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## N-alkanes phase change materials and their microencapsulation for thermal energy storage:

Peng, Hao; Zhang, Dong; Ling, Xiang; Li, Yang; Wang, Yan; Yu, Qinghua; She, Xiaohui; Li, Yongliang; Ding, Yulong

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## *n*-alkanes phase change materials and their microencapsulation for thermal energy storage: a critical review

Hao Peng<sup>a\*</sup>, Dong Zhang<sup>a</sup>, Xiang Ling<sup>a</sup>, Yang Li<sup>a</sup>, Yan Wang<sup>a</sup>, Qinghua Yu<sup>b,c\*</sup>,

Xiaohui She<sup>b</sup>, Yongliang Li<sup>b</sup>, Yulong Ding<sup>b</sup>

<sup>a</sup> Jiangsu Key Laboratory of Process Enhancement and New Energy Equipment Technology, School of Mechanical and Power Engineering, Nanjing Tech University, No. 30 Pu Zhu South Road, Nanjing 211816, P. R. China
 <sup>b</sup> Birmingham Centre for Energy Storage, School of Chemical Engineering, University of Birmingham, Birmingham B15 2TT, UK

<sup>c</sup> School of Power and Mechanical Engineering, Wuhan University, Wuhan 430072, P. R. China

\* Corresponding author Tel: 86-25-83243112

Email address: phsight1@hotmail.com (H. Peng)

\* Corresponding author Tel: 44-121-4146965

Email address: yqh2015@hotmail.com (Q. Yu)

#### Energy & Fuels

Abstract: n-alkanes and their blends, are characterized as phase change materials (PCMs) due to their superior thermodynamic performances, for storing thermal energy in various practical applications (solar or wind energy). Such materials present some limitations, including lower thermal conductivity, supercooling, phase segregation, volume expansion, among others. To address these problems, microencapsulation of *n*-alkanes and their blends is being successfully developed. A considerable amount of works has been published in this regard. Hence, the aim of this review is focused on two aspects: summarize the pure *n*-alkanes and their blends PCMs; describe their microencapsulation. PCM-interesting characteristics (transition temperatures and enthalpies) of pure *n*-alkanes, multinary alkanes and paraffins (over 140 types) were listed, while the phase equilibrium evaluations of multinary alkanes were elaborated. The essential information: core and shell materials, crystallization and melting characteristics, encapsulation/thermal storage efficiencies, thermal conductivities and synthesis methods of microencapsulated *n*-alkanes and their blends were listed (over 200 types). A brief introduction of the synthesis methods, such as physical, chemical, physical-chemical and self-assembly processes, were presented. The characterization of microcapsules like thermal properties (phase change behaviors, thermal conductivity and thermal stability), physical properties (microcapsules size distribution & morphologies, efficiencies, mechanical strength and leakage) and chemical properties were discussed and analyzed. Finally, the practical applications of microencapsulated *n*-alkanes and their blends in the field of slurry, buildings, textiles and foam were reported.

*keywords*: *n*-alkanes; phase change materials; microencapsulation; thermal energy storage; microencapsulated phase change materials

C <sub>n</sub>	pure <i>n</i> -alkanes	$\Delta n_c$	difference of carbon atom number
$C_{2p}$	even-numbered n-alkanes	Acronyms	
$C_{2p+1}$	odd-numbered n-alkanes	AFM	atomic force microscopy
d	diameter (m)	DSC	differential scanning calorimetry
E <sub>en</sub>	encapsulation efficiency	FT-IR	fourier transformation infrared spectroscopy
$E_{es}$	energy storage efficiency	LHES	latent heat energy storage
FP	freezing point (°C/K)	LFA	laser flash apparatus
LH	latent heat (J/g)	MPCM	microencapsulated phase change material
$L_r$	leakage rate	PCMs	phase change materials
$M_t$	mass of microcapsules after a certain time (g)	PSD	particle size distribution
$M_0$	mass of dried microcapsules (g)	SEM	scanning electron microscope
MP	melting point (°C/K)	TES	thermal energy storage
n <sub>c</sub>	carbon atom number	TGA	thermogravimetric analysis
$T_{mo}$	melting onset temperature (°C)	WR	weight ratio
$T_{mp}$	melting peak temperature (°C)	XRD	X-ray diffraction
$T_{co}$	crystallization onset temperature (°C)	Greek syml	bols
$T_{cp}$	crystallization peak temperature (°C)	λ	thermal conductivity (W/m·K)
x	molar faction	Subscripts	
$\Delta H_m$	melting enthalpy (J/g)	С	core
$\Delta H_c$	crystallization enthalpy (J/g)	w	shell
$\Delta T_s$	supercooling degree (°C)	р	MPCM particles

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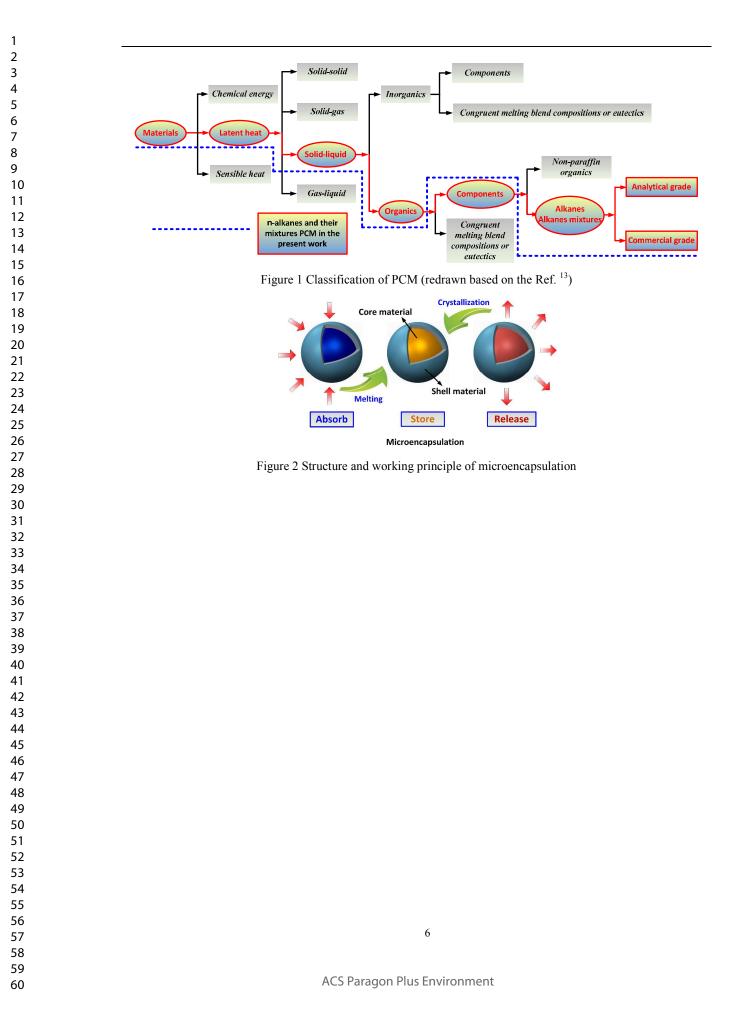
#### 1 Introduction

Latent heat energy storage (LHES) using phase change materials (PCMs) is one of the most efficient methods to store thermal energy, such as in the renewable energy systems (solar or wind energy), building, refrigeration, textile, among others. PCMs have the competitive merits of higher thermal storage capacity and isothermal behavior, in contrast to sensible heat energy storage. Admittedly, high energy storage density and capacity for charging and discharging are the desirable features of any heat/cold thermal energy storage (TES) systems. These systems with PCMs as thermal energy materials have been investigated for many years <sup>1-12</sup>.

In general, the PCMs with solid-liquid phase change are mainly used to store thermal energy. Abhat <sup>13</sup> proposed a commonly used classification of these PCMs, organic and inorganic, as shown in Figure 1.

Among organic materials perspective for LHES, alkanes and their blends, many referred to as paraffins, are very attractive for using as PCM due to their superior thermodynamic performances, such as stable phase change, minimal supercooling, high enthalpies, among others. However, they also have limitations such as lower thermal conductivity, phase segregation and volume expansion in the process of phase transition. In addition, the leakage problem might occur during the melting process as well. These problems have been addressed by microencapsulated PCMs (MPCMs), which are named as 'PCM microcapsules'. Figure 2 shows a typical structure of microcapsules which pack the PCMs core individually with the organic or inorganic shell, and the microencapsulation working principle is introduced as well. The size of microcapsules can vary from few nanometers to microns. Microencapsulation helps to overcome low thermal conductivity by increasing the surface to volume ratio for the PCM. Microcapsules also provide a stable structure can therefore handle liquids as a solid material and prevent leakage of the melted PCMs.

Currently, even though many reviews with respect to the various PCMs for TES are available <sup>2, 13-16</sup>, as well as the review articles related to the microencapsulation of PCMs <sup>17-24</sup>, however, to the best of our knowledge, the literature review on the *n*-alkanes PCMs and their microencapsulation for TES is never found. Actually, the *n*-alkanes and their blends had been extensively studied for the past five decades, but only a few works were related to their PCMs utilization. In contrary, the researches in regard to microencapsulated *n*-alkanes and their blends as PCMs showed a prosperous upward tendency in recent decade. Undoubtedly, the researches on these two aspects supplement each other. Therefore, a main line to link these two aspects is essential (Materials  $\rightarrow$ Microcapsules). To this end, this paper attempts to summarize the *n*-alkanes and their blends PCMs firstly (the blue dot line in Figure 1), and then describes their microencapsulation systematically. The synthesis techniques, thermal properties, physical properties and chemical properties are summarized and analyzed. Finally, the practical applications of microencapsulated *n*-alkanes and their blends in the field of slurry, buildings, textiles and foam were reported.



#### 2 Pure *n*-alkanes and their blends as PCMs

#### 2.1 Pure n-alkanes

The properties of pure *n*-alkanes  $C_nH_{2n+2}$  (hereafter denoted by  $C_n$ ) have been studied extensively in literatures, which include melting point, enthalpy, heat capacity, conductivity, density, among others. Among these properties, melting point and enthalpy are the PCM-interesting characteristics that predominantly affect the performance of a TES system.

In regard to these two properties, the most comprehensive review of 67  $C_n$  (carbon number  $C_1 \sim C_{390}$ ) was presented by Dirand et al.<sup>25</sup>. In addition to this, a part of  $C_n$  (within the range of carbon number in Dirand et al's review) were measured by Himran et al.<sup>26</sup>, Rajabalee et al.<sup>27</sup>, Ventola et al.<sup>28-29</sup>, Mondieig et al.<sup>30</sup> and Huang et al.<sup>31</sup> using DTA or DSC instruments as well.

Dirand et al <sup>25</sup> distinguished the thermodynamic data of the  $C_n$  into four parts: melting points, enthalpies, order-disorder (o-d) transition enthalpies and disorder-disorder (d-d) transition temperatures. This is due to the fact that the  $C_n$  have complex polymorphic nature with the existence of a mesostate, therefore, the phase change processes were very complicated and simply characterized by a solid-solid and a solid-liquid equilibrium transitions at constant temperature <sup>25, 30</sup>. Regardless of the complex phase change behavior of  $C_n$ , Figure 3 depicted the two dominating properties (melting points and enthalpies) of  $C_n$  from octane to pentacontane ( $C_8 \sim C_{50}$ ) by summarizing and averaging the available data obtained by the above mentioned literatures. It should be noted that the enthalpies showed in Figure 3 are the solid-solid and solid-liquid transition enthalpies. The data accuracies in Figure 3 were estimated, the melting points and the enthalpies with the deviations of  $\pm 1\%$  and  $\pm 3\%$ , respectively.

Except for thermodynamic properties, the thermophysical properties (specific heat capacity, density, thermal conductivity, among others) of  $C_n$  were studied by Huang et al. <sup>31</sup>, Atkinsion et al. <sup>32</sup>, Johansen <sup>33</sup>, Watanabe <sup>34</sup> and Vargaftik <sup>35</sup>, and a summarized review with respect to these properties was conducted by Kenisarin <sup>36</sup>.

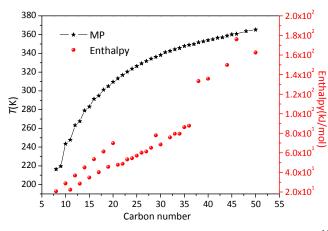


Figure 3. Melting points and enthalpies of some  $C_n$  on the basis of Dirand et al. <sup>25</sup> (from  $C_8$  to  $C_{50}$ )

#### 2.2 Multinary C<sub>n</sub>

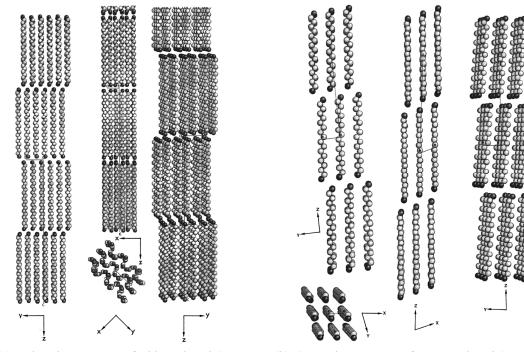
Generally, the  $C_n$  have specific melting points and enthalpies, which limit their practical applications. However, their blends (binary, ternary or multinary systems) have proved the greater value as tunable PCMs for TES systems because the temperature range are substantially enlarged and enriched.

If following the permutation and combination theory, the binary and ternary mixtures of the  $C_n$  (41 types in the

present work) should have  $C_{41}^2 + C_{41}^3 = 820 + 10660 = 11480$  groups. It is absolutely impossible to accomplish the studies for these huge groups of combination. Dirand et al. <sup>37</sup> pointed out that the behavior of mixtures of C<sub>n</sub>'s have to obey the four laws of thermodynamics: (a) Phase stability; (b) Miscibility in the solid state; (c) Size of molecules; and (d) Thermodynamic representation of phase equilibrium. According to these fundamental laws, the possible combinations are therefore dramatically reduced.

