliforms (Sorensen 469 470 et al. 2015, Sorensen et al. 2016). Pfeiffer et al. (2008) obtained 471 excellent correlation (0.90 - 0.95) with faecal coliforms on 472 samples from a wastewater polluted river and (Tedetti et al. 473 2012) found a good correlation (0.78) between the PARAFAC 474 component and Escherichia Coli + enterococci on wastewater 475 impacted coastal water samples. More recently, (Baker et al. 476 2015) obtained a log correlation of 0.74 between fluorescence

477 and E. Coli measurements. These findings are encouraging, but 478 more work should be done to explore the link between 479 fluorescent components and faecal coliforms and its potential 480 use in on-line monitoring applications. In a comparison with 481 flow cytometer measurements, peak T intensity correlated with an increase of total live and dead bacteria numbers (Bridgeman 482 483 et al. 2015). The researchers found that four bacteria isolated from a potable water tap sample showed different responses in 484 485 the fluorescence signal, although the intensity of peak T 486 fluorescence did not correlate with the bacteria counts. Nevertheless, peak T fluorescence could be used to assess the 487 488 microbiological activity in a water system.

489

#### 490 **4** Fluorescence detection of wastewater pollution

491 Fluorescence spectroscopy has shown its capabilities as a 492 real-time assessment tool for wastewater quality due to its 493 advantages and correlation with standard parameters. This technique could be very effective in detecting raw wastewater 494 495 contamination in water bodies. Also, the impact of wastewater 496 effluents on natural waters could be evaluated, since effluent 497 organic matter has different composition and characteristics 498 from naturally occurring OM (Wang et al. 2015). Therefore it 499 is important to look at the different types of wastewater for 500 particular characteristics that may facilitate identification in the receiving water bodies. 501

502

#### 503 4.1 Sources of wastewater

504 Studies published so far on fluorescence spectroscopy 505 have focused on domestic, farm and industrial wastewater, 506 which includes textile, pulp mill, coke or brewery industries. 507 More studies are needed on wastewater from oil refineries, 508 metal processing, fermentation factories, pharmaceutical 509 industry, chemical plants, meatpacking and processing etc.

510

#### 511 4.1.1 Domestic wastewater

Wastewater is the flow of water used by a community 512 513 and includes household wastes, commercial and industrial 514 waste stream flows, and stormwater (Drinan and Spellman Domestic wastewater contains the solid and liquid 515 2012). 516 discharges of humans and animals, contributing with millions 517 of bacteria, virus, and non-pathogenic and pathogenic organisms. It may also contain sanitary products, cleaners and 518 detergents, trash, garbage and any other substances that are 519 520 poured or flushed into the sewer system (Drinan and Spellman 2012). Public treatment facilities may also collect industrial 521 effluents and thus chemicals, dyes, acids, alkalies, grit or 522 523 detergents can be found in municipal wastewater (Drinan and 524 Spellman 2012). Stormwater runoff, if collected by WwTPs, 525 may bring into the system large amounts of sand, gravel, roadsalt and other grit (Drinan and Spellman 2012). 526

527 As discussed in the previous sections, there are numerous 528 compounds that may contribute to the fluorescence peaks. 529 Generally, fluorescence spectra of untreated and treated 530 domestic wastewater are characterized by intense peaks in the region Em < 380 nm, especially peak T, associated with high 531 microbial abundance, and by significantly lower intensity peaks 532 533 A and C fluorescence (Baker 2001, Hudson et al. 2007, Hur 534 and Cho 2012, Bridgeman et al. 2013). In some studies, the 535 fluorescence spectra of effluents showed a higher prevalence of 536 peaks A and C, compared to peaks T and B (Ghervase et al. 537 2010a, Riopel et al. 2014). Among peaks, T and C seem to be 538 present at most municipal wastewater samples (Tables SM1 539 and SM2) and may serve as indicators of wastewater contamination. Peak B is rarely analysed at wastewater EEMs 540 541 due to the potential interferences from scattering; however, this fraction could indicate the proximity of the measurement point 542 to the discharge point or freshness of the contamination. 543 According to Pfeiffer et al. (2008), the fluorescence of both 544 545 peak T and peak B decreases in intensity with increasing 546 distance from the release point, but peak B is completely 547 removed at longer distances, due to dilution or breakdown of 548 the organic fraction. For peak B removal, seasonal shifts should 549 also be taken into account as rainfall could contribute to 550 dilution, sunlight irradiation could cause photodegradation or increase microbial uptake during summer (Meng et al. 2013). 551

552 From the myriad of fluorophores, FWAs may display distinctive features in the EEMs for municipal wastewater 553 samples (Bridgeman et al. 2013). However, this fraction is not 554 specific to domestic wastewater, as it has been detected at 555 paper mill effluents (Baker 2002a, Ciputra et al. 2010, 556 Bassandeh et al. 2013) or landfill leachates (Graham et al. 557 558 2015). Therefore, peaks T and C seem to be the best tools of monitoring domestic wastewater quality. 559

560 In addition to fluorescence intensity increase, it has been shown that discharge of domestic sewage may change the 561 562 properties of OM from the receiving water bodies. For example, Xue et al. (2011) found that sewage effluents change 563 564 the capacity of OM to form disinfection by-products and decrease its sensitivity to UV light. Also, changes in 565 566 aromaticity and hydrophobicity of OM have been reported. These OM characteristics have been assessed after discharge, 567 using the emission wavelength of peak C. In two studies 568 undertaken by Goldman et al. (2012) on OM wastewater 569 570 effluent and by Ghervase et al. (2010b) on untreated sewage 571 discharge, it was found that the fluorescence signal of the two 572 types of samples presented lower peak C emission wavelength, 573 indicating lower aromaticity compared to natural OM. While, 574 Spencer et al. (2007a) reported higher aromaticity of the OM 575 from an estuarine sample with anthropogenic impact from domestic wastewater effluents, compared to the estuarine OM. 576

577 Goldman et al. (2012) found that the mixture of effluent and 578 river waters produce midrange values and, therefore, a potential 579 increase in aromaticity with distance from discharge could be 580 expected. In marine environments, fluorescence measurements on wastewater discharges showed great complexity of the 581 mixing properties. Petrenko et al. (1997) observed 4 layers in 582 583 the seawater column, 2 layers being affected by sewage representing the "old" and "new" plume waters and 2 layers 584 585 unaffected by effluent. According to the researchers, the release 586 of wastewater increased 2 fold to the concentration of 587 ammonium, silicate and phosphate in sewage affected plumes 588 and could stimulate the growth of phytoplankton. Baker and 589 Inverarity (2004) also found an increase in nitrate and phosphate concentrations downstream of discharge into urban 590 591 rivers.