#### 2.2.1 Binary systems

Alkanes have complex crystalline structures for the odd and even numbers of carbons in the chain. Dirand et al. <sup>37</sup> and Craig et al <sup>38</sup> proposed the following classification with the key structures from  $C_{13}$ - $C_{60}$ . The odd-number  $C_n$  have ' $C_{23}$ -*Pbcm*' orthorhombic structure ( $C_{13}$ - $C_{41}$ ), as shown in Figure 4(a), the even-number  $C_n$  have ' $C_{18}$ -*P*1' triclinic structure for  $C_{14}$ - $C_{26}$ , as shown in Figure 4(b), ' $C_{36}$ -*P*2 $_1/a$ ' monoclinic structure for  $C_{28}$ - $C_{36}$ , '*Pbca*' orthorhombic structure for  $C_{38}$ ,  $C_{40}$  and  $C_{44}$ , and ' $C_{36}$ -*Pca*2 $_1$ ' orthorhombic structure for  $C_{46}$ ,  $C_{50}$  and  $C_{60}$  <sup>38</sup>. These different structures will influence their solid state miscibility as well as the phase change characteristics of their mixtures. Karvchenko <sup>39</sup> proposed a basic rule to predict the miscibility in the binary systems of  $C_n$  from the different factor of the molecule lengths, as shown in Table 1.



(a)  $C_{23}$ -*Pbcm*' key structure of odd-numbered  $C_{2p+1}$ 's (b)  $C_{2p+1}$ 

 $(11 \le 2p + 1 \le 41)$ 

(b) 'C<sub>18</sub>-P1' key structure of even-numbered C<sub>2p</sub>'s (6 $\leq$ 2p

≤26)

Figure 4 Key structures of odd-numbered and even-numbered  $C_n^{-38}$ 

Table 1. Miscibility of binary  $C_n$  mixtures versus number difference of Carbon atoms in the solid state at room temperature according to Kravchenko's predictions <sup>39</sup> ( $n_c$  is the carbon atoms numbers)

$\Delta n_{\rm c} = n_{\rm c} - n_{\rm c}'$	Total miscibility	Partial miscibility	No miscibility	Comments
1	$n_{\rm c} > 16^1$	$17 > n_{\rm c} > 7$	$n_{\rm c} < 8$	<sup>1</sup> if the two consecutive $C_{2p}$ and $C_{2p+1}$ do not
2	<i>n</i> <sub>c</sub> >33	$34 > n_{\rm c} > 13$	<i>n</i> <sub>c</sub> <14	have the same crystalline structure, they
4	$n_{\rm c} > 67$	$68 > n_{\rm c} > 27$	n <sub>c</sub> <28	cannot form a continuous solid solution.

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Based on this rule, the studies related to binary mixtures of  $C_n$ 's as PCMs were performed. The engineering blends prioritization for a specific application temperature, the blends phase equilibrium evaluation to select congruent melting or eutectic type of more suitable compositions as potential PCMs, are the primary focused issues in this review. Gunasekara et al. <sup>40</sup> presented a review of phase equilibrium in the design of suitable blended PCMs for TES, and summarized a series of  $C_n$  blends systems. However, some of the  $C_n$  blends were still missing. Therefore, based on their work, Table 2 summarized more comprehensive binary  $C_n$  mixtures ( $C_8 \sim C_{50}$ ) by listing the PCM-interesting characteristics, and the temperature range is from 211.7K to 359.1K (-61.5°C~86.0°C) <sup>25-28, 39-61</sup>. The compositions are either weight, molar, or volumetric percentage, while the enthalpy are either kJ/kg or kJ/mol. Table 2. Thermodynamic characteristics of binary mixtures of  $C_n$ 's PCM for TES based on Ref. <sup>40</sup> (NA: not available; MP: melting point)

No.	Binary	Characteristics <sup>2</sup>	Composition ( <sup>w</sup> w%, <sup>a</sup> mol%, <sup>v</sup> V%)	MP(K)	Enthalpy ( <sup>k</sup> kJ/kg, <sup>m</sup> kJ/mol)	Year	Re
1	C <sub>8</sub> -C <sub>10</sub>	Е	<sup>a</sup> 16C <sub>10</sub>	211.7	NA	1995	27
2	C <sub>10</sub> -C <sub>12</sub>	Е	<sup>a</sup> 20C <sub>12</sub>	238.2	NA	2002	29
3	$C_{11}$ - $C_{12}$	Р	<sup>a</sup> 65C <sub>12</sub>	251.2	NA		
4	$C_{11}$ - $C_{13}$	Е	<sup>a</sup> 23C <sub>13</sub>	246.1	NA		
5	$C_{11}$ - $C_{18}$	IIM <sup>3</sup>	<sup>w</sup> 21C <sub>18</sub>	279.6	NA	2015	41
6	C <sub>12</sub> -C <sub>13</sub>	ICM	<sup>a</sup> 17.7C <sub>13</sub>	257.5	<sup>k</sup> 185	2017	42-4
7	$C_{12}$ - $C_{14}$	Е	<sup>a</sup> 19C <sub>14</sub>	258.2	NA	1996	44
8	C <sub>12</sub> -C <sub>15</sub>	Е	<sup>a</sup> 24 C <sub>15</sub>	258.6	<sup>m</sup> 25.8	1998	45
9	$C_{13}$ - $C_{14}$	Р	<sup>a</sup> 25C <sub>13</sub>	272.0	<sup>k</sup> 212-110	2002	29
10	C <sub>13</sub> -C <sub>15</sub>	Е	<sup>a</sup> 20C <sub>15</sub>	266.4	<sup>m</sup> 26	1998	46
11	C <sub>14</sub> -C <sub>15</sub>	Е	<sup>a</sup> 15C <sub>15</sub>	276.2	NA	2005	47
12	$C_{14}$ - $C_{16}$	Е	<sup>v</sup> 8.33C <sub>16</sub>	274.9	<sup>k</sup> 156.2	1999	48
		ICM	<sup>a</sup> 6.74C <sub>16</sub>	274.9	<sup>k</sup> 146	2003	49
		ICM	<sup>a</sup> 7.7C <sub>16</sub>	275.0	<sup>k</sup> 146	2004	50
		Е	<sup>a</sup> 17.5C <sub>16</sub>	276.2	NA	2004, 2005	30,
13	$C_{14}$ - $C_{18}$	Е	NA	275.3	<sup>k</sup> 227.5	2004	51
14	$C_{14}$ - $C_{21}$	Е	NA	278.6	<sup>k</sup> 200.3		
15	$C_{14}$ - $C_{22}$	Е	NA	278.7	<sup>k</sup> 234.3		
16	C <sub>15</sub> -C <sub>16</sub>	Р	<sup>a</sup> 86C <sub>16</sub>	287.2	NA	1997	52
17	C <sub>15</sub> -C <sub>17</sub>	ICM	<sup>a</sup> 12.5C <sub>17</sub>	281.2	NA	1996, 1997	44,
18	C <sub>15</sub> -C <sub>18</sub>	Е	NA	282.2	<sup>k</sup> 271.9	2007	53
19	C <sub>15</sub> -C <sub>21</sub>	Е	<sup>a</sup> 6.5C <sub>21</sub>	281.5	<sup>k</sup> 163	1996	44
20	C <sub>15</sub> -C <sub>22</sub>	Е	NA	281.6	<sup>k</sup> 214.8	2004	51
21	$C_{16}$ - $C_{17}$	Е	<sup>a</sup> 8.1C <sub>17</sub>	289.3	NA	1997, 2004	30,
22	$C_{16}$ - $C_{18}$	Е, Р	<sup>a</sup> 12.5C <sub>18</sub> , <sup>a</sup> 78C <sub>18</sub>	288.2, 295.3	NA	2004	30
23	$C_{16}$ - $C_{28}$	Е	<sup>a</sup> 5C <sub>28</sub>	290.4	NA	2000	54
24	C <sub>16</sub> -C <sub>41</sub>	Е	<sup>a</sup> 4C <sub>41</sub>	290.5	NA		

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25	$C_{17}$ - $C_{18}$	Р	$a88C_{18}$	298.3	NA	2004	30
26	C <sub>17</sub> -C <sub>19</sub>	ICM	<sup>a</sup> 5C <sub>19</sub>	295.0	<sup>m</sup> 38.9	1996	55
27	C <sub>18</sub> -C <sub>19</sub>	E	<sup>a</sup> 6C <sub>19</sub>	299.3	NA	2004	30
28	C <sub>18</sub> -C <sub>20</sub>	E, P	<sup>a</sup> 6C <sub>20</sub> , <sup>a</sup> 90C <sub>20</sub>	301.2, 308.4	NA		
29	C <sub>18</sub> -C <sub>21</sub>	E	NA	299.2	173.9	2004	51
30	C <sub>18</sub> -C <sub>22</sub>	E	NA	300.2	203.8		
31	C <sub>19</sub> -C <sub>20</sub>	Р	<sup>a</sup> 94C <sub>20</sub>	308.3	NA	2004	30
32	C <sub>19</sub> -C <sub>21</sub>	ICM	<sup>a</sup> 10C <sub>21</sub>	305.5	<sup>m</sup> 43.5	1985	56
33	C <sub>20</sub> -C <sub>21</sub>	Е	<sup>a</sup> 5C <sub>21</sub>	308.5	NA	2004	30
34	C <sub>20</sub> -C <sub>22</sub>	Е	<sup>a</sup> 3C <sub>22</sub>	309.5	NA	1996	44
35	C <sub>21</sub> -C <sub>22</sub>	Р	<sup>a</sup> 5C <sub>22</sub>	316.8	<sup>m</sup> 48.7	1999	57
36	C <sub>21</sub> -C <sub>23</sub>	Р	<sup>a</sup> 1.5C <sub>23</sub>	313.7	NA	1996	58
37	C <sub>22</sub> -C <sub>23</sub>	IIM <sup>3</sup>	<sup>a</sup> 20C <sub>23</sub>	317.4	NA	1998	59
38	C <sub>22</sub> -C <sub>24</sub>	IIM <sup>3</sup>	<sup>a</sup> 20C <sub>24</sub>	317.9	NA	2004	30
39	C <sub>23</sub> -C <sub>24</sub>	IIM <sup>3</sup>	<sup>a</sup> 20C <sub>24</sub>	320.6	NA		
40	C <sub>23</sub> -C <sub>25</sub>	IIM <sup>3</sup>	<sup>a</sup> 20C <sub>25</sub>	321.9	<sup>m</sup> 52.6	1999	60
41	C <sub>25</sub> -C <sub>27</sub>	Р	<sup>a</sup> 96C <sub>27</sub>	330.3	NA	2004	30
42	C <sub>25</sub> -C <sub>28</sub>	ICM	24.6C <sub>28</sub>	327.0	NA	1995, 1996	61-6
43	$C_{26}-C_{28}$	Р	<sup>a</sup> 93C <sub>28</sub>	333.3	<sup>m</sup> 62.3	2004	63
44	C <sub>28</sub> -C <sub>41</sub>	Е	<sup>a</sup> 8C <sub>41</sub>	337.2	NA	2000	54
45	C <sub>32</sub> -C <sub>34</sub>	IIM <sup>3</sup>	<sup>a</sup> 20C <sub>34</sub>	343.0	<sup>k</sup> 172	2005	28
46	C <sub>32</sub> -C <sub>36</sub>	ICM	<sup>a</sup> 5C <sub>36</sub>	342.2	<sup>k</sup> 168		
47	C <sub>34</sub> -C <sub>36</sub>	IIM <sup>3</sup>	<sup>a</sup> 20C <sub>36</sub>	346.5	<sup>k</sup> 171		
48	C <sub>36</sub> -C <sub>40</sub>	PIP	<sup>a</sup> 50C <sub>40</sub>	350.2	<sup>k</sup> 223		
49	C40-C44	PIP	<sup>a</sup> 52C <sub>44</sub>	355.2	<sup>k</sup> 229		
50	C <sub>44</sub> -C <sub>50</sub>	Е	<sup>a</sup> 9C <sub>50</sub>	359.1	NA	1995, 1996	61-6

<sup>2</sup> E-eutectic; P-peritectic; ICM-isomorphous congruent minimum melting; IIM-isomorphous incongruent melting (ascendant type); PIP-partially isomorphous peritectic

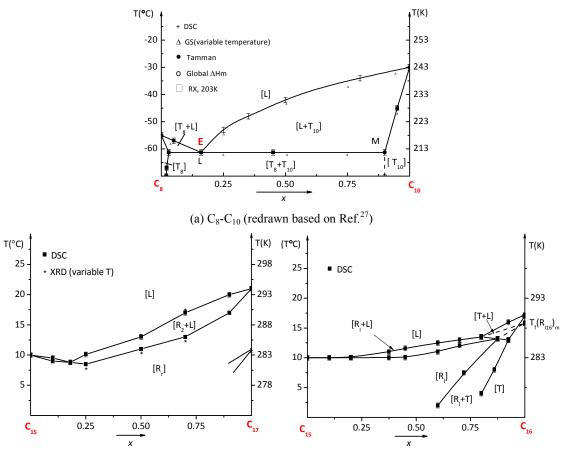
<sup>3</sup> in IIM type, the melting point is extracted from the proposed data in literature for molar percentage of ~20 mol% in *n*-alkanes with longer chains.

As shown in Table 2, a part of studies aimed at finding the right compositions in the right  $C_n$  blends for PCM utilization. The first priority is to adjust the melting point of blends at the required temperature level in practical application, and then to choose the blends having a narrow thermal window that can store or release 95% of the total latent heat. Simultaneously, several studies with respect to the phase equilibrium were proposed as well, and potential PCM materials for TES might be found in light of some features (eutectic or peritectic point) in binary solidus-liquidus phase diagrams. Among these investigations focused on engineering or potential binary blended PCMs, systematic evaluations on a group of substantial binary mixtures were conducted by Ventola et al. and Mondieig et al. <sup>28-30</sup>. Mondieig et al. <sup>30</sup> ascertained that the group of  $C_n$  had a rich, complex polymorphic nature with the existence of mesostate. This mesostate regarded as rotator (R) is a crystalline state, having rotational freedom along their long axes, between the normal, ordered solid state and liquid. As a consequence, the  $C_n$  blends appeared

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very complex phase change behaviors (melting or freezing types), and sometimes, the confusion conclusions presented by different investigators are inevitable.