592

#### 593 4.1.2 Animal wastewater

Animal wastes represent an important source of water 594 595 pollution, through the release of untreated wastewater or 596 surface runoff from farms. This type of wastewater produces 597 BOD values that are 1 to 3 times higher than sewage BOD 598 (Baker 2002b). Most meat processing units treat the wastewater 599 prior to release, however animal wastewater varies temporally 600 in composition, requiring continuous monitoring for effective detection and removal of pollutants. Relatively few studies 601

602	have looked at the potential of using fluorescence spectroscopy
603	to monitor the quality of animal wastewater. However, data
604	gathered so far can help define particular characteristics of
605	animal wastewater OM. The fluorescence of animal wastewater
606	is generally dominated by the region Em < 380 nm. In
607	particular, peak T fluorescence seems to be common to all
608	samples, as it has been detected at farmyard runoff (Old et al.
609	2012), pig and cattle slurry, silage liquor, sheep barn waste
610	(Baker 2002b), poultry processing unit (Ghervase et al. 2010b)
611	and cattle slaughter house (Louvet et al. 2013). The researchers
612	also observed a low peak C fluorescence relative to peak T.
613	Baker (2002b) calculated the ratio between the fluorescence
614	intensity of these two peaks and found that peak T intensity
615	was 2 to 25 times higher than that of peak C, the highest ratio
616	being obtained for silage liquor, while the lowest was seen at
617	the sheep barn waste. A similar peak T/C ratio was obtained by
618	Old et al. (2012) at farmyard runoff samples. The ratio of peaks
619	T and C fluorescence intensity shows that farm waste pollution
620	events could leave a signature in river waters (Baker 2002b)
621	and confirm the potential of using fluorescence as a low cost
622	and rapid technique for tracing animal derived pollutants (Old
623	et al. 2012). Interestingly, pig and cattle slurry presented peak
624	B fluorescence at a similar intensity to that of peak T. Peak B
625	was also detected at poultry wastewater (Ghervase et al.
626	2010b), having even higher fluorescence than that of peak T.

627 <u>Ghervase et al. (2010b)</u> suggested using the ratio of peak T and
628 peak B to detect poultry wastewater pollution in rivers.
629 However, this ratio applicability could be limited only to
630 certain types of animal wastewaters.

Cattle slaughterhouse wastewater may contain albumin 631 and haemoglobin that would contribute to the Em < 380 nm 632 633 fluorescence region (Louvet et al. 2013). Also, bovine serum albumin may contribute to the fluorescence region of Em > 380634 635 nm. Louvet et al. (2013) found another fluorescence peak that could belong to metalloporphyrins ( $\lambda_{excitation} / \lambda_{emission} = 400$  -636 440 nm / 450 - 510 nm). These components are attributed to red 637 638 blood, which is a major pollutant in slaughterhouse wastewater. 639 Again, the ratio of peaks T and C fluorescence intensity was found to be an effective indicator of biodegradation of 640 641 slaughter house wastewater (Louvet et al. 2013). Nevertheless, 642 the composition of animal derived pollutants is highly variable in time and depends on the animal species, physiological state 643 and diet (Baker 2002b, Louvet et al. 2013). Therefore, more 644 645 studies are needed to better understand the properties of OM from animal derived wastewater and set clear characteristics for 646 enhanced detection of pollution events. 647

648

#### 649 4.1.3 Industrial sources of wastewater

Industrial wastewater is primarily derived from themanufacturing and processing of chemicals, textiles, wood,

652 pulp mill or paper. The composition of effluents varies 653 depending on the raw materials used, the type of process and 654 the efficiency of material removal (Sánchez Rojas and Bosch 655 Ojeda 2005). Studies on continuous monitoring and evaluation 656 of industrial wastewater using fluorescence spectroscopy are scarce, limiting identification of particular features of 657 658 wastewater fluorescence spectra. Few studies focussed on wastewater from petrochemical, chemical and biochemical 659 660 industry (Borisover et al. 2011), brewery (Janhom et al. 2009, 661 Janhom et al. 2011), textile (Li et al. 2015), pulp mill and paper processing (Baker 2002a, Ciputra et al. 2010, Cawley et al. 662 663 Bassandeh et al. 2013) computer components 2012. 664 manufacturing (Cohen et al. 2014) and coke industry (Ou et al. 2014). In one short-term monitoring study, Yang et al. (2015a) 665 666 analysed and compared the fluorescence spectra of samples from the effluents of 57 facilities belonging to 12 industrial 667 categories (non-alcoholic drinks, electronic devices, food, 668 leather and fur, meat, organic chemicals, pulp and paper, 669 670 petrochemical, resin and plastic, steel, steam-power and textile 671 dyeing) aiming to evaluate the potential of fluorescence spectroscopy to identify wastewater sources. The researchers 672 were able to characterise and differentiate industrial effluents 673 674 cluster analysis, **EEM-PARAFAC** and FT-IR. using 675 Components from both < 380 nm > regions were observed, but no component dominated over all samples. For instance, the 676

677 peak T component presented the highest fluorescence intensity 678 at leather and fur wastewater, while peak C components 679 dominated the EEMs of food wastewater samples. Therefore, 680 Yang et al. (2015a) concluded that, without additional analyses it may be difficult to identify an industrial source with 681 fluorescence spectroscopy. However, Borisover et al. (2011) 682 683 observed a bathochromic shift of the peak T component induced by polarity and composition of local environment. 684 685 They studied samples collected from rivers impacted by 686 industrial effluents of oil refineries, petroleum and chemical and biochemical plants. The researchers recommended using 687 688 this component as fluorescent tracer of non-specific industrial 689 pollution.

690 Studies that evaluated wastewater samples from 691 particular industries have identified specific fluorophores. For 692 example, at pulp mill wastewater effluents, Cawley et al. (2012) found a component that was attributed to lignosulfonic 693 acid or to a mixture of fluorophores from the many lignin 694 695 degradation products. However, the authors highlighted that 696 this component may exhibit different emission maxima 697 depending on variations in the actual chemical moieties present in each sample. A similar component was found by Bassandeh 698 699 et al. (2013) at samples collected from the biologically treated 700 effluent of a newsprint mill and the authors attributed it to 701 ligning or chemicals involved in the paper making process.

702	Cawley et al. (2012) and Bassandeh et al. (2013) both
703	identified distinctive PARAFAC peaks for the lignin derived
704	components. However, Santos et al. (2001) observed very
705	intense peaks and additional shoulders at the peak C for
706	samples collected from rivers downstream of pulp mill effluent
707	discharge. Also, compared to samples upstream, the researchers
708	detected an additional peak at $\lambda_{excitation} / \lambda_{emission} \sim 290 / \sim 340 nm$ ,
709	which coincides with the peak T fluorescence. Baker (2002a)
710	suggested that peak T fluorescence results from the lignin and
711	sugars produced by the pulping process, which are likely to be
712	rich in aromatic proteins. This component correlated with TOC
713	(r=0.62, N=18), indicating that peak T fluorescence was a
714	significant contributor to the TOC at paper mill effluents, as
715	this correlation was not seen at the river samples. In addition to
716	lignin derived components, <u>Baker (2002a)</u> identified a peak
717	associated with FWAs, which are commonly used in papers.
718	The differences in results, found by these studies, could be
719	attributed to variations in chemical moieties or to the fact that
720	Cawley et al. (2012) and Bassandeh et al. (2013) used
721	PARAFAC for data processing to provide better separation
722	between lignin and other peak T or peak C fluorophores.
723	A distinctive feature was also detected at textile industry

refluents by <u>Li et al. (2015)</u>, who found a triple excitation response to the mission wavelength at 460 nm. They refluence this feature as specific to textile-derived

727 components, because most fluorophores in region Em > 380728 nm present dual excitation peaks at emission wavelength 729 between 400 and 500 nm. The triple excitation peaks were 730 associated with 1-amino-2-naphtol structure, based on a 731 spectral comparison with the standard solution and were suggested to be used as specific indicators in textile effluents. 732 733 Li et al. (2015) also found that for peak T fluorescence there were much more species with varying emission wavelengths, 734 735 which could relate to azo dyes as these substances emit similar 736 fluorescence in this region.

737 As shown in section 2.2 and Table 1, peak B fluorescence 738 could represent phenol-like matter, hydrocarbons or cresols as 739 found by Ou et al. (2014) at coke wastewater samples. In 740 addition to peak B and peak C fluorophores, Ou et al. (2014) 741 identified component associated a with heterocyclic 742 components and polycyclic aromatic hydrocabons (PAHs), such as fluoranthene or naphtol. PAHs were also detected by 743 Cohen et al. (2014) at samples collected from a WwTPs that 744 745 receives 50% of its crude wastewater from a computer 746 component factory. Based on spectral similarities, Cohen et al. 747 (2014) suggested that this component contains a pyrene-like 748 moiety.

While for textile, pulp mill or coke wastewater,
distinctive components have been identified, brewery
wastewater has been shown to contain only the typical peaks T,

A and C (Janhom et al. 2009, Janhom et al. 2011), generated by the cleaning and washing of raw materials. They also showed that the fluorescence of brewery wastewater samples belonged primarily to hydrophobic acids and hydrophilic bases OM fractions.

757

#### 758 4.2 Wastewater tracking in aquatic systems

Discrimination between sources using fluorescence 759 760 spectroscopy may be challenging since domestic wastewater can be mixed with industrial effluents and agricultural runoffs 761 762 (Andersen et al. 2014). Industrial wastewater could also contain 763 domestic discharges from the toilets and kitchens within 764 factories (Reynolds and Ahmad 1995). Moreover, organic pollutants like optical brighteners, PAHs or lignins have 765 766 widespread application and thus can be found in any type of wastewater. 767

In particular for industrial wastewater it may be more 768 difficult to separate sources due to the varied composition of 769 770 the solution. The release of industrial effluents in water bodies 771 may lead to the production of fluorescent fractions formed of a mixture of proteinaceous and non-proteinaceous substances, 772 773 which generates a bathchromic shift in the typical peak T 774 fluorescence emission wavelength. According to Borisover et al. (2011) this component may be used as a tracer of non-775 776 specific industrial pollution. However, various industrial

777 wastewaters produce high quantities of particular fluorophores 778 like PAHs or heterocyclic compounds, differentiating them from domestic wastewater. As shown by Cohen et al. (2014) 779 780 the pyrene-like components separated the wastewater with 50% 781 industrial input from the more domestic wastewater sources. Also, the devices, developed by Tedetti et al. (2013) and Puiu 782 783 et al. (2015), that separate PAHs from other peak T fluorophores, hold great promise in detecting both domestic 784 and industrial sources of pollution. Additionally, chemical 785 separation can be undertaken by the use of time resolved laser 786 787 induced fluorescence, which is capable to identify components 788 based on their lifetimes. PAHs have a relatively long 789 fluorescence lifetimes and great quantum efficiency, which help at distinguishing PAHs from the OM background 790 791 (McGowin 2005).

However, the question remains as to how to differentiate 792 793 between wastewater from domestic, animal farms and industry sources, which are characterized by intense Em < 380 nm 794 795 region. Domestic wastewater contains PAHs (Huang et al. 796 2010), which have a distinctive fluorescence signal; however, 797 the quantities could be too low in comparison to other 798 fluorophores and therefore the fluorescence of PAHs could be 799 exceeded by other compounds.

800 Component distinction can also be undertaken by801 PARAFAC, which may be able to separate overlapping

802 components or identify specific pollutant indicators (Cohen et 803 al. 2014, Yang et al. 2015b). However, in case of low 804 concentrated pollutants, such as detergents, peak picking has 805 been shown to be more effective than PARAFAC (Mostofa et al. 2010). Therefore, a combination of these techniques could 806 better provide a thorough view of the sample composition and 807 808 OM interaction with pollutants. Fluorescence spectroscopy could be used as an early warning system in case of accidental 809 810 pollution and could serve as a quick method in initial 811 identification of the source of wastewater, before more complex and expensive analyses would be employed. 812

813

## 814 5 Control of wastewater treatment processes using 815 fluorescence spectroscopy

Two decades ago, the studies of Reynolds and Ahmad 816 (1995) and Tartakovsky et al. (1996) demonstrated the potential 817 of using fluorescence spectroscopy for both off- and on-line 818 monitoring in wastewater treatment. Recent studies have 819 820 suggested that this technique could be applied to process control and optimization (Bridgeman et al. 2013). With 821 822 increasingly stringent regulation it will be more difficult to control treatment efficiency with current techniques, (BOD, 823 824 COD and TOC), which are expensive, time-consuming and unreliable (Bridgeman et al. 2013, Rehman et al. 2015). More 825 pressure is put on WwTPs when other environmental 826