Generally, as mentioned by Gunasekara et al. <sup>40</sup>, it is accepted that the binary systems belonging to the completely or almost completely isomorphous congruent types are  $C_{15}-C_{17}^{44, 52}$ ,  $C_{17}-C_{19}^{55}$ ,  $C_{19}-C_{21}^{56}$ ,  $C_{25}-C_{28}^{61-62}$ ,  $C_{32}-C_{36}^{28}$ , the binary isomorphous incongruent melting systems (ascendant type) found are  $C_{11}-C_{18}^{41}$ , all the odd-odd and odd-even blends from  $C_{22}$  to  $C_{24}^{30, 59}$ ,  $C_{23}-C_{25}^{60}$ ,  $C_{32}-C_{34}$  and  $C_{34}-C_{36}^{28}$ . The remainders are partially isomorphous. The phase change characteristics of these binary  $C_n$  blends include: eutectic, peritectic, isomorphous congruent melting (ICM), isomorphous incongruent melting (IIM) and partially isomorphous peritectic (PIP) <sup>40</sup>, which are elaborated in Table 2. Actually, most of these phase change characteristics are deduced from the binary phase diagram, and hence Figure 5 depicted the typical phase diagrams of eutectic system ( $C_8-C_{10}$ ), peritectic system ( $C_{15}-C_{16}$ ) and ICM system ( $C_{15}-C_{17}$ ) that were redrawn by extracting the figure data from the original literatures <sup>27, 52</sup>.



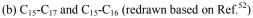


Figure 5 Phase diagrams of binary systems  $C_8-C_{10}$ ,  $C_{15}-C_{17}$  and  $C_{15}-C_{16}$  (redrawn based on Ref. <sup>27</sup> and Ref. <sup>52</sup>) (a)  $C_8-C_{10}$  (redrawn based on Ref.<sup>27</sup>) (b)  $C_{15}-C_{17}$  and  $C_{15}-C_{16}$  (redrawn based on Ref.<sup>52</sup>)

The most frequently studied binary  $C_n$  system is  $C_{14}$ - $C_{16}$ <sup>30, 40, 47-50</sup>, however, the reported phase change characteristics of these works have discrepancies. For example, it has been reported with a eutectic <sup>48</sup>, an isomorphous congruent minimum melting type <sup>49 50</sup>, and as a partially isomorphous system with a eutectic and a peritectic <sup>30</sup>. The temperatures of these eutectic/congruent melting points are rather close, but the compositions vary from each other (in Table 2). Actually, the confusion in regard to the  $C_{14}$ - $C_{16}$  binary system is the distinction

between a partially isomorphous eutectic and an isomorphous congruent minimum melting type. Overall evaluations including crystallography, miscibility and phase equilibrium of  $C_{14}$ - $C_{16}$  blends were conducted by Ventolà et al.<sup>29</sup> and Mondieig et al.<sup>30</sup>, which are crucial for a deep understanding of the system's phase change behaviors. As mentioned in Craig et al's work<sup>38</sup>, both components of the  $C_{14}$  and  $C_{16}$  have '*P*1' triclinic structure. Hence, He et al.<sup>48</sup> pointed out that the  $C_{14}$ - $C_{16}$  binary is an isomorphous system and found a eutectic point of the laboratory-grade  $C_{14}$ - $C_{16}$  mixture occurs at 91.67%  $C_{14}$  (8.33%  $C_{16}$ ), and the phase change temperature at this point is approximately 1.7°C. But four years later, they ascertained that this point is not a eutectic point <sup>49</sup>. Subsequently Mondieig et al.<sup>30</sup> said that the system should be partially isomorphous with a eutectic one (*x* is from 0.46 to 0.93) at high temperature side. The other confused binary system is  $C_{12}$ - $C_{13}$ . Yilmaz et al.<sup>64</sup> presented the liquidus line of  $C_{12}$ - $C_{13}$  and found a maximum melting point of -3.3°C at 80%  $C_{13}$ , whereas Ventolà et al.<sup>29</sup> identified a eutectic composition in this system. Most recently, Gunasekara et al.<sup>40, 42-43</sup> carried out an overall experimental investigation of  $C_{12}$ - $C_{13}$ , The obtained phase diagram indicated a congruent minimum-melting solid solution and polymorphs phases at lower temperatures. However, the system does not represent a eutectic, which is against to phase diagrams proposed by the Yilmaz et al.<sup>64</sup> and Ventolà et al.<sup>64</sup>.

Thanks to these discrepancies and confusions, a full understanding of the phase equilibrium of binary  $C_n$ , primarily the construction of the solidus is required, for the sake of seeking the appropriate PCM for a specified TES system.

#### 2.2.2 Multinary systems

Compared to the binary systems, a relatively small number of investigations with respect to the ternary and multinary systems were performed. Table 3 summarized the PCM-interesting characteristics of ternary mixtures of  $C_n (C_{11} \sim C_{36})$ . Since a set of compositions for these ternary systems were reported in the literatures, in order to select a PCM with similar phase change behavior of a pure compound <sup>29</sup>, the compositions with narrowest thermal window were listed in Table 3. Actually, few works were related to the right compositions selection of PCM, except for Ventolà et al.<sup>28-29</sup>. Ventolà et al.<sup>28-29</sup> proposed some potential PCM compositions to cater to the application temperatures (-11°C and 70~85°C), within a narrow thermal window, storing or releasing 95% of the total heat. They also indicated that the thermal window should be as small as possible (just 1~2°C) for most of practical applications. Multinary  $C_n$  systems were conducted by Craig et al. <sup>65</sup> ( $C_{18}$ - $C_{19}$ - $C_{20}$ - $C_{21}$ - $C_{22}$ - $C_{23}$ - $C_{24}$ - $C_{25}$ ,  $C_{22}$ - $C_{23}$ - $C_{24}$ - $C_{25}$ - $C_{26}$ , however, the main content was to determine the unit-cell parameters and to present the crystallographic high resolution synchrotron diffraction data, which was irrelevant to the present subject.

As a consequence, as most of ternary or multinary  $C_n$  mixtures are not directly PCM-ideal materials (like congruent melting or eutectic types), the phase change characteristics, such as phase diagrams, phase separation, among others., need to be better evaluated to confirm their potential and suitability as PCMs.

No.	Ternary	Composition (mol%)	MP (K)	Thermal Window δ <sub>95%</sub> (K)	Enthalpy (kJ/kg)	Year	Ref.
1	$C_{11}$ - $C_{12}$ - $C_{13}$	3C <sub>11</sub> , 85C <sub>12</sub> , 12C <sub>13</sub>	257.1	1.2	141.3	2002	29
2	C <sub>12</sub> -C <sub>13</sub> -C <sub>14</sub>	51C <sub>12</sub> , 40C <sub>13</sub> , 9C <sub>14</sub>	261.4	1.6	144.1		

Table 3. Thermodynamic characteristics of ternary mixtures of  $C_n$ 's PCM for TES(NA: not available)

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3	$C_{14}$ - $C_{15}$ - $C_{16}$	$73C_{14}, 14C_{15}, 13C_{16}$	276.3	0.5	NA	1999 60
4	$C_{15}$ - $C_{16}$ - $C_{17}$	77C <sub>15</sub> , 7C <sub>16</sub> , 16C <sub>17</sub>	283.2	0.6	NA	1997 <sup>52</sup>
5	$C_{16}$ - $C_{17}$ - $C_{18}$	80C <sub>16</sub> , 10C <sub>17</sub> , 10C <sub>18</sub>	289.5	NA	NA	1999 <sup>60</sup>
6	$C_{18}$ - $C_{19}$ - $C_{20}$	90C <sub>18</sub> ,5C <sub>19</sub> , 5C <sub>20</sub>	300.6	0.2	NA	
7	$C_{19}$ - $C_{20}$ - $C_{21}$	90C <sub>19</sub> ,5C <sub>20</sub> , 5C <sub>21</sub>	305.5	0.2	NA	
8	$C_{16}$ - $C_{28}$ - $C_{41}$	50C <sub>16</sub> , 24C <sub>28</sub> , 26C <sub>41</sub>	347.7	NA	NA	2000 54
9	$C_{22}$ - $C_{23}$ - $C_{24}$	48C <sub>22</sub> , 48.5C <sub>23</sub> , 3.5C <sub>24</sub>	319.0	NA	NA	1999 <sup>67</sup>
10	C <sub>32</sub> -C <sub>34</sub> -C <sub>36</sub>	34C <sub>32</sub> , 31C <sub>34</sub> , 35C <sub>36</sub>	345.2	1.0	NA	2005 23

Paraffins and paraffin waxes consist of a mixture of hydrocarbon molecules containing between twenty to forty carbon atoms (80%~95% C<sub>n</sub>), which are produced from petroleum, coal or oil shale. Therefore, paraffins can be identified as the unrefined alkanes blends. Generally, paraffins are relatively cheap in comparison with pure C<sub>n</sub> and have high enthalpies, which are the common PCMs utilized in practical applications. The melting points and enthalpies for laboratorial and commercial paraffins PCMs have been reported extensively nowadays <sup>68 69 70</sup>.

#### 2.3 Summaries and discussions

In PCM literature with  $C_n$  and their blends as a whole, it is well known that the  $C_n$  have the merits of chemically stable, noncorrosive and high enthalpies, in particular are regarded as the ideal PCMs. However, the specific melting points and relative high price limit their practical applications. Simultaneously, the  $C_n$  blends can provide suitable materials to work as PCM if two conditions are respect. The first is to find the right compositions in the right  $C_n$  blends to obtain the melting point at the required level of temperature. The second one is to choose blends having a narrow thermal window that can store or release 95% of the total latent heat.

To employ  $C_n$  blends as PCM with robust performances, an overall understanding of their phase diagrams and phase change behaviors is crucial. A narrow thermal window (phase change temperature range) with no phase separation is the properties pursued for an ideal and functional PCM.

Generally, the phase diagrams of  $C_n$  blends are complex, and previous works showed that congruent melting compositions are definitely the most expected for PCMs, with the solid and liquid in equilibrium having the same composition. Eutectics, peritectics, ICM, IMM, PIP types of phase change characteristics are elaborated through phase diagrams in this review as well. Among these phase change behaviors, eutectics and peritectics have been considered largely from a PCM selection perspective; even though peritectics are not ideal because of the supercooling and phase separation might occur in peritectics nonequilibrium cooling process. Furthermore, the literature assessment presented here, mostly focused on the binary  $C_n$  systems. Some popular systems to be considered as PCM were specified, for example,  $C_{14}$ - $C_{16}$ ,  $C_{15}$ - $C_{18}$ ,  $C_{15}$ - $C_{21}$ ,  $C_{20}$ - $C_{22}$ ,  $C_{26}$ - $C_{28}$ , and  $C_{44}$ - $C_{50}$ , among others. The ternary systems for PCMs were rarely involved, except for the  $C_{11}$ - $C_{12}$ - $C_{13}$ ,  $C_{12}$ - $C_{13}$ - $C_{14}$  and  $C_{32}$ - $C_{34}$ - $C_{36}$ .

Despite numerous studies have proposed, there is still a lot to explore. First, it is interesting that the binary system with a large discrepancy in chain length ( $\Delta n_c \ge 6$ ) still showed a eutectic characteristic ( $C_{11}$ - $C_{18}$ ,  $C_{14}$ - $C_{21}$ ,  $C_{14}$ - $C_{22}$ ,  $C_{15}$ - $C_{21}$ ,  $C_{15}$ - $C_{22}$ ,  $C_{16}$ - $C_{28}$ ,  $C_{16}$ - $C_{41}$ ,  $C_{28}$ - $C_{41}$ ), which does not respect the basic laws revealed by Dirand et al. and Karvchenko <sup>37, 39</sup>. Therefore, a huge amount of new combinations can be created, and then deserve further investigations. Second, ternary systems are the neglected category in the PCM-context (few works published), but are promising for exploration in the future. Finally, the phase equilibrium identification of  $C_n$  blends is done to

various levels by different works; some are very comprehensive, while some are just preliminary. The confusions in regard to the phase change characteristics of blends  $C_{14}$ - $C_{16}$ ,  $C_{12}$ - $C_{13}$  mentioned above are attributed to this issue. To obtain PCM-design conclusions of a blend, a comprehensive phase equilibrium study is fundamental, which may require multiple testing technologies: DSC, TGA, XRD, FT-IR, and SEM, among others.  $C_n$  blends could be quite complex, e.g. with intricate metastable phases such like mesostates, that require such a combination of detection techniques. Therefore, the comprehensive studies in related to phase equilibrium of  $C_n$  blends are worth improving.

#### 3 Microencapsulation of n-alkanes and their blends in PCMs design

This section has three sub-sections, which includes: Summarization of microencapsulated  $C_n$  and their blends, Synthesis methods for  $C_n$  and their blends microcapsules, and Characterization of microencapsulated  $C_n$  and their blends.

The first sub-section 3.1 summarized the microcapsules with various core materials:  $C_n$ , Paraffins,  $C_n$  blends and  $C_n$  mixed with other compositions (Tables 4-7). Based on the information in Tables 4-7, the sub-section 3.2 described the synthesis methods and elaborated some typical examples in regard to these methods. The last sub-section 3.3 discussed the characterization of microencapsulated  $C_n$  and their blends.

#### 3.1 Summarization of microencapsulated Cn and their blends

This sub-section summarized the microcapsules with various core materials:  $C_n$ , Paraffins,  $C_n$  blends and  $C_n$  mixed with other compositions, for their use as PCM in practical applications from 2007 to 2017. Their most important information chosen here are: compositions of both core and shell materials, crystallization and melting characteristics, encapsulation/energy storage efficiency, thermal conductivity and synthesis method. Their remainder information, for instance, shell characterization, chemical properties, thermal reliability, applications, among others, are discussed in sub-sections 3.3 & Section 4.

An enormous amount of experimental results are available concerning the microencapsulated  $C_n$  and their blends as PCMs. To bring-about their PCM design highlights, the data in the following tables are thus chosen along certain basic concepts regarding: microcapsules synthesis methods, microcapsules modification methods, and the multinary core or shell materials respectively.