827 implications, such as energy and chemical consumption or 828 greenhouse gases emissions are considered (Wang et al. 2015). 829 Fluorescence spectroscopy offers a robust technique available 830 for a rapid and low cost estimation of effluent quality. 831 However, studies on fluorescence monitoring of WwTPs processes are scarce and only one long-term study at 5 832 833 municipal WwTPs has been achieved (Cohen et al. 2014). Also, only one real-time monitoring study has been published 834 835 on two recycled water systems (Singh et al. 2015). According 836 to Reynolds (2002), WwTPs are hostile environments, making 837 continuous and dynamic monitoring of wastewater quality 838 difficult due to problems associated with fouling. This would 839 require regular cleaning, which is time consuming. In addition, the fluorescence signal could be affected by pH, IFE, 840 841 temperature and metal ions, requiring subsequent corrections. However, recent development of devices, already on market, 842 show great promise since they convert the on-line peak T 843 fluorescence signal into BOD equivalent values, using an 844 845 internal calibration factor or a multispectral approach 846 (ChelseaInstruments 2015, ModernWater 2015, 847 ZAPSTechnologies 2015). This type of instruments could provide an immediate estimation of changes in wastewater 848 849 quality, displaying capabilities of effective process control.

850

#### 851 **5.1 Monitoring of fluorescent OM**

852 Fluorescence real-time monitoring of wastewater quality 853 is difficult to implement due to multiple potential factors that 854 may interfere with the signal. The only real-time monitoring study was undertaken by (Galinha et al. 2011a) on a pilot scale 855 856 membrane bioreactor system to predict performance 857 parameters. EEMs were recorded for 10 months and processed with multivariate techniques. They concluded that although 858 859 fluorescence was able to describe total COD for influent and 860 effluent, it could not accurately predict other performance 861 parameters and hence, fluorescence cannot totally replace 862 conventional monitoring of membrane bioreactors (Galinha et 863 al. 2011a). Nevertheless, real-time monitoring studies at fullscale WwTPs should be undertaken in order to assess the 864 865 feasibility of the method and the issues that can arise from its implementation. The studies done on the monitoring of surface 866 waters identified major issues and offered solutions, which 867 could be used to build a strategy for wastewater on-line 868 869 monitoring. The issues reported so far include: biofilm 870 formation, temperature, turbidity, inner filter effect, calibration procedure, presence of quenching elements. Most of these 871 872 problems are thoroughly reviewed by Henderson et al. (2009). 873 Therefore, only the recent studies will be discussed. Before the study of Carstea et al. (2010) no long-term, real-time 874 monitoring experiments were done due to fouling issues. 875

876 Carstea et al. (2010) showed that over a period of 11 days of 877 continuous EEM recordings on an urban river, biofilm 878 formation on the water extraction system had no influence on 879 the fluorescence signal. However, higher rates of biofilm 880 formation are expected in wastewater, compared to surface water, due to the large quantities of extracellular polymeric 881 882 substances that enhance cell adhesion to solid surfaces 883 (Tsuneda et al. 2003).

884 Regarding temperature, Chen et al. (2015) tested a newly 885 developed, portable laser induced fluorescence system, for its monitoring capabilities, on estuarine water and found that 886 887 changes affected the fluorescence temperature results. 888 Yamashita et al. (2015) and Khamis et al. (2015) also reported the impact of temperature on the fluorescence of OM, at 889 890 monitoring studies on open ocean and urban river. Carstea et al. 891 (2014) have shown that peak T fluorescence suffers more 892 thermal quenching at samples with higher urban anthropogenic 893 impact compared to natural sources. Therefore, temperature 894 could have a major impact on OM fluorescence from 895 wastewater. However, a temperature-compensating tool has 896 been proposed and tested by Watras et al. (2011). Khamis et al. 897 (2015) also proposed a compensating tool for turbidity, which 898 can have a great impact on the fluorescence signal when large 899 particles are present. It is yet to be tested on wastewater 900 samples.

901	The inner filter effect (IFE) is another major issue at
902	wastewater samples. The IFE is the apparent decrease in the
903	emitted fluorescence intensity or a distortion of the band-shape
904	resulting from the absorption of the excited and emitted
905	radiation (Henderson et al. 2009). Kothawala et al. (2013)
906	found that the best correction tool for the IFE is the absorbance
907	based approach, proposed by Lakowicz (2006). This approach
908	can be applied to samples with absorbance values of up to 1.5
909	cm <sup>-1</sup> ; at samples above this value a dilution of 2x is
910	recommended (Kothawala et al. 2013). However, the study of
911	Kothawala et al. (2013) was undertaken on lake water samples
912	and it is not known if these rules apply to wastewater
913	monitoring. As seen in Tables SM1 and SM2, for the
914	wastewater evaluation studies there are two preferred methods
915	for reducing the IFE: dilution and post-measurement
916	mathematical correction. A dilution factor of 10 was used in
917	some studies, while in others the samples were diluted until a
918	specific absorbance value was achieved. Most studies report the
919	absorbance values at wavelengths within the excitation region
920	of peak T. In specific studies, no dilution was used to analyse
921	samples as this procedure in not applied to on-line
922	measurements (for example, (Baker and Inverarity 2004,
923	Louvet et al. 2013, Li et al. 2014). However, IFE could be a
924	serious issue for monitoring studies, as this factor might lead to
925	an underestimation of the degree of pollution and poor

prediction of BOD, COD or TOC. In this case, dilutions to a
certain absorbance value (< 0.05 cm<sup>-1</sup>, as used in most studies,
Tables SM1 and SM2) or post-measurement IFE correction are
recommended. However, other solutions should be found to
counteract IFE, as the use of UV absorbance measurements, in
addition to fluorescence spectroscopy, reduces the practicality
of the method for on-line monitoring.

addition. 933 In Yamashita et al. (2015) proposed 934 fluorescence sensors calibration for dark blanks and/or 935 sensitivity. Solutions of L-tryptophan (Tedetti et al. 2013, 936 Khamis et al. 2015, Sorensen et al. 2015) and quinine sulphate 937 (Conmy et al. 2004, Chen et al. 2015, Yamashita et al. 2015) 938 are generally used as calibration standards for the two fluorescence regions. However, Khamis et al. (2015) mention 939 940 that uncalibrated systems may be used if qualitative data is 941 needed.

Finally regarding the presence of quenching components, 942 Wang et al. (2014) have proved that the presence of humic-like 943 944 components could reduce the fluorescence of peak T in effluent 945 organic matter. However, even more complex interactions 946 could occur in wastewater samples. Galinha et al. (2011b) 947 found that the addition of bovine serum albumin to domestic 948 wastewater samples determined a decrease with 31-58 % of peak T fluorescence. They concluded that the complexity of 949 interferences on the fluorescence signal might not allow the 950

951 simple and direct quantitative measurement of specific 952 fluorophores in complex biological systems, such as 953 wastewater. Also, in a study aiming to identify the contribution 954 of extracellular polymeric substances to dye removal, Wei et al. 955 (2015) showed that methylene blue has a substantial quenching 956 effect on peaks T and C fluorescence. Several studies (Baker 2001, 2002b, Spencer et al. 2007a, Xue et al. 2011) have 957 stressed that, although peak T is dominant in fluorescence 958 959 spectra of wastewater, it is very likely that sewage generates 960 high quantities of other components, which may significantly 961 impact peak T fluorescence. Nevertheless, a study conducted 962 by Zhou et al. (2015) on a drinking water source contaminated 963 with domestic wastewater, showed that all peaks were sensitive to pollutant concentration, especially peak T, which could be 964 965 used as an early warning tool for contamination. Moreover, 966 Goldman et al. (2012) were able to predict the percentage of municipal wastewater in rivers with 80 % confidence, by the 967 use of multivariate linear regression and the fluorescence of 968 969 both peak T and peak C. They recommended applying this 970 model to develop in situ instruments, inform monitoring 971 progress and develop additional water quality indicators. Also, 972 Hur and Cho (2012) recommended the use of absorbance 973 values at 220 nm and 254 nm, and PARAFAC components similar to peaks T and C, as estimation indices for BOD and 974 COD in wastewater effluent contaminated river. 975

976

## 977 5.2 Monitoring of treatment processes with fluorescence 978 spectroscopy

979 Typical wastewater treatment begins with a series of 980 physical operations (pre-treatment and primary treatment), such 981 as screening and sedimentation to remove the floating and 982 settleable solids. These steps are followed by biological 983 processes, which are used to convert the finely divided and 984 dissolved OM from wastewater into flocculant settleable 985 biological solids (Tchobanoglous et al. 1991). Biological processes include the suspended growth activated sludge 986 987 process, anaerobic/anoxic/oxic, sequencing batch reactor, 988 membrane reactor, trickling filter, etc. Activated sludge is the most common process, involving the entrainment of air for 989 990 microbial degradation of OM. In the final steps of the 991 biological treatment, the sludge flocs are separated from the 992 treated effluent, through sedimentation, before the effluent is discharged to a water body. In some WwTPs, additional 993 994 treatment processes (tertiary and quaternary), such as filtration, 995 chlorination, UV disinfection or reverse osmosis are adopted 996 after the biological treatment and subsequent sedimentation 997 (Yang et al. 2015b).

998 Few studies have focused, so far, on wastewater quality
999 monitoring in treatment works, using fluorescence
1000 spectroscopy, to understand the behavior of OM along the

1001	process train, the removal of components and the potential of
1002	applying fluorescence as a control tool. Among these studies,
1003	some looked into the treatment of specific domestic/industrial
1004	wastewater (Janhom et al. 2009, Janhom et al. 2011, Zhu et al.
1005	2011, Yu et al. 2013), the removal and behavior of refractory
1006	OM in treatment works (Hur et al. 2011), characterization of
1007	reverse osmosis permeates (Singh et al. 2009, Singh et al. 2012,
1008	2015) or compared fluorescence EEM-PARAFAC and
1009	HPLC/HPSEC techniques (Li et al. 2014). Fluorescence
1010	monitoring of wastewater quality was performed at time frames
1011	spanning from 1 month to 20 months, by collecting samples
1012	from the inlet and outlet (Reynolds 2002, Riopel et al. 2014) or
1013	along different treatment steps (Singh et al. 2009, Hambly et al.
1014	2010, Murphy et al. 2011, Singh et al. 2012, Bridgeman et al.
1015	2013, Cohen et al. 2014, Ou et al. 2014, Singh et al. 2015). The
1016	longest monitoring study was undertaken by Cohen et al.
1017	(2014), who analyzed the wastewater quality from municipal
1018	treatment plants during 20 months. <u>ENREF 23 ENREF 126</u> Most
1019	of the monitoring studies involved WwTPs that employed
1020	activated sludge, as biological treatment process. Nevertheless,
1021	a few long-term and short-term monitoring studies have proven
1022	the capacity of fluorescence to evaluate the treatment
1023	performance in plants that used trickling filters (Bridgeman et
1024	al. 2013), anaerobic/anoxic/oxic (Yu et al. 2014), a novel
1025	anoxic/aerobic/aerobic system (Ou et al. 2014) or other

1026 advanced biological treatments, such as phase isolated ditches, 1027 bio-Denipho process, sequencing batch reactors (Hur et al. 2011). Hur et al. (2011) found no difference in OM 1028 1029 characteristics fluorescence between conventional and 1030 advanced biological treatment, while Bridgeman et al. (2013) were able to show, using fluorescence spectroscopy, that 1031 1032 activated sludge was more effective than trickling filters, in removing the organic fraction. Variations in the fluorescence 1033 1034 signal among WwTPs were also observed by Murphy et al. 1035 (2011). Nevertheless, the general consensus is that the behavior 1036 of certain fluorescence peaks can be followed along treatment 1037 plants to test performance. Cohen et al. (2014) suggested using 1038 both peak T and peak C components as indicators of total microbial in wastewater. 1039 activity Therefore, varied instrumentation available on market or under development 1040 (Bridgeman et al. 2015) that measure both components may be 1041 1042 applied to monitor treatment efficiency.