- In regard to the synthesis methods of microcapsules. There are many different synthesis methods of microcapsules, which need various chemical reagents, such as initiator, cross-linking agent, nucleating agent, monomer, surfactant, emulsifier, among others. The different mass fraction of these chemical reagents will cause various core-shell ratio, shell morphology, encapsulation efficiency (section 3.3.3.2), among others. In this situation, the information of microencapsulation with highest encapsulation efficiency are chosen and listed in the tables. Normally, the highest encapsulation efficiency microcapsules also have highest enthalpy of melting and crystallization for the same core in most of studies.
- In regard to the modification of microcapsules. For instance, nano-particles can be used to enhance the shell/core thermal conductivities or to intensify the strength of shell structure; graphene oxide can be used to prevent the leakage of microencapsulation, among others. In this circumstance, the information of microcapsules with and without modified materials are listed in the tables.
- In regard to the multinary core or shell materials. Some literatures presented the microencapsulation with multi-compositions core or shell. In this situation, all the combinations are listed in the tables.

#### 3.1.1 $C_n$ and modified $C_n$ microcapsules

Table 4. Characterization	n of C <sub>n</sub> and modified	C <sub>n</sub> microcapsules	(NA: not available)
---------------------------	----------------------------------	------------------------------	---------------------

She	11	Core	Crysta	llization	Me	lting	$E_{en}$ & $E_{es}$	λ	Synthesis method	Re
Components <sup>4</sup>	WR (w/w%)	Components	FP (°C)	LH (J/g)	MP (°C)	LH (J/g)	(%)	$(W/m \cdot K)$	Synthesis method	ĸ
MF		C <sub>12</sub>	-29.30	187.2	-7.80	187.2	90.0	NA	in-situ polymerization	71
AS		C <sub>14</sub>	e1.98	111.0	<sup>e</sup> 6.02	113.5	70.2	NA	phase separation	72
ABS			<sup>e</sup> 1.37	104.8	<sup>e</sup> 5.91	107.1	66.3			
PC			°2.23	110.9	<sup>e</sup> 7.16	113.2	74.7			
PUF		C <sub>14</sub>	2.81	134.5	9.01	134.2	61.8	NA	in-situ polymerization	73
PS-co-EA	NA	C <sub>14</sub>	-0.18	184.9	7.97	182.7	79.3	NA	emulsion polymerization	74
SiO <sub>2</sub>		C <sub>14</sub>	<sup>e</sup> -0.39	139.9	<sup>e</sup> 2.39	140.1	62.0	0.1250~ 0.1510	interfacial polymerization	75
CaCO <sub>3</sub>		C <sub>14</sub>	<sup>e</sup> 1.58	58.2	°5.35	58.5	<sup>es</sup> 25.9	0.4920~ 0.6500	self-assembly	76
PMMA-co-PUF	28.8:71.2	C <sub>14</sub>	3.70	183.2	9.60	185.9	87.5	NA	in-situ polymerization	77
PMMA			2.80	133.8	8.10	133.6	63.4			
PUF			3.30	159.5	8.30	171.8	78.5			
PMMA		C <sub>15</sub>	<sup>e</sup> 6.10	<sup>e</sup> 119.0	10.00	107.0	NA	NA	suspension polymerization	78
PS-co-EA	NA	C <sub>15</sub>	5.20	127.9	11.60	121.8	69.2	NA	emulsion polymerization	74
PFR		C <sub>16</sub>	3.91	96.5	17.29	98.1	38.0	NA	phase separation	79
PS		C <sub>16</sub>	NA	NA	22.74	80.3	NA	NA	suspension polymerization	80
GA-co-GEL	NA	C <sub>16</sub>	NA	NA	21.00	144.7	NA	NA	complex coacervation	81
PMMA		C <sub>16</sub>	14.85	128.2	17.34	145.6	61.4	NA	emulsion polymerization	82
PBA		C <sub>16</sub>	14.54	120.6	16.58	120.2	50.7	NA	emulsion polymerization	83
PMMA		C <sub>16</sub>	12.60	100.0	21.60	96.0	NA	NA	suspension polymerization	84
					16					

PODMMA			21.40	109.0	19.50	108.0	NA		
EC		C <sub>16</sub>	19.51	147.1	15.25	140.8	71.7	NA	emulsion polymerization
PS/GO	NA	C <sub>16</sub>	10.60	190.5	24.90	183.1	<sup>es</sup> 78.5	NA	emulsion polymerization
PS-co-EA	NA	C <sub>16</sub>	17.23	149.6	24.04	140.5	81.6	NA	emulsion polymerization
MUF		C <sub>16</sub>	7.70	169.8	14.70	167.4	<sup>es</sup> 84.7	0.0530	emulsion polymerization
MUF/GP	99.3:0.7		10.70	155.3	15.90	154.2	<sup>es</sup> 77.8	<sup>e</sup> 0.1030	
MUF/GP	98.7:1.3		NA	138.3	15.80	136.5	<sup>es</sup> 69.1	0.1540	
MUF/GP	97.4:2.6		NA	103.6	14.60	104.7	<sup>es</sup> 52.2	<sup>e</sup> 0.1650	
PUF		C <sub>16</sub>	10-12	87-116	20-23	86-115	NA	0.0557	interfacial polymerizatio
PUF/Ag NPs	93.4:6.6		10-12	73-94	19-23	83-105	NA	0.0663	
PUF/Ag NPs	87.7:12.3		4-12	76-131	22-26	73-137	NA	0.0664	
PUF/Ag NPs	78.1:21.9		7-13	70-89	21-23	71-89	NA	0.1231	
MMA-co-AA	NA	C <sub>16</sub>	15.30	79.6	16.20	84.5	25.6	NA	emulsion polymerization
PMMA		C <sub>16</sub>	8.60	NA	18.30	62.9	28.9	NA	suspension polymerization
BA-co-MMA	NA		7.60	NA	19.40	63.1	28.9	NA	
PMMA		C <sub>17</sub>	18.40	84.2	18.20	81.5	38.0	NA	emulsion polymerization
PS-co-EA	NA	C <sub>17</sub>	17.23	149.6	24.04	140.5	81.6	NA	emulsion polymerization
SiO <sub>2</sub>		C <sub>17</sub>	16.15	61.4	21.90	60.3	30.9	NA	sol-gel process
MF		C <sub>18</sub>	28.70	145.0	40.60	144.0	59.0	NA	in-situ polymerization
PUF		C <sub>18</sub>	26.5-17.7	17.4	26.0-33.0	18.8	NA	NA	in-situ polymerization
TiO <sub>2</sub>		C <sub>18</sub>	21.00	92.0	28.70	97.0	NA	NA	spraying
GA-co-GEL	NA	C <sub>18</sub>	NA	NA	30.30	165.8	NA	NA	complex coacervation
MF		C <sub>18</sub>	23.14	149.2	26.91	146.5	<sup>es</sup> 69.0	NA	in-situ polymerization
PU		C <sub>18</sub>	27.04	188.9	22.82	187.9	88.0	NA	interfacial polymerizatio
PU		C <sub>18</sub>	22.60	187.9	27.00	188.9	88.0	NA	interfacial polymerization

PMF			23.10	149.2	26.90	146.5	68.3	NA	in-situ polymerization
SiO <sub>2</sub>		C <sub>18</sub>	22.10	185.6	27.10	184.9	85.9	0.4568	sol-gel process
SiO <sub>2</sub>		C <sub>18</sub>	22.00	NA	27.10	NA	NA	0.3290	interfacial polymerization
St-co-DVB	90.7:9.3	C <sub>18</sub>	16.00	127.0	29.00	125.0	56.8	NA	suspension polymerization
PEMA		C <sub>18</sub>	29.80	197.1	32.70	198.5	89.5	0.1600	emulsion polymerization
PMMA			30.20	205.9	31.90	208.7	94.7	0.1400	
PMMA		C <sub>18</sub>	18.30	174.4	36.80	173.7	<sup>es</sup> 77.3	NA	suspension polymerization
PDVB		C <sub>18</sub>	19.00	220.0	29.00	220.0	NA	NA	suspension polymerization
PMMA		C <sub>18</sub>	4.50	182.8	35.20	156.4	<sup>es</sup> 75.3	NA	suspension polymerization
PU		C <sub>18</sub>	25.19	°159.5	28.61	<sup>e</sup> 159.1	NA	NA	in-situ polymerization
PU/Fe <sub>3</sub> O <sub>4</sub>	NA		26.16	<sup>e</sup> 169.7	28.81	<sup>e</sup> 165.7	NA		
MMA-co-AMA	90.9:9.1	C <sub>18</sub>	10.60	50.0	27.80	68.5	30.9	NA	in-situ polymerization
BMA-co-MAA	NA	C <sub>18</sub>	<sup>e</sup> 23.85	125.8	<sup>e</sup> 21.85	130.3	<sup>es</sup> 56.9	NA	suspension polymerization
PBA		C <sub>18</sub>	13.40	123.7	31.60	126.4	<sup>es</sup> 55.6	NA	suspension polymerization
PBMA			16.60	124.6	29.10	120.3	<sup>es</sup> 54.4		
CaCO <sub>3</sub>		C <sub>18</sub>	23.43	82.2	29.19	84.4	40.4	1.2640	self-assembly
SiO <sub>2</sub>		C <sub>18</sub>	23.72	84.9	27.96	87.6	41.8	0.8910	sol-gel process
BMA-co-BA	57.1:42.9	C <sub>18</sub>	12.90	125.5	30.90	116.4	<sup>es</sup> 53.7	NA	suspension polymerization
BMA-co-BA-co-MAA	57.1:28.6:14.3		11.70	130.0	30.90	136.3	<sup>es</sup> 59.2	NA	
BMA-co-MAA	57.1:42.9		12.30	152.9	32.80	144.3	<sup>es</sup> 66.0	NA	
BMA-co-AA	57.1:42.9		16.60	143.0	27.60	141.5	<sup>es</sup> 63.2	NA	
PSMA		C <sub>18</sub>	21.50	94.8	21.80	87.9	<sup>es</sup> 40.6	NA	suspension polymerization
PMMA		C <sub>18</sub>	22.60	90.0	29.00	91.0	NA	NA	suspension polymerization
PODMMA			22.80	100.0	28.20	98.0	NA		
PODMAA		C <sub>18</sub>	15.40	90.0	31.50	91.0	26.0	NA	suspension polymerization

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PDDA		C <sub>18</sub>	25.82	124.4	27.34	124.4	<sup>es</sup> 58.0	NA	self-assembly
MPS-co-VTMS	25:75	C <sub>18</sub>	17.42	169.4	27.84	166.7	<sup>es</sup> 76.0	NA	self-assembly
PAA		C <sub>18</sub>	26.50	126.0	31.80	125.0	NA	NA	spraying
PLMA		C <sub>18</sub>	10.60	108.9	28.60	118.0	<sup>es</sup> 50.4	NA	suspension polymerization
PU		C <sub>18</sub>	19.40	173.2	28.60	170.4	66.7	NA	interfacial polymerization
SiO <sub>2</sub>		C <sub>18</sub>	24.27	72.2	32.56	73.5	35.6	NA	sol-gel process
PMMA		C <sub>18</sub>	13.20	153.7	24.92	132.1	<sup>es</sup> 78.0	NA	suspension polymerization
PMMA:UM-Si <sub>3</sub> N <sub>4</sub>	76.9:23.1		13.60	140.3	25.24	139.2	<sup>es</sup> 76.3		
PMMA:M-Si <sub>3</sub> N <sub>4</sub>	97.1:2.9		15.24	151.3	24.54	150.3	<sup>es</sup> 82.3		
PMMA:M-Si <sub>3</sub> N <sub>4</sub>	94.3:5.7		14.69	150.5	24.31	146.9	<sup>es</sup> 81.1		
PMMA:M-Si <sub>3</sub> N <sub>4</sub>	87:13		16.37	138.2	24.27	143.0	<sup>es</sup> 76.7		
PMMA:M-Si <sub>3</sub> N <sub>4</sub>	76.9:23.1		16.14	122.1	25.33	121.11	<sup>es</sup> 66.4		
PUF		C <sub>18</sub>	20-22	91-115	30-34	94-117	NA	0.0695	interfacial polymerization
PUF/Ag NPs	94.1:5.9		18-22	142-168	33-36	143-168	NA	0.0978	
MMA-co-AA		C <sub>18</sub>	25.90	84.4	26.40	86.1	34.7	NA	emulsion polymerization
OSi		C <sub>18</sub>	24.58	102.0	27.92	107.5	51.3		interfacial polymerization
SiO <sub>2</sub>		C <sub>18</sub>	24.17	98.85	27.35	109.5	51.5	0.4483	interfacial polymerization
SiO <sub>2</sub>		C <sub>18</sub>	26.22	226.3	28.32	227.7	NA	NA	sol-gel process
TiO <sub>2</sub>		C <sub>18</sub>	15.28	40.7	25.68	42.8	22.5	NA	sol-gel process
PMMA/SiO <sub>2</sub>	66.7:33.3	C <sub>18</sub>	13.66	131.4	24.30	129.8	66.4	NA	emulsion polymerization
PU/PUT	NA	C <sub>18</sub>	23.20	141.0	28.60	143.0	NA	NA	interfacial polymerization
PU			24.00	130.0	27.90	133.0	NA		
PUF		C <sub>18</sub>	20.40	175.0	30.70	176.0	81.0	NA	in-situ polymerization
MF		C <sub>18</sub>	<sup>e</sup> 21.00	137.2	NA	NA	67.5	NA	in-situ polymerization
PMMA/TiO <sub>2</sub>	97.2:2.8	C <sub>18</sub>	20.65	139.3	24.60	139.9	<sup>es</sup> 67.6	NA	suspension polymerization