1043

## 1044 5.3 Removal of fluorescence components along the 1045 treatment plant processes

1046 Studies have shown that the OM, especially in the region 1047 Em < 380 nm is significantly removed after the biological 1048 treatment process (Fig. 2). This is to be expected since the 1049 biological treatment removes biodegradable material (<u>Cohen et</u> 1050 <u>al. 2014</u>). <u>Riopel et al. (2014)</u> reported a 60% reduction in the

1051	peak T fluorescence. Within the Em < 380 nm region, peak T
1052	component experiences a different degree of removal compared
1053	to peak B component. Yu et al. (2013) found that peak T
1054	fluorescence decreases with 60 % in the anaerobic/anoxic zone,
1055	almost 40 % in the oxic zone and 5% in the final clarification
1056	process, whilst peak B fluorescence is reduced by 55%, almost
1057	100% and 0% in the respective zones. Yu et al. (2014) reported
1058	slightly higher reduction percentages for peak B in the
1059	anaerobic/anoxic/oxic system. They also observed that peak T
1060	remained relatively consistent in the treatment process (41 - 48
1061	%), but peak B decreased dramatically (33 - 7 %). However,
1062	Murphy et al. (2011) and Janhom et al. (2009) found a poor
1063	removal of peak B fluorescence. Janhom et al. (2009) stated
1064	that peak B substances are not considered refractory and
1065	suggested that these substances could be related to some
1066	humic-bound proteinaceous constituents, which may be
1067	biologically resistant. Nevertheless, Cohen et al. (2014) advises
1068	caution when comparing the sensitivity of fluorescent
1069	components to wastewater treatment due to possible multiple
1070	differences in the treatment system. In addition to the
1071	biological treatment, Cohen et al. (2014) found that soil-aquifer
1072	treatment causes a further significant decrease in the
1073	concentration of the OM fluorescing in the $\text{Em} < 380 \text{ nm}$
1074	region. Murphy et al. (2011) and Hambly et al. (2010) also
1075	observed that chlorination generated a high removal rate of the

1076 peak T fraction at recycled treatment plants.

1077 Compared to peaks T and B components, peaks A and C 1078 are removed to a lower extent in the first stages of the treatment 1079 works (Fig. 2). Riopel et al. (2014) reported a reduction in the 1080 peak C component of 28 % and an increase in peak M with 4 % 1081 from influent to effluent. Cohen et al. (2014) found that one 1082 component in the Em > 380 nm region, sensitive to microbial activity, was removed, while other two components could not 1083 1084 be removed by the biological treatment. Yu et al. (2013) 1085 observed a reduction in peak C - like component below 10 %. 1086 Later, Yu et al. (2014) showed that one component in the 1087 region Em > 380 nm increases from 6 % in the primary 1088 treatment to 19 % after the biological treatment. An increase in the fluorescence of this component was observed by Ou et al. 1089 1090 (2014) in anoxic and aerobic treatments. Poor degradation of 1091 these components was also reported by Janhom et al. (2011) at 1092 an activated sludge treatment process. Yu et al. (2015b) found that with increasing retention times at sequencing batch reactor 1093 1094 the peak C components increase in the soluble microbial 1095 products. These products are generated by substrate utilization 1096 or biomass decay and cell lysis, and are regarded as 1097 autochthonous matter. Cohen et al. (2014) and Riopel et al. 1098 (2014) suggest that these fluorescent components are either 1099 potentially produced during the process or are recalcitrant to 1100 decomposition. Riopel et al. (2014) mention that large

1101 molecules degrade into smaller molecules that have a fulvic-1102 like behavior, based on the polyphenol postulate of humic 1103 susbtances formation. They explain that due to the high 1104 microbial activity in WwTPs, the secreted exocellular enzymes 1105 will oxidize the polyphenols into quinones. The quinones will 1106 agglomerate with metabolites like amino acids or peptides, 1107 leading to the formation of humic polymers, which could be fulvic acids because they are smaller in size. Another 1108 1109 explanation for the poor removal of these components is 1110 provided by Hur et al. (2011) who studied the fate of refractory 1111 OM in WwTPs. Refractory OM is not easily removed by the 1112 biological treatment process due to its recalcitrant nature. 1113 Moreover, Hur et al. (2011) showed that in most WwTPs, the percentage distribution of refractory OM increases in the 1114 1115 effluents.

Tertiary and quaternary treatment stages are responsible 1116 for removing most of the fraction that fluoresces in the region 1117 Em > 380 nm (Fig. 2). Hambly et al. (2010) observed that 1118 1119 chlorination generated a higher reduction in peak C compared to previous treatment steps. Singh et al. (2012) found a 1120 minimum of 97 % removal of peak C fluorophores after the 1121 1122 reverse osmosis process. Murphy et al. (2011) also reported 1123 almost complete removal of components following reverse 1124 osmosis treatment step.

Removal of fluorescent compounds, like FWAs and 1125 1126 PAHs, was also analysed. Bridgeman et al. (2013) found 1127 FWAs only in crude wastewater and not after other treatment 1128 steps, concluding that this fluorescent fraction associates with 1129 particulate matter, which is removed by the primary treatment 1130 stage. In addition, Tavares et al. (2008) stated that subsequent 1131 disinfection processes may further remove FWAs from wastewater. According to Hayashi et al. (2002), up to 80 % of 1132 1133 FWAs are removed after the biological treatment, and thus 1134 these compounds could be used as molecular markers of less 1135 effective treatment processes. Ou et al. (2014) found that, for 1136 coke wastewater, the novel anoxic/aerobic/aerobic system 1137 successfully removed PAHs. While, Cohen et al. (2014) observed no reduction in the pyrene-like component along the 1138 1139 treatment steps.

In most monitoring studies, other changes in the 1140 fluorescence spectra with regard to peak shape and position 1141 were observed. However, the findings regarding peak position 1142 1143 are not consistent across studies, potentially due to differences 1144 in the treatment process or source of wastewater. For example, 1145 Zhu et al. (2011) observed that peak C presented a blue shift of 1146 5 nm for the excitation wavelength and of 21 nm for the 1147 emission wavelength, from influent to effluent, at membrane 1148 bioreactor treated supermarket wastewater. Hur et al. (2011) reported a 20 nm excitation wavelength red shift between 1149

1150 influent and effluent, at refractory OM from municipal 1151 wastewater. Yet, Riopel et al. (2014), using PARAFAC, found 1152 no change in the peak C position or shape between sample 1153 locations. Riopel et al. (2014) observed that the PARAFAC 1154 component similar to peak T was elongated to longer wavelengths at influent samples compared to effluent. They 1155 1156 attributed this elongation to the free or bound nature of the components. In the study of Zhu et al. (2011), peak T 1157 1158 fluorescence displayed a red shift of 5 nm in the emission 1159 wavelength, from influent to effluent (Zhu et al. 2011). 1160 According to Zhu et al. (2011), the red shift is associated with 1161 the presence of carbonyl containing substances, hydroxyl, 1162 alkoxyl, amino groups and carboxyl constituents, while a blue shift is linked to a decomposition of condensed aromatic 1163 moieties and the break-up of the large molecules into small 1164 1165 molecules.