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PMMA			20.56	148.3	24.99	153.8	<sup>es</sup> 73.2			
MMA-co-MPS	75:25	C <sub>18</sub>	16.91	166.1	26.20	165.3	74.9	NA	suspension polymerization	1
MF		C <sub>18</sub>	25.26	137.9	28.22	137.1	59.3	NA	in-situ polymerization	1
MF/CNT-PSS	NA	C <sub>18</sub>	18.81	207.4	29.85	211.2	<sup>es</sup> 80.1	0.2500	self-assembly	1
MF			18.86	218.5	30.32	222.0	<sup>es</sup> 84.2	0.1900		
MMA-co-MAA	NA	C <sub>18</sub>	26.40	87.7	27.30	94.2	NA	NA	emulsion polymerization	1
PMMA/PIM	95.9:4.1	C <sub>18</sub>	15.16	129.5	24.73	129.7	66.4	NA	suspension polymerization	
PMMA			14.89	152.6	24.89	149.2	76.3			
PMMA		C <sub>18</sub>	14.90	125.0	22.80	123.0	55.4	NA	emulsion polymerization	
PAMA		C <sub>18</sub>	11.40	106.6	31.80	104.8	51.3	NA	suspension polymerization	
SF		C <sub>18</sub>	14.74	90.2	22.82	88.2	46.7	NA	self-assembly	
SF		C <sub>18</sub>	<sup>e</sup> 18.50	<sup>e</sup> 70.0	<sup>e</sup> 22.50	<sup>e</sup> 68.0	NA	NA	self-assembly	
GA-co-GEL	NA	C <sub>19</sub>	NA	NA	34.00	44.1	NA	NA	complex coacervation	
PMMA		C <sub>19</sub>	31.03	142.9	31.23	139.2	60.3	NA	emulsion polymerization	
SA		C <sub>19</sub>	18.52	81.9	32.10	81.7	56.0	NA	electro spraying	
SA		C <sub>19</sub>	28.76	120.9	35.65	107.3	84.3	NA	electro spraying	
SiO <sub>2</sub>		C <sub>19</sub>	26.24	80.8	36.89	74.8	41.1	NA	sol-gel process	
PMMA		C <sub>20</sub>	34.90	87.5	35.20	84.2	35.0	NA	emulsion polymerization	
EC-co-MC	90.9:9.1	C <sub>20</sub>	30.60	186.1	38.00	202.4	90.0	NA	self-assembly	
PSX		C <sub>20</sub>	<sup>e</sup> 30.34	<sup>e</sup> 88.8	<sup>e</sup> 39.37	<sup>e</sup> 160.4	NA	NA	emulsion polymerization	
Fe <sub>3</sub> O <sub>4</sub> /SiO <sub>2</sub>	NA	C <sub>20</sub>	33.42	169.6	39.15	170.2	71.8	NA	self-assembly	
CaCO <sub>3</sub>		C <sub>20</sub>	33.22	85.4	37.29	86.1	37.9	1.0570	self-assembly	
PMMA		C <sub>20</sub>	32.70	111.0	40.20	110.0	NA	NA	suspension polymerization	
PODMMA			31.40	110.0	39.20	113.0	NA			
MF		C <sub>20</sub>	33.60	162.4	38.40	166.6	NA	NA	emulsion polymerization	

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TiO <sub>2</sub>		C <sub>20</sub>	36.29	150.9	42.73	152.5	78.0	0.7490	sol-gel process
ZnO		C <sub>20</sub>	<sup>e</sup> 30.70	135.6	39.80	136.4	<sup>e</sup> 69.5	NA	in-situ polymerization
SiO <sub>2</sub>		C <sub>20</sub>	31.86	78.6	40.48	81.2	33.0	NA	sol-gel process
ZrO <sub>2</sub>		C <sub>20</sub>	36.74	121.3	43.59	126.5	64.7	NA	self-assembly
MMA-co-AA	NA	C <sub>20</sub>	33.80	88.4	31.70	90.9	32.9	NA	emulsion polymerization
TiO <sub>2</sub> /Fe <sub>3</sub> O <sub>4</sub>	NA	C	32.40	144.2	38.60	144.7	53.8	NA	self-assembly and
$110_{2}/12_{3}0_{4}$	INA	C <sub>20</sub>	32.40	144.2	38.00	144./	55.8	INA	interfacial polymerization
ZrO <sub>2</sub>		C <sub>20</sub>	39.37	158.4	45.25	163.9	64.5	0.9060	in-situ polymerization
Cu <sub>2</sub> O		C <sub>20</sub>	32.52	163.1	38.71	165.3	61.6	3.6520	self-assembly
TiO <sub>2</sub> /GP	NA	C <sub>20</sub>	e33.00	<sup>e</sup> 168.0	<sup>e</sup> 40.90	<sup>e</sup> 170.0	NA	<sup>e</sup> 0.7000	interfacial polymerizatio
TiO <sub>2</sub>			<sup>e</sup> 32.10	<sup>e</sup> 162.0	<sup>e</sup> 40.95	<sup>e</sup> 164.0	NA	<sup>e</sup> 0.6500	
MMA-co-MAA	NA	C <sub>20</sub>	35.50	101.4	36.30	107.7	NA	NA	emulsion polymerization
Ag/SiO <sub>2</sub>	NA	C <sub>20</sub>	<sup>e</sup> 31.02	<sup>e</sup> 166.5	<sup>e</sup> 40.86	<sup>e</sup> 168.2	NA	NA	interfacial polymerizatio
CNP/GEL/SA	NA	C <sub>20</sub>	32.37	105.1	35.42	114.7	41.5	NA	complex coacervation
Ch/CNP	NA	C <sub>20</sub>	32.76	114.5	35.53	120.5	43.6	NA	complex coacervation
PMMA		C <sub>21</sub>	39.59	137.9	39.24	138.2	NA	0.1800	emulsion polymerization
PMMA		C <sub>22</sub>	40.60	48.7	41.00	54.6	28.0	NA	emulsion polymerization
PUT		C <sub>22</sub>	34.00	88.0	42.00	79.0	31.6	NA	interfacial polymerizatio
Fe <sub>3</sub> O <sub>4</sub> /SiO <sub>2</sub>	NA	C <sub>22</sub>	40.00	156.3	44.90	157.6	NA	NA	interfacial polymerizatio
PMMA		C <sub>28</sub>	53.20	88.5	50.60	86.4	43.0	NA	emulsion polymerization
PMMA		C <sub>28</sub>	60.66	156.1	60.02	152.5	NA	0.2000	emulsion polymerization
PS		C <sub>32</sub>	61.80	174.8	70.90	285.5	<sup>es</sup> 61.2	NA	emulsion polymerization

<sup>4</sup> Melamine-Formaldehyde (MF); Acrylonitrile-styrene copolymer (AS); Acrylonitrile-styrene-butadiene copolymer (ABS); Polycarbonate (PC); Poly(urea-formaldehyde) (PUF); Styrene-co-Ethylacrylate (PS-co-EA); Poly(methyl methacrylate) (PMMA); Phenolic resin (PFR); Polystyrene (PS); Gum arabic (GA); Gelatin (GEL); Gum arabic-co-Gelatin (GA-co-GEL); Poly(butyl acrylate) (PBA); Poly(butyl methacrylate) (PBMA); Poly(n-octadecyl acrylate-methyl methacrylate) (PODMMA); Ethyl

cellulose (EC); Graphene oxide (GO); Melamine-urea-formaldehyde (MUF); Graphene (GP); Nano particles (NPs); Poly(methyl methacrylate-co-acrylic acid) (MMA-co-AA); Poly(butyl acrylate-co-methyl methacrylate) (BA-co-MMA); Polyurea (PU); Polymelamine-Formaldehyde (PMF); Styrene-divinybenzene (St-co-DVB); Poly(ethyl methacrylate) (PEMA); Poly(divinybenzene) (PDVB); Poly(methyl methacrylate-co-allyl methacrylate) (MMA-co-AMA); Poly(n-butyl methacrylate-co-butyl acrylate-co-methacrylic acid) (BMA-co-MAA); Poly(n-butyl methacrylate-co-butyl acrylate-co-butyl acrylate-co-methacrylic acid) (BMA-co-MAA); Poly(n-butyl methacrylate-co-butyl acrylate) (BMA-co-AA); Poly(n-butyl methacrylate-co-methacrylic acid) (BMA-co-MAA); Poly(n-butyl methacrylate-co-acrylic acid) (BMA-co-AA); Poly(stearyl methacrylate) (PSMA); Poly(n-octadecyl methacrylate-co-methacrylic acid) (PODMAA); Poly(diallyldimethylammonium chloride) (PDDA); 3-(trimethoxysilyl) propyl methacrylate-co-vinyltrimethoxysilane (MPS-co-VTMS); Polyamic acid (PAA); Poly(lauryl methacrylate) (PLMA); Unmodified Si<sub>3</sub>N<sub>4</sub> (UM-Si<sub>3</sub>N<sub>4</sub>); Modified Si<sub>3</sub>N<sub>4</sub> (M-Si<sub>3</sub>N<sub>4</sub>); Organosilica (OSi); Polyurethane (PUT); Poly(methyl methacrylate-co-3-(trimethoxysilyl) propyl methacrylate) (PIMA); Poly(Allyl methacrylate) (PAMA); Silk fibroin (SF); Sodium alginate (SA); Ethyl cellulose-co-methyl cellulose (EC-co-MC); Polysiloxane (PSX); Clay nano-particles (CNP); Chitosan (Ch)

<sup>e</sup> data extracted from the figures in literatures

<sup>es</sup>  $E_{es}$  data from the literature according to Eq.(3) in Section 3.3.2.2

#### 3.1.2 Paraffins microcapsules

#### Table 5. Characterization of Paraffins microcapsules (NA: not available)

Shell		Core	Crystall	lization	Mel	ting	$E_{en}$ &	λ	Synthesis method	R
Components <sup>5</sup>	WR (w/w%)	Components	FP (°C)	LH (J/g)	$MP(^{\circ}C)$	LH (J/g)	$E_{es}$ (%)	$(W/m \cdot K)$	Synthesis method	К
PS		Paraffin	NA	NA	<sup>e</sup> 42.04	<sup>e</sup> 41.7	20.6	NA	suspension polymerization	164
PUF		Paraffin	50.40	201.2	53.30	200.4	97.9	NA	in-situ polymerization	165
SiO <sub>2</sub>		Paraffin	58.27	107.1	58.37	165.7	87.5	NA	sol-gel method	166
St-co-MMA	20:80	Paraffin	NA	NA	<sup>e</sup> 41.81	<sup>e</sup> 83.7	43.2	NA	suspension polymerization	167
PMMA		Paraffin	NA	NA	28.00	101.0	61.2	NA	emulsion polymerization	168
PMMA		Paraffin	50.10	112.3	55.80	106.9	66.0	NA	self-assembly	169
MF/nano-Al <sub>2</sub> O <sub>3</sub>	100:0	Paraffin	47.3-28.7	106.5	33.6-54.1	112.7	<sup>es</sup> 65.9	NA	in-situ polymerization	170
	92.3:7.7		49.1-31.8	110.6	36.9-55.5	115.3	<sup>es</sup> 68.0			
	88.9:11.1		48.4-31.9	87.9	37.4-56.1	98.3	<sup>es</sup> 59.0			
	78.9:21.1		43.1-26.1	89.4	38.7-60.2	101.4	<sup>es</sup> 57.4			
	71.4:28.6		43.2-26.2	88.5	38.6-59.9	94.4	<sup>es</sup> 55.0			
	65.2:34.8		42.6-25.2	79.1	39.9-61.6	84.1	<sup>es</sup> 49.1			
MMA-co-AA	NA	Paraffin	NA	NA	60.00	113.0	NA	NA	emulsion polymerization	171
SiO <sub>2</sub>		Paraffin	45.00	43.8	56.50	45.5	31.7	NA	in-situ polymerization	172
PMMA		Paraffin	NA	NA	<sup>e</sup> 61.5	<sup>e</sup> 140.3	60.7	NA	emulsion polymerization	173
PAM		Paraffin	14-31	121.7	29-41	122.1	87.0	NA	interfacial polymerization	174
SiO <sub>2</sub>		Paraffin	55.78	144.1	57.96	156.9	82.2	NA	sol-gel process	175
PLA		Paraffin	50.20	170.5	58.20	176.6	NA	NA	emulsion polymerization	176
BMA-co-MAA	NA	Paraffin	<sup>e</sup> 50.85	<sup>e</sup> 102.0	<sup>e</sup> 53.85	°99.0	<sup>es</sup> 69.9	NA	suspension polymerization	108
		Paraffin	56.80	147.2	58.60	164.1	87.1	NA	sol-gel process	177
TiO <sub>2</sub>										

		Paraffin	48.90	98.2	56.32	94.3	NA	<sup>e</sup> 0.2530		
		Paraffin	49.39	91.3	56.29	85.7	NA	<sup>e</sup> 0.3100		
		Paraffin	49.69	87.4	55.85	83.28	NA	<sup>e</sup> 0.3180		
PAn		Paraffin	48.95	121.0	56.63	108.9	79.9	NA	in-situ polymerization	179
PUF		Paraffin	NA	NA	26.10	74.2	52.8	NA	in-situ polymerization	180
PUF		Paraffin	NA	NA	26.20	47.7	37.4	NA	in-situ polymerization	18
MAA-co-EMA	57.1:42.9	Paraffin	26.30	103.2	29.30	102.9	<sup>es</sup> 62.6	NA	suspension polymerization	18
PLMA		Paraffin	23.04	73.0	29.50	76.7	<sup>es</sup> 45.5	NA	suspension polymerization	118
SiO <sub>2</sub>		Paraffin	23.29	110.8	26.12	111.7	61.9	0.3948	self-assembly	18
PHEMA		Paraffin	48.06	167.3	57.88	168.0	97.7	NA	redox polymerization	18
PS-co-EA	NA	Paraffin	37.41	49.1	42.39	49.0	32.1	NA	emulsion polymerization	18
SiO <sub>2</sub>		Paraffin	57.40	83.1	49.20	89.7	<sup>es</sup> 50.8	NA	emulsion polymerization	18
SiO <sub>2</sub> /GO	NA		57.70	81.6	49.70	87.1	<sup>es</sup> 49.6			
PMMA:SiO <sub>2</sub>	NA	Paraffin	19.80	71.0	26.80	69.9	<sup>es</sup> 57.4	NA	self-assembly	18
MF/GO	NA	Paraffin	NA	NA	41.08	202.8	93.9	NA	in-situ polymerization	18
MF			NA	NA	39.85	200.3	92.7			
St-co-AA-co-BA	NA	Paraffin	<sup>e</sup> 13.80	<sup>e</sup> 109.7	<sup>e</sup> 20.80	<sup>e</sup> 112.1	NA	NA	in-situ polymerization	18
MF		Paraffin	NA	NA	47.66	126.0	65.0	NA	in-situ polymerization	19
MF/GP	NA	Paraffin	57.10	85.0	50.50	90.8	51.1	0.3120	in-situ polymerization	19
MF			57.10	94.9	49.90	102.9	57.5	0.2610		
PMMA/(BN/TiO <sub>2</sub> )	66.7:33.3	Paraffin	51.60	141.5	53.00	140.8	72.1	0.3527~ 0.4419	emulsion polymerization	19
PMMA		Paraffin	NA	NA	59.90	137.2	89.5	NA	suspension polymerization	19
SiO <sub>2</sub>		Paraffin	NA	NA	49.00	13.0	11.0	NA	interfacial polymerization	194
PS-co-MAA	NA	Paraffin	49.25	94.7	51.48	96.0	<sup>es</sup> 69.5	NA	emulsion polymerization	195

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EMA-co-AA-co-St-co-T MPTA	NA	Paraffin	24.90	115.3	30.70	117.8	<sup>es</sup> 70.8	NA	suspension polymerization	19
PU		Paraffin	NA	NA	27.5	92.5	44.5	NA	interfacial polymerization	1
MR		Paraffin	NA	NA	39.8	92.2	NA	<sup>e</sup> 0.1880~ 0.2660	purchased	1
MMA-co-MA/Al <sub>2</sub> O <sub>3</sub> NPs	90.9:9.1	Paraffin	22.54	110.0	22.47	110.4	64.3	0.2442	emulsion polymerization	1
			23.19	104.3	23.43	105.5	61.2	0.2786		
			23.32	92.4	23.75	93.4	54.2	0.3104		
			22.76	84.0	23.14	84.5	49.2	0.3409		
			22.03	75.5	23.49	76.3	44.3	0.3591		
			22.58	75.1	22.96	75.4	43.9	0.3816		
PMMA		RT21	8.0	111.9	21.90	113.4	85.6	NA	suspension polymerization	2
PMMA		RT21	7.90	111.9	22.00	113.9	86.3	NA	suspension polymerization	2
PMMA		RT25	NA	NA	20.73	113.9	NA	NA	suspension polymerization	2
LDPE-co-EVA	NA	RT27	NA	NA	28.40	98.1	49.3	NA	spray drying	2
PMMA		RT27	<sup>e</sup> 7.50	167.0	e22.00	163.2	NA	NA	suspension polymerization	2
CaCO <sub>3</sub>		RT28	27.41	107.2	23.33	105.8	59.0	0.714	self-assembly	2
CaCO <sub>3</sub>		RT42	49.36	137.8	49.41	138.7	58.2	0.817		
CaCO <sub>3</sub>		RT42	NA	NA	48.62	143.6	NA	0.814	self-assembly	2
St-co-BA	70:30	RT80	55.20	25.0	80.90	23.9	<sup>es</sup> 80.0	NA	emulsion polymerization	2

<sup>5</sup> Styrene-co-methyl methacrylate (St-co-MMA); Polyamide (PAM); Polylactic acid (PLA); Polyaniline (PAn); Poly(methacrylic acid-co-ethyl methacrylate) (MAA-co-EMA); Poly(2-hydroxyethyl methacrylate) (PHEMA); Styrene-co-acrylic acid-co-n-butyl acrylate (St-co-AA-co-BA); Boron nitride (BN); Ploy(styrene -co-methylacrylic acid) (PS-co-MAA); Poly(ethyl methacrylate-co- acrylic acid-co-styrene-co-trimethylolpropane triacrylate) (EMA-co-AA-co-St-co-TMPTA); Melamine resin (MR); Poly(Methyl methacrylate-co-methacrylate) (MMA-co-MA); Poly(Styrene-co-butyl acrylate) (St-co-BA); Carbon nanofibers (CNFs)

<sup>e</sup> data extracted from the figures in literatures

<sup>es</sup>  $E_{es}$  data from the literature according to Eq.(3) in Section 3.3.2.2

#### 3.1.3 $C_n$ & paraffin blends microcapsules

Table 6. Characterization of	C <sub>n</sub> & paraffin blends n	nicrocapsules (NA: not available)
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\_\_\_\_\_

Shell	Cor	e	Crystall	ization	Melt	ing	$E_{en}$ & $E_{es}$	λ		
Components	Components	WR (w/w%)	FP (°C)	LH (J/g)	MP (°C)	LH (J/g)	(%)	κ (W/m·K)	Synthesis method	Ref.
PUF	C <sub>16</sub> :C <sub>20</sub>	66:34	24.5-12.0	54.8	9.0-23.5	51.7	NA	NA	in-situ polymerization	94
PMMA	C <sub>17</sub> :C <sub>24</sub>	90:10	20.14	83.8	20.22	86.0	50.2	NA	emulsion polymerization	208
	C <sub>18</sub> :C <sub>19</sub>	95:5	26.44	112.3	26.45	117.9	65.3			
	C <sub>19</sub> :C <sub>24</sub>	95:5	30.96	99.0	31.22	104.9	55.8			
	C <sub>20</sub> :C <sub>24</sub>	90:10	35.75	165.5	35.88	169.3	65.4			
PS	C <sub>18</sub> :C <sub>24</sub>	90:10	16.48	152.8	25.96	156.4	64.4	NA	emulsion polymerization	209
MF	C <sub>18</sub> :C <sub>20</sub>	66.7:33.3	NA	NA	33.00	144.0	NA	NA	in-situ polymerization	210
PU	Paraffin (solid:liquid)	30:70	NA	NA	28.10	58.4	NA	NA	interfacial polymerization	211
LDPE-co-EVA	RT27:CNFs	98:2			27.60	95.6	48.1	NA	spray drying	203
MMA	RT21:RT58	95:5	17.51	108.3	22.28	110.4	83.6	NA	suspension polymerization	212
CaCO <sub>3</sub>	RT28:RT42	50:50	27.67; 40.62	122.8	19.76; 34.76	82.8	57.4	0.701	self-assembly	205

#### 3.1.4 Microencapsulation of $C_n$ mixed with other compositions

Table 7. Characterization of microencapsulation of C<sub>n</sub> mixed with other compositions (NA: not available)

Shell		Core		Crystal	lization	Me	lting	E & E	λ		
Components <sup>6</sup>	WR (w/w%)	Components	WR (w/w%)	FP (°C)	LH (J/g)	MP (°C)	LH (J/g)	E <sub>en</sub> & E <sub>es</sub> (%)	(W/m∙ K)	Synthesis method	Ref.
EP		C <sub>14</sub> :DMB	50:50	<sup>e</sup> -4.50	NA	<sup>e</sup> 5.50	54.7	42.1	NA	interfacial polymerization	213
PUF		C18:PEG600	13:87	27.0-25.2	1.6	26.0-32.5	3.9	NA	NA	in-situ polymerization	94
		C <sub>16</sub> :PEG1000: Na <sub>2</sub> CO <sub>3</sub> ·10H <sub>2</sub> O	11:50:39	15.8-13.4	42.5	13.0-23.5	44.6	NA			
MMA-co-AMA	90.9:9.1	C <sub>18</sub> :PPy	89.4:10.6	11.70	29.2	28.2	141.4	63.7	NA	in-situ polymerization	107
PU/PUT	NA	Paraffin:BS	90.9:9.1- 66.7:33.3	NA	NA	28-35	58.1-87.6	42.2-63.7	NA	interfacial polymerization	214
MMA-co-DVB	95:5	Paraffin:BS	90:10	28.17	33.3	34.7	117.5	85.2	NA	in situ polymerization	215
PU/PUT	NA	Paraffin:BS	83.3:16.7	NA	NA	33.70	82.6	59.4	NA	interfacial polymerization	216
			50:50	NA	NA	32.29	80.1	58.2			
			66.7:33.3	NA	NA	32.51	72.4	55.0			
DVB-co-AMA	50:50	Paraffin:BS	50:50	NA	NA	32.12	94.0	68.3	NA	suspension polymerization	217
PU		C <sub>18</sub> : 1-tetradecanol	92.9:7.1	22.40	164.4	30.20	165.5	NA	NA	interfacial polymerization	119
		C <sub>18</sub> :paraffin	98.3:1.7	17.50	159.9	28.10	161.9	NA			
SiO <sub>2</sub>		Paraffin: P(GMA-EDMA)	NA	°53.5	<sup>e</sup> 78.0	°55.5	°78.8	NA	NA	sol-gel process	218

<sup>6</sup> Epoxy polymer (EP); Dimethylbenzene (DMB); polypyrrole (PPy); poly(glycidylmethacrylate-ethylene dimethacrylate) (P(GMA-EDMA)); Butyl stearate (BS);

poly(methylmethacrylate-co-divinylbenzene) (MMA-co-DVB); poly(divinylbenzene-co- allyl methacrylate) (DVB-co-AMA)

<sup>e</sup> data extracted from the figures in literatures

#### 3.2 Synthesis methods for C<sub>n</sub> and their blends microcapsules

In this sub-section, a brief description of each synthesis method (as mentioned in Table 4-7) is summarized firstly. Then, some typical examples in regard to these methods are elaborated.

Normally, the commonly used synthetic techniques for  $C_n$  and their blends microcapsules can be classified under three categories: physical, chemical and physical-chemical methods. Apart from these technologies, other methods such as self-assembly, also exist in some literatures.

#### 3.2.1 Physical methods

The physical method retains the original chemical compositions of the shell materials, which are formed by physical processes like dehydration, adhesion, among others.

In many physical methods, Electrospraying, as the most commonly used method for microcapsules synthesis, is introduced in this sub-section.

#### Electrospraying

- General processes<sup>117</sup>: (1) preparing the PCM solution and shell material solution in two separate syringes;
   (2) two separated solutions are fed into different nozzles (outer and inner nozzle) at the particular feed rates;
   (3) the fabricated microcapsules are collected in a container and gently stirred for curing;
   (4) washing and drying the microcapsules.
- A typical example: Figure 6 shows the schematic of microencapsulation using electrospraying method according to Yuan et al.'s work <sup>117</sup>. At first, PAA solution and liquid  $C_{18}$  were placed in two separate plastic syringes, and then injected into the coaxial composite nozzle. The PAA solutions were extruded through outer nozzle while the  $C_{18}$  solutions were came out through the inner nozzle. Finally, the fabricated microcapsules were dripped into a container, washed and dried. The diameters of microcapsules ranged from 0.5 to 3  $\mu$ m.

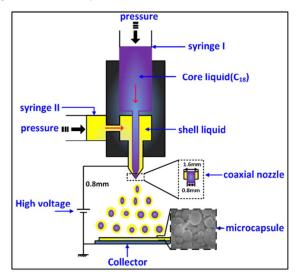


Figure 6 Schematic of electrospraying method for the  $C_{18}$  microencapsulation (redrawn based on Ref. <sup>117</sup>) 3.2.2 Chemical method

Generally, there are 4 types of polymerization processes namely in-situ polymerization, interfacial polymerization, suspension polymerization and emulsion polymerization, which are described below.

#### 3.2.2.1 In-situ polymerization

- General processes <sup>71</sup>: (1) the synthesis of the pre-polymer solution through the mixture of pre-polymers (shell materials) and solvents (water); (2) preparation of oil/water (O/W) emulsion with emulsifier (sometimes modifying agent); (3) microcapsules formation by adding this pre-polymer into the O/W emulsion; (4) microcapsules collection by rinsing, filtering and drying. This method is typically used for organic shell materials like MF and PUF.
- A typical example: Figure 7 shows the schematic of microencapsulation using in-situ polymerization method according to Zhu et al.'s work <sup>71</sup>. A pre-polymer was first synthesized by mixing melamine and formalin solution in the distilled water (formation of MF shell). Then,  $C_{12}$  was dispersed in aqueous sodium hydroxide solution to form an emulsion (O/W emulsion). The pre-polymer was added to the  $C_{12}$  emulsion by droplets to achieve polymerization. Finally, the microcapsules were rinsed and air-dried at room temperature. In this work, it was indicated that the average capsule diameters were strongly affected by the stirring rates. The size range is from 330nm to 15.69µm.

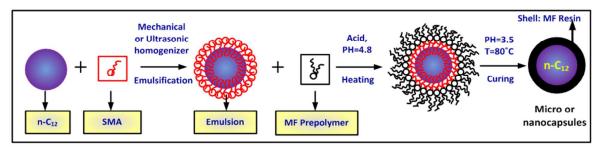


Figure 7 Schematic of in-situ polymerization for the C<sub>12</sub> microencapsulation (redrawn based on Ref. <sup>71</sup>)

#### 3.2.2.2 Interfacial polymerization

- General processes <sup>97</sup>: (1) formation of the oil phase with PCM and hydrophobic monomers; (2) dissolve the hydrophilic monomers in the aqueous solution; (3) microcapsules formation the by adding hydrophilic groups in the form of droplets into oil phase; (4) microcapsules collection by filtering, washing and drying from the emulsion. This method is typically used for organic shell materials like PU and PUT.
- A typical example: Figure 8 shows the schematic of microencapsulation using interfacial polymerization method according to the work of Zhang and Wang <sup>97</sup>. Firstly, the mixed oil solution consisting of C<sub>18</sub> and TDI was dispersed in an aqueous solution to form an oil-in-water microemulsion (oil phase C<sub>18</sub>/TDI mixture). Then, the other requisite monomer, amine, was dropped into the emulsion and reacts with TDI. As a result, a urea-linked polymeric shell was formed at the oil-water interfaces. Finally, the resultant microcapsules were filtered, washed and dried. The particle size of the microcapsules was within a range of 3~12 μm.