1166

## 1167 5.4 Fluorescence control and optimisation of treatment1168 processes

Increasingly stringent regulation has put major pressure
on water utilities to find new technologies and implement
control concepts that would improve the overall performance of
WwTPs (<u>Rehman et al. 2015</u>). As discussed in previous
sections, fluorescence spectroscopy has the potential to be used
as a highly effective monitoring technique of treatment quality.

1175 This could be achieved through the use of peak T fluorescence, 1176 which could replace the out-dated and inaccurate BOD 1177 (Bridgeman et al. 2013). Consequently, fluorescence 1178 spectroscopy could provide the WwTPs with the optimum tool 1179 for real-time control and remediation of plant performance 1180 failures (Chong et al. 2013).

1181 Additionally, Bridgeman et al. (2013) and Ahmad and Reynolds (1995) suggested that fluorescence could improve the 1182 1183 process control in activated sludge process. The bacteria and 1184 microorganisms that form the activated sludge are fed with 1185 wastewater containing organic waste. In order to sustain the 1186 biological activities into the activated sludge process for BOD 1187 reduction, air is pumped into the tanks to provide sufficient quantities of dissolved oxygen. Aeration is one of the most 1188 1189 energy intensive operations from the WwTPs, almost 65 % of energy being consumed for the activated sludge process 1190 1191 (Rehman et al. 2015). Water utilities often over aerate to ensure meeting discharge regulations (Bridgeman et al. 2013). 1192 1193 It is estimated that, by monitoring OM in WwTPs, 40 % of the 1194 energy costs could be saved (Ahmad and Reynolds 1995). 1195 Thus, fluorescence may be used to optimize process control in 1196 treatment works and eliminate the unnecessary costs associated 1197 with overtreatment (Bridgeman et al. 2013).

1198 Promising results regarding online monitoring and 1199 process control were obtained by <u>Singh et al. (2015)</u>, who

1200 published the first real-time study on two municipal recycled 1201 treatment plants. The researchers used a peak C sensor to prove 1202 the robustness of the technique in detecting reverse osmosis 1203 membrane fouling and integrity. They showed that the sensor 1204 was sufficiently sensitive to detect subtle differences between 1205 membrane permeates and identify underperformance issues. 1206 Also, no indication of fouling on probe and no deviation of probe performance were observed, during the experimental 1207 1208 period. This study demonstrated the potential of using 1209 fluorescence for treatment process assessment and control.

1210

#### 1211 6 Conclusions and future considerations

1212 The use of real-time fluorescence could lead to a positive change in the water industry, as operators would be able to start 1213 1214 immediate remedial actions in case of accidental pollution events, cut costs associated with complex analytical approaches 1215 1216 and comply with discharge regulation. Wastewater treatment processes reduce peak T fluorescence primarily by biological 1217 1218 treatment, and peak C through chlorination and reverse 1219 osmosis. There are several simple probes or fluorometers 1220 available on market that measure these two components or more complex systems that convert the peak T fluorescence 1221 1222 signal into BOD values. 1223 However, in case of monitoring surface waters

1224 contaminated with wastewater, the use of simple fluorometers

1225	may not be the best solution to identify the exact source and
1226	take the appropriate remedial actions. Several fluorophores,
1227	with varied origins, were shown to contribute to peaks T and C,
1228	hindering the identification of the source of wastewater
1229	pollution in natural water systems. Single or double wavelength
1230	instruments could only be used as a time and cost effective first
1231	measure for early warning.
1232	Implementation of fluorescence instrumentation for on-line
4222	manifesting is substituted as the second fortune and

monitoring is relatively slow due to several factors, such as 1233 high quantities of suspended solids, temperature, fouling etc. In 1234 1235 order to counteract these issues, dilution of samples is 1236 recommended: to a factor of 10 or to an absorbance value of < 0.05 cm<sup>-1</sup>, in the peak T absorbance region. However, 1237 wastewaters are highly variable in concentration and 1238 1239 composition and therefore a general dilution factor may not be recommended. In addition, post-measurement mathematical 1240 1241 correction could be applied to reduce the impact produced by 1242 external factors.

1243

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Figure 1. Main techniques of processing fluorescence EEMs. Examples of a) peaks identified with the peak picking method, and b) components identified with PARAFAC, for samples of water systems impacted by domestic wastewater.

Figure 2. Removal of fluorescent components during treatment; the removal percentages represent collective values from several studies (<u>Tchobanoglous and Burton 1991</u>, <u>Reynolds 2002</u>, <u>Hambly et al.</u> 2010, Janhom et al. 2011, <u>Murphy et al. 2011</u>, <u>Singh et al. 2012</u>, <u>Cohen et al. 2014</u>, <u>Ou et al. 2014</u>, <u>Riopel et al. 2014</u>, <u>Yu et al. 2014</u>) and unpublished data. Blue arrow – low decrease, Orange arrow – moderate removal, red arrow – high removal.