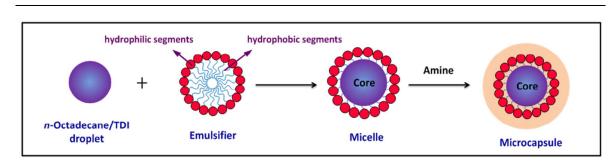


Figure 8 Schematic of interfacial polymerization for the  $C_{18}$  microencapsulation (redrawn based on Ref. <sup>97</sup>)

#### 3.2.2.3 Suspension polymerization

- General processes<sup>80</sup>: (1) PCM, monomers and initiators form the oil phase and suspend in the aqueous solution as discrete droplets (add surfactants); (2) initiators triggering the microcapsules polymerization from the oil phase (core materials); (3) separation of microcapsules from the emulsion. This method is typically used for organic shell materials like PMMA.
- A typical example: Figure 9 shows the schematic of microencapsulation using suspension polymerization method according to Ai et al.'s work <sup>80</sup>. The first step was emulsifying the oil phase into aqueous phase. Casein molecules as the mini-reactors act to stabilize the fine oil droplets through the polymerization period. Then, The C<sub>16</sub>, monomers and initiators formed the oil phase. The precipitation polymerization took place within the oil droplets after the temperature was elevated. Finally, phase separation of polymer occurred, resulting polymer particles precipitate and move to the interface of oil droplets. The size of the microcapsules was within a range of 3~15 µm.

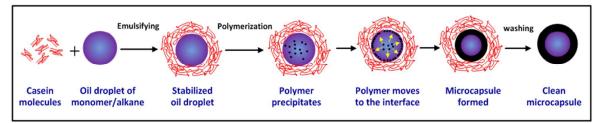


Figure 9 Schematic of suspension polymerization for the C<sub>16</sub> microencapsulation (redrawn based on Ref. <sup>80</sup>)

#### 3.2.2.4 Emulsion polymerization

- General processes<sup>219</sup>: (1) PCM and monomers form the oil phase and suspend in the aqueous solution as discrete droplets (add surfactants); (2) initiators are dissolved in the aqueous phase; (3) initiators triggering the microcapsules polymerization; (4) separation of microcapsules from the emulsion. This method is typically used for organic shell materials like PMMA and PS.
- A typical example: Figure 10 shows the schematic of microencapsulation using suspension polymerization method according to Macro's work <sup>219</sup>. The first step was preparing the wax and monomers emulsion in hot water with stirrer and detergents, then the initiators was dissolved into aqueous solution and polymer shell grew between the interphase of wax and water, finally, a highly cross linked polymer formed the dense shell on each droplet of wax. The size of the microcapsules was within a range of 2~20 µm.

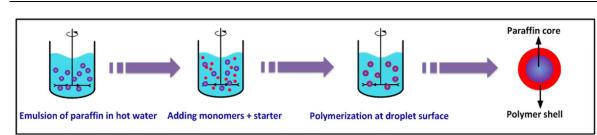


Figure 10 Schematic of emulsion polymerization for the paraffin microencapsulation (redrawn based on Ref. <sup>219</sup>) *3.2.3 physical-chemical methods* 

#### 3.2.3.1 Coacervation

- General processes<sup>220-221</sup>: (1) dispersion of the PCM in an aqueous solution containing the shell polymer;
   (2) deposition of the coating material (polymer) on the core material; (3) rigidizing of the coating material by thermal, cross linking or desolvation techniques to obtain microcapsules.
- A typical example: Figure 11 shows the schematic of microencapsulation using coacervation method according to the work of Uddin et al. and Fabien <sup>220-221</sup>. In Uddin's work, firstly, gelatine solution was prepared by dissolving in distilled water. Then, the solid paraffin was dispersed in the gelatine solution by gentle stirring and maintaining the temperature at a constant value. At this temperature, paraffin particles melted and, apparently, became coated with gelatine. Finally, the microencapsulated paraffin was hardened with cross-link agent and dehydrated by ethyl alcohol. Microencapsulated paraffin sizes are approximately 500 µm which are larger than the other synthesis methods.

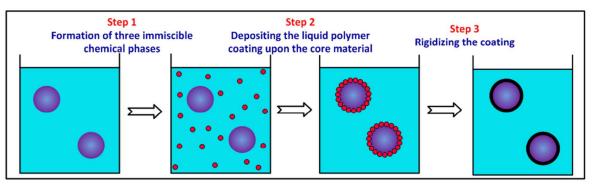
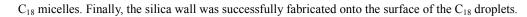


Figure 11 Schematic of coacervation method for the paraffin microencapsulation (redrawn based on Ref. <sup>220-221</sup>) **3.2.3.2 Sol-gel process** 

- General processes<sup>111</sup>: (1) formation of oil phase with PCM and surfactants (emulsifiers) (PCM O/W emulsion) (2) preparation of sol solution by dissolving the precursor compounds in water under an acidic environment; (3) microcapsules formation through condensation polymerization by adding sol solution into the PCM O/W emulsion drop by drop; (4) separation of microcapsules from the emulsion. This method is typically used for inorganic shell materials like silica and titanium oxide.
- A typical example: Figure 12 shows the schematic of microencapsulation using sol-gel method according to He et al.'s works <sup>111</sup>. The oily C<sub>18</sub> was first dispersed in an aqueous solution containing a nonionic surfactant (PEO-PPO-PEO) to form a stable O/W emulsion. Then, the silica sol was prepared by dissolving sodium silicate in water under an acidic or weakly alkaline circumstance. Afterwards, the silica sol was added into the O/W emulsion drop by drop, leading to the formation of silica gel surrounding the

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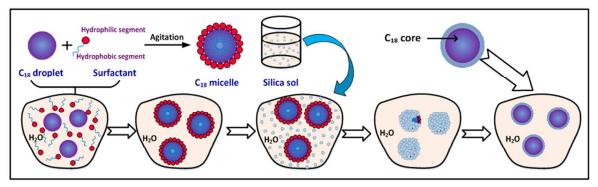


Figure 12 Schematic of sol-gel method for the C<sub>18</sub> microencapsulation (redrawn based on Ref.<sup>111</sup>)

#### 3.2.4 Other methods

Gao et al. <sup>153</sup> fabricated a microencapsulated  $C_{20}$  capsules through a self-assembly process, as shown in Figure 13. First, O/W emulsion containing  $C_{20}$  micelles was built first with the aid of surfactant. Then, CuSO<sub>4</sub> was added into the emulsion system, copper ions were attracted onto the surfaces of  $C_{20}$  micelles and form a self-assemble system with copper species at the oil-water interface. Next, a Cu(OH)<sub>2</sub> layer was generated surrounding the  $C_{20}$  micelles through precipitation reaction by adding a NaOH aqueous solution into this self-assemble system. The Cu(OH)<sub>2</sub> layer was further reduced with glucose reducing agent, Finally, a well-defined Cu<sub>2</sub>O shell encapsulating the  $C_{20}$  core was fabricated. This method actually has two key factors: the first is the selection of an appropriate surfactant template that can supply specific and local interactions among the core materials to attract precursors for self-assembly themselves, and the second one is the accurate control of a balance between the deposition and precipitation of precursors at the oil-water interface.

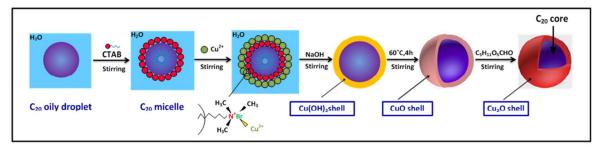


Figure 13 Schematic of self-assembly for the C<sub>20</sub> microencapsulation (redrawn based on Ref.<sup>153</sup>)

#### 3.3 Characterization of microencapsulated C<sub>n</sub> and their blends

The  $C_n$  and their blends microcapsules should be characterized from three aspects including thermal, physical and chemical properties to examine their microencapsulation properties, determine their application ranges, and propose improvement methods of properties. The thermal, physical and chemical properties comprise several key sub-properties, respectively. In this sub-section, the method of characterization for each property is firstly described; the corresponding microencapsulation characteristics and their improvement methods are then elaborated with some typical examples.

#### 3.3.1 Thermal properties

#### 3.3.1.1 Phase change properties

The phase change properties of bulk PCM and MPCM are generally measured by differential scanning calorimetry (DSC) analysis. As shown in Figure. 14, DSC testing results are presented in the form of endothermic and exothermic curves with temperature variations during heating and cooling phases, respectively. By analyzing the curves, the key phase change properties can be obtained as follows:

 $T_{mo}$ : The melting onset temperature in endothermic curves;

 $T_{mp}$ : The melting peak temperature in endothermic curves;

 $\Delta H_m$ : The melting enthalpy in endothermic curves;

 $T_{co}$ : The crystallization onset temperature in exothermic curves;

 $T_{cp}$ : The crystallization peak temperature in exothermic curves;

 $\Delta H_c$ : The crystallization enthalpy in exothermic curves;

 $\Delta T_s$ : Supercooling degree, defined as  $T_{mp}$ - $T_{cp}$ .

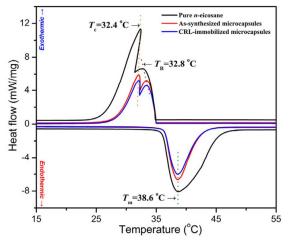


Figure 14 DSC thermograms of as-synthesized and CRL-immobilized microcapsules 151

The thermal conductance, geometric confinement or nucleation induction of shell results in the shift of the phase change temperature  $^{188-189}$ . The melting temperature of  $C_n$  in the microcapsules is generally similar to that of the bulk  $C_n$ . In contrast, the crystallization temperature of  $C_n$  in the microcapsules is significantly lowered compared to that of the bulk  $C_n$ . This means that  $C_n$  will experience severe supercooling when it is encapsulated in microcapsules, which is most likely owing to the lack of nuclei in such a tiny space  $^{212}$ . Supercooling results in that the latent heat is released at a lower temperature or in a wider temperature range, which is disadvantageous for the energy storage application. Therefore, the supercooling is still a major obstacle to the widespread application of

microencapsulated  $C_n$  and hence lots of efforts have been devoted to reduce the supercooling of  $C_n$  in microcapsules. Currently, there mainly exist two types of methods to eliminate or suppress the supercooling. One is to add nucleating agents into core to promote heterogeneous nucleation, such as paraffin or alcohols with high freezing point and solid nanoparticles. Another is to modify the shell composition and structure to mediate a homogeneous nucleation by shell-induced heterogeneous nucleation. Wu et al. <sup>119</sup> reported that adding around 8.3 wt% paraffin or 1-tetradecanol into core materials can suppress supercooling of microencapsulated C18. Similarly, Al-Shannaq et al. <sup>212</sup> selected 5wt% RT58 or 15 wt% 1-octadecanol as nucleating agents to decrease the supercooling of microencapsulated RT21 from 14°C to less than 5°C. Tang et al. 114 developed a novel microencapsulated C18 with ODMA-co-MAA copolymer as shell to realize low supercooling. The use of ODMA led to the formation of a number of small alkyl nanodomains on the inner wall of shell, which can act as nuclei to induce the heterogeneous nucleation of C18 in the microcapsules; thus the supercooling degree of microencapsulated C18 with the ODMA-co-MAA copolymer as shell is notably lower than that with MF as shell. Cao et al.<sup>222</sup> optimized the composition and structure of the adopted MF resin shell by adjusting ratio of melamine to formaldehyde, pH of pre-polymer, and pH of emulsion to achieve shell-induced nucleation of the triclinic and rotator phases and thus suppress the supercooling. Besides modified organic shell, inorganic shell also has a positive role in diminishment of supercooling. Tang et al.  $^{123}$  selected SiO<sub>2</sub> as shell to microencapsulating C<sub>18</sub> to realize extremely low supercooling, which is less than that of the bulk or pure C18. This is because that the microstructure with no cross-linking on its interior wall of the silica shell is helpful for the nucleation of  $C_{18}$ . The second method is generally more advantageous in the effective latent heat of the MPCM microcapsules, because the effective latent heat will be reduced by the relatively large amount of additive in the first method.

The latent heat of MPCM is lower than that of pure PCM because of the shell existing. In order to increase the latent heat of MPCM the thinner or lighter shells are required, which will cause more challenges in the synthesis process and material selection of shell. Tang et al. <sup>123</sup> confirmed that the dosage reduction of the raw materials used to synthesize shell can increase the latent heats of the MPCM decrease accordingly. Wan et al. <sup>189</sup> found that the latent heat of fusion increases with the increase in the percentage of pentaerythritol triacrylate (PETA) which was employed as cross-linking agents. They explained it by that a higher degree of cross-linking can lead to higher core/shell size ratio. When the content of PETA was increased from 4 wt% to 22 wt%, the latent heat of melting of the PCM microcapsules measured was increased from 87.9 J/g to 112.1 J/g. Compared those microcapsules containing C18 in Table 4, it can be seen that the microcapsules using SiO<sub>2</sub> as shell <sup>123</sup> has much higher latent heat than the others, and it thus has advantages in thermal energy storage.

## 3.3.1.2 Thermal conductivity

Currently no sufficient information on the measurement of thermal conductivity of single MPCM particle can be found in the literature. Although the thermal conductivity of MPCM was measured using laser flash apparatus (LFA, LINSEIS LFA1000) by Chai et al. <sup>148</sup>, an EKO HC-110 thermal conductivity meter by Yu et al. <sup>110</sup> or a Sweden Hot Disk thermal conductivity meter with 7577 probe by Jiang et al. <sup>199, 205</sup>, they did not specify how to test the thermal conductivity of a single microcapsule. Pressing massive microcapsules into a tablet is likely a feasible measurement method to approximately obtain the thermal conductivity of single microcapsule <sup>21, 198, 206</sup>. The thermal conductivity of single microcapsule can be theoretically estimated based on the composite sphere approach as follows <sup>223-224</sup>:

$$\frac{1}{\lambda_p d_p} = \frac{1}{\lambda_c d_c} + \frac{d_p - d_c}{\lambda_w d_p d_c}$$
(1)

where  $\lambda_p$ ,  $\lambda_c$  and  $\lambda_w$  are the thermal conductivities of the single MPCM particle, the core material and the shell material, respectively;  $d_p$  and  $d_c$  are the diameter of the single MPCM particle and core, respectively.