Potential fluorophores	Potential Component Region		Peak position (nm) Reference		Potential sources in Ww		
nuor opnor es	Lignin phenols		~ 245 (295) / 302	<u>Walker et al.</u> (2009)	Partially degraded food waste,		
		Em < 380 nm	270-2907300- 350	( <u>Hernes et al.</u> 2009) (Stedmon and	etc. Wastewater of paper and pulp		
	Vanilic acid		/ 326	<u>Cory 2014</u> )	2004) fibres from food ( <u>Huang et al.</u>		
Lignins	Syringic acid		/ 338	( <u>Stedmon and</u> <u>Cory 2014</u> )	2010)		
	Breakdown products	Em > 380 nm	230-275 (300- 390) / 400-520	(Baker 2002b, Ciputra et al. 2010, Osburn and Stedmon 2011, Cawley et al. 2012, Bassandeh et al. 2013)	Paper mill effluents ( <u>Baker 2002b</u> , <u>Ciputra et al. 2010</u> , <u>Cawley et al.</u> <u>2012</u> , <u>Bassandeh et al. 2013</u> )		
Aromatic hydrocarbon	Toluene		266 / 300 - 400	Persichetti et al. (2013)	Municipal Ww ( <u>Huang et al. 2010</u> , <u>Mrowiec 2014</u> ); Ww with petrol derivatives ( <u>Mehdizadeh et al. 2011</u> )		
Phenols	Cresols		210-285 / 290- 310	<u>del Olmo et al.</u> ( <u>1996)</u>	Pharmaceutical, fossil fuel or pesticide industries ( <u>Tchaikovskaya</u> <u>et al. 2007</u> ); Domestic Ww from disinfectants ( <u>Tertuliani et al. 2008</u> )		
Aromatic amino acids	Tyrosine	Em <	275 / 304	Lakowicz (2006)	Proteins and peptides ( <u>Lakowicz</u> 2006); Domestic Ww( <u>Burleson et al.</u> <u>1980, Dignac et al. 2000, Huang et</u> <u>al. 2010</u> )		
	Tryptophan		295 / 353	Lakowicz (2006)	Proteins and peptides ( <u>Lakowicz</u> 2006); Livestock Ww ( <u>Choi et al.</u> 2013)		
Indole	R		230 / 330-350	<u>Determann et al.</u> (1998)	Municipal Ww ( <u>Dignac et al. 2000</u> , <u>Tertuliani et al. 2008</u> , <u>Huang et al.</u> <u>2010</u> ); Coal tar, oil shale, personal care products, pesticides and pharmaceuticals ( <u>Gu and Berry</u> <u>1991</u> , <u>Tertuliani et al. 2008</u> , <u>Aiken</u> <u>2014</u> )		
DNA			267 / 327	<u>Vayá et al. (2010)</u>	Proteins ( <u>Lakowicz 2006</u> ); Municipal Ww ( <u>Huang et al. 2010</u> )		
	$\mathbf{O}$	Em < 380 nm	Short UV	Baker et al. (2014)	Municipal Ww ( <u>Guo et al. 2010</u> , <u>Huang et al. 2010</u> ); Landfill leachate ( <u>Baker and Curry 2004</u> )		
Polyaromatic hydrocarbons	Phenanthrene, anthracene, pyrene, fluoranthene, benzo[a]pyrene	Em > 380 nm	220-300 / 370- 430	( <u>Schwarz and</u> <u>Wasik 1976, Patra</u> and Mishra 2001, <u>Yang et al. 2016</u> )	Industrial Ww ( <u>Cohen et al. 2014</u> , <u>Ou et al. 2014</u> ); Municipal Ww ( <u>Huang et al. 2010</u> )		
Quinones		Em >			Microbes, fungi, plants ( <u>Aiken</u> <u>2014</u> ); Activated sludge ( <u>Hu et al.</u> <u>2000</u> )		
Flavonoids		380 nm			Plants ( <u>Aiken 2014</u> ); food ( <u>Egert and</u> <u>Rimbach 2011</u> ); olive oil mill Ww ( <u>Leouifoudi et al. 2014</u> )		
Humic acids			220-320 (400-	<u>IHSS (2015)</u>			

#### Table 1. Fluorophores contributing to regions Em < 380 nm >.

		500) / 400-550		Municipal Ww ( <u>Huang et al. 2010</u> )	
Pharmaceutical ly active compounds	Carbamazepine Fluorquinolone Piroxican	308 / 410 (in 2 mol L <sup>-1</sup> HCl, and 20 min irradiation time) 290 / 500 294 / 372 (in media with pH < 2)	Hurtado-Sanchez Mdel et al. (2015)	Faeces, urine ( <u>Zhang et al. 2008</u> )	
Fluorescent whitening agents	Fluorescent whitening agents		( <u>Takahashi and</u> <u>Kawamura 2006,</u> <u>Tavares et al.</u> <u>2008</u> )	Laundry detergents, sanitary products, toilet paper and tissues; Papermaking industry ( <u>Takahashi</u> and <u>Kawamura 2006</u> , <u>Assaad et al.</u> <u>2014</u> )	

Ww-wastewater

Reference	Samples	Sample size	Sample pH	Analysis temperature	Fluorescence Peak	BOD	COD	TOC
ReynoldsandAhmad (1997)	Raw, settled and treated Ww	129	N/A	Room temperature	280 / 340	0.94- 0.97	N/A	N/A
Ahmad and Reynolds (1999)	Raw Ww	25	3 - 7	10-80 <sup>0</sup> C	248 / 350	0.97	N/A	N/A
Reynolds (2002)	Raw Ww	56	6.8 ±0.4	$26 \pm 10^{0} \text{ C}$	280 / 350	0.93	0.94	0.93
Baker and Inverarity (2004)	Ww effluents and effluent impacted rivers	434	N/A	N/A	220/350	0.85	N/A	N/A
Wang et al. (2007)	Ww impacted lake	26	NI/A	Room	294 / 320	0.54	0.16	N/A
		20	IN/A	temperature	360 / 425	0.65	0.03	N/A
Hudson et al. (2008)	Ww effluents				280/350	0.71	N/A	0.77
		141	N/A	$20^0 \mathrm{C}$	300-370 / 400-500-	0.34	N/A	0.75
Bridgeman et al. (2013)	Domestic Ww, raw and treated	19	NI/A	20 <sup>0</sup> C	275-285 / 340-360	0.92	0.56	N/A
		40	N/A	20 C	320-355 / 410-470	0.88	0.78	N/A
<u>Cohen et al. (2014)</u>	Domestic and industrial Ww, raw	25.34	78 85	Room	<240 (275) / 346	0.82	0.82- 0.99	0.85- 0.99
	and treated	25-54	1.0-0.3	temperature	<240 (305) / 422	0.72	0.91	0.99
Ou et al. (2014)	Industrial Ww, raw	120	7.0	Room	280 / 220	NI/A	0.02	NI/A

7 - 9

120

temperature

N/A

280/320

0.92

N/A

## Table 2. Correlation coefficients for peaks T and C (or PARAFAC analogous

Ww-wastewater; N/A-not available

and treated







- Several fluorophores contribute to common peaks hindering pollution source tracking
- Previous on-line studies may help build a strategy for wastewater analysis
- Dilution of samples, typically up to x10, useful to limit inner filter effect
- Calibration may not be needed for qualitative data
- Research gaps: online application of fluorescence and rapid data processing tools