One of the aims of  $C_n$  or paraffin microencapsulation is to increase the heat transfer surface to overcome their low conductivities. However, the MPCMs using organic polymers as shells still exhibit poor heat transfer property due to its low thermal conductivities of the organic shells. The poor heat transfer property results in a low efficiency of thermal storage and release, which has been regarded as a dominating drawback in energy storage application <sup>91</sup>. Fast heat transfer in MPCMs is required to enable a prompt response during the charging and discharging processes of the thermal energy. Therefore the thermal conductivity of MPCMs needs to be enhanced. Several methods of elevating the thermal conductivity of MPCMs have been proposed by researchers recently. One is to modify the shell with inorganic nanoparticles, including Fe<sub>3</sub>O<sub>4</sub> <sup>178</sup>, Al<sub>2</sub>O<sub>3</sub> <sup>199</sup>, graphene <sup>87, 191</sup>, CNT <sup>132</sup>, BN/TiO<sub>2</sub> <sup>192</sup>. Jiang <sup>199</sup> employed emulsion polymerization to embed Al2O3 nanoparticles into P(MMA-co-MA) shell, which improved the thermal conductivity of the paraffin microcapsules. They reported that the thermal conductivity of the paraffin microcapsules would increase from 0.2442 W/(m·K) to 0.3816 W/(m·K) when the mass ratio of Al<sub>2</sub>O<sub>3</sub> nanoparticles was increased from 0 to 38%. Another is to directly adopt inorganic materials as shells, such as TiO<sub>2</sub><sup>138, 148</sup>, SiO<sub>2</sub><sup>75, 111</sup>, CaCO<sub>3</sub><sup>76, 110</sup>,  $ZrO_2$ <sup>152</sup> and  $Cu_2O$ <sup>153</sup>. Wang's research group <sup>148</sup> used TiO<sub>2</sub> as shell to microencapsulate C<sub>20</sub> through sol–gel method to increase the thermal conductivity from 0.161 W/(m·K) to 0.749 W/(m·K). They also employed  $ZrO_2^{-152}$  and  $Cu_2O_2^{-152}$  $^{153}$  to microencapsulate C<sub>20</sub> to obtained higher thermal conductivity of the microcapsules without decreasing thermal storage capacity. It should be noted that although the thermal conductivity of MPCM is further increased with the increase in the mass ratio of inorganic nanoparticles or shell, the latent heat of phase change correspondingly decreased. A compromise should be made between the two aspects of energy storage performances.

## 3.3.1.3 Thermal stability

Thermal stability of MPCM includes two aspects, which are thermal degradation behavior and thermal reliability. The thermal degradation behavior indicates the temperatre limit of stable operation of MCPM, which is investigated by thermogravimetric analysis (TGA) under continueously heating <sup>166, 208</sup>. Jiang et al. <sup>145</sup> conducted the thermal degradation test for  $C_{20}$  microcapsules with Fe<sub>3</sub>O<sub>4</sub>/SiO<sub>2</sub> shell using TGA. The TGA curves for pure  $C_{20}$  and  $C_{20}$  microcapsules with differnet core/shell mass ratios are shown in Figure 15. This figure shows a typical one-step thermal degradation behavior for all smaples presents and a remarkable increment in thermal degradation temperature (at which the sample undergoes the most rapid mass loss) after  $C_{20}$  was microencapsulated. They stated that the compact Fe<sub>3</sub>O<sub>4</sub>/SiO<sub>2</sub> hybrid shell hindered the decomposition of microencapsulated  $C_{20}$  and thus improved thermal degradation temperature of the microcapsules. Zhang et al. <sup>188</sup> reported that a two-step thermal degradation process was observed for a GO-modified MF/paraffin microcapsule. They pointed out that the first step thermal degradation temperature of first step due to formation of less defect shell. The increase in thermal degradation temperature ensures the stable work of MPCM at a higher temperature far above the melting point of core PCM.

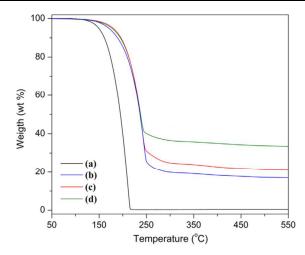


Figure 15 TGA curves of (a) pure  $C_{20}$  and the  $Fe_3O_4/SiO_2$  hybrid shell microencapsulated  $C_{20}$  synthesiezed with core/shell mass ratios of (b) 7/3, (c) 5/5 and (d) 4/6<sup>145</sup>

The thermal reliability enables long-term serving durability of MPCMs, which is analyzed by DSC based on a large number of repeated thermal cycles of alternate melting and solidification <sup>116, 121</sup>. If the properties of phase change exhibit tiny or even no change after sufficient thermal cycles, the MPCM is regarded as thermally reliable. Chai et al. <sup>148</sup>performed thermal reliability tests of a representative  $C_{20}$  microcapsule sample with TiO<sub>2</sub> shell using DSC. Figure 16 shows the multiple DSC curves of over 100 thermal cycles of the microcapsule. This figure indicates that their synthesized microcapsules can maintain stable phase change properties for a long-term utility period. Fourier transform infrared (FT-IR) spectroscopy can also be used to exam the thermal reliability through testing chemical composition as an auxiliary means <sup>162</sup>. Sarı et al. <sup>91</sup>demonstrated the FT-IR spectra of PMMA/C<sub>17</sub> microcapsules before and after thermal cycling, which are shown in Figure 17. This figure shows that the frequencies of characteristic peaks have little change after 5000 thermal cycles, which means no effects of thermal cycling. Therefore, their synthesized microcapsules are thermally stable from the viewpoint of chemical structure.

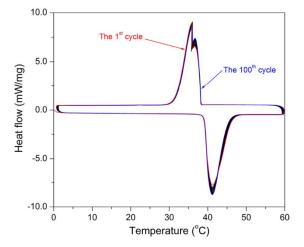


Figure 16 DSC curves over 100 cycles for the  $C_{20}$  microcapsule with TiO<sub>2</sub> shell <sup>148</sup>

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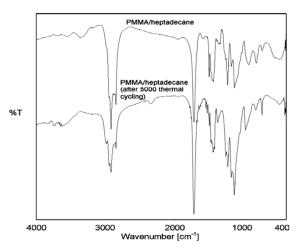


Figure 17 FT-IR Spectra of PMMA/C<sub>17</sub> microcapsules before and after thermal cycling <sup>91</sup>

#### 3.3.2 Physical properties

## 3.3.2.1 Microcapsule size distribution

The sizes of PCM microcapsules are crucial to their thermal storage performance, especially for MPCM slurry application <sup>160, 223-224</sup>. The particle size distribution (PSD) of microcapsules can be measured using a diameter distribution analyzer <sup>107</sup> or a scanning electron microscope (SEM) <sup>90, 123</sup>. The PSD is affected by many factors, such as viscosity of materials, shell compositions, process parameters and synthesis methods. de Cortazar et al. <sup>173</sup> pointed out that the average particle size increased with paraffin/MMA ratio and explained it by taking into account viscosity of the system, which affected the onset of acoustic cavitation and thus droplet size. Lashgari et al. <sup>90</sup> reported that the average sizes of C<sub>16</sub> microcapsules using PMMA and BA-co-MMA as shells were 140  $\mu$ m and 155  $\mu$ m, respectively. De Castro et al. <sup>160</sup> found that the increase of the homogenization speed resulted in a smaller average particle size and a narrow size distribution of C<sub>22</sub>/PU microcapsules through interfacial polymerization. When the homogenization speed increased from 6000 rpm to 20000 rpm, the average particle size decreased from 10  $\mu$ m to 2  $\mu$ m. Su et al. <sup>21</sup> summarized the statistics results of PSD of capsules prepared via various synthesis methods, which indicated that the size distribution range is notably different from each other for the various methods.

#### 3.3.2.2 Efficiencies

Two types of efficiencies of microencapsulation were adopted in the literatures: encapsulation efficiency and energy storage efficiency. Generally, these two efficiencies were mainly affected by the ratio of core/shell, the mass of emulsifier and cross-link agent, as well as the synthesis methods.

The encapsulation and the energy storage efficiency are calculated using Eq. (2) and Eq.(3), where  $\Delta H_{m,MPCM}$ and  $\Delta H_{c,MPCM}$  are the melting and crystallization enthalpies of the PCM microcapsule <sup>97,99</sup>,  $\Delta H_{m,PCM}$  and  $\Delta H_{c,PCM}$  are the crystallization enthalpies of pure PCM. The latent heat is measured by differential scanning calorimeter (DSC).

Encapsulation efficiency <sup>99</sup>

$$E_{en} = \frac{\Delta H_{m,\text{MPCM}}}{\Delta H_{m,\text{PCM}}} \times 100\%$$
<sup>(2)</sup>

• Energy storage efficiency <sup>97</sup>

$$E_{es} = \frac{\Delta H_{m,\text{MPCM}} + \Delta H_{c,\text{MPCM}}}{\Delta H_{m,\text{PCM}} + \Delta H_{c,\text{PCM}}} \times 100\%$$
(3)

Basically, these two efficiencies represent the ratio of core PCM to shell materials. In the above Tables 4-7, the values of  $E_{en}$  were listed if only  $E_{en}$  or both  $E_{en}$  and  $E_{es}$  are available in the literatures. Otherwise, the values of  $E_{es}$  were listed but marked 'es' as a superscript in front of the data.

## 3.3.2.3 Microcapsule morphologies

The morphologies of the fabricated microcapsules can be examined by a SEM after coating a gold layer with a thickness of several nanometres<sup>183</sup>. The key morphologies which need to be confirmed are as follows: (a) whether agglomeration of microcapsules exists; (b) whether the shape of microcapsules is spherical; and (c) whether cracks, dents or defects exist on shell surface. The morphologies of microcapsules are markedly affected by types of emulsifiers, types of cross-linking agents and shell compositions. Su et al. <sup>190</sup> compared the morphologies of paraffin microcapsules with MF shell under two different types of emulsifiers. The emulsifier with higher value of hydrophilic-lipophilic balance (HLB) led to the agglomeration of microcapsules as shown in Figure 18(a), while the emulsifier with a lower HLB value prevented the agglomeration but resulted in more obvious dents on the shell surface as shown in Figure 18(b). Qiu et al. <sup>109</sup> analysed the effects of cross-linking agents on the morphologies of C18 microcapsules with PBA shell. They found that the dimples on the surface of the microcapsules using divinylbenzene (DVB) as cross-linking agent were less in number and larger in size compared with those using pentaerythritol triacrylate (PETA) as cross-linking agent as shown in Figure 19. Meanwhile, DVB as cross-linking agent largely improved the degree of adhesions of microcapsules compared to PETA. Lashgari et al. 90 reported that the C<sub>16</sub> microcapsules with PMMA shell were wrinkled although they have spherical profile as shown in Figure 20(a), while the microcapsules with BA-co-MMA polymer shell exhibited smooth surface and absence of wrinkles as shown in Figure 20(b). It was explained by that BA-co-MMA offers greater flexibility and lower interfacial tension with C<sub>16</sub> compared to MMA.

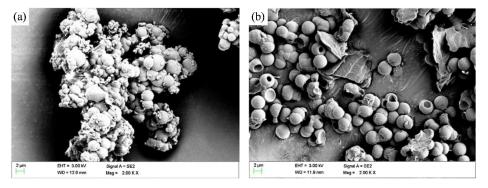


Figure 18 SEM images of paraffin microcapsules under different emulsifiers with (a) high HLB and (b) low HLB

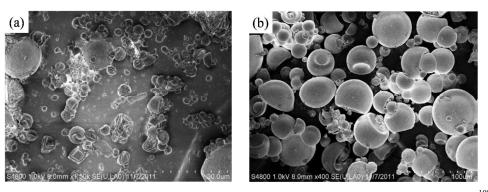


Figure 19 SEM images of  $C_{18}$  microcapsules with (a) PETA and (b) DVB as cross-linking agents <sup>109</sup>

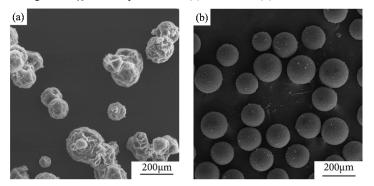


Figure 20 SEM images of  $C_{16}$  microcapsules with (a) PMMA shell and (b) BA-co-MMA polymer shell <sup>90</sup> 3.3.2.4 Mechanical strength

The mechanical integrity of microcapsules is the basis of successful application of microcapsules in thermal energy storage, however the PCM microcapsules are confronted with the possibility of rupture during repeated thermal charging-discharging cycling, especially in its usage as slurries because of repeatedly pumping <sup>23</sup>. The mechanical strength of microcapsules thus needs to be carefully considered. The mechanical properties of microcapsules can be analysed by atomic force microscopy (AFM) <sup>203, 225-226</sup>. Borreguero et al. <sup>203</sup> applied AFM probe to exert forces on RT27 microcapsules with LDPE-EVA copolymer shell and they found that the force required to produce the same deformation of microcapsules increased by approximately 83% when 2 wt% of carbon nanofibers was added into microcapsules. Giro-Paloma et al. 225 used AFM in nanoindentation mode to determine the maximum force that paraffin microcapsules with acrylate shell can afford before breakage at different temperatures. Values of effective modulus were calculated for microcapsule agglomerates of 150 µm in diameter and single microcapsule of 6 µm according to the measured results. They pointed out that values of effective Young's modulus depended on the temperature and particle size. The agglomerates presented higher effective modulus than single microcapsule and the effective Young's modulus of single microcapsule showed a remarkable decrease at 80 °C because this temperature is close to the acrylate shell glass transition temperature. They also compared the mechanical properties between paraffin microcapsules with acrylate and MF shells <sup>226</sup>. It was concluded that the acrylate shell exhibited better breakage resistance compared to MF shell, because the MF shell prepared using in-situ polymerisation tended to be more brittle and pressure-sensitive. When the temperature rose to make the paraffin become liquid state, the mechanical properties would be notably lowered.

#### 3.3.2.5 Leakage of PCM

When the shell of PCM microcapsules possesses porous structure or cracks, leaking of liquid core PCM occurs.

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And once leakage paths are formed, the core PCM will constantly leak until the PCM is depleted. Leakage rates  $(L_r)$  at different times are usually used to indicate the leakage-prevention performance of microcapsule structure. A typical measuring procedure of  $L_r$  is as follows <sup>188</sup>: A certain mass  $M_0$  of dried microcapsules are individually put on filter papers. Then they are moved into an oven in which the temperature is fixed over the melting point of core PCM. The samples need to be taken out from the oven periodically at a prescribed time interval to weigh their mass which are indicated by  $M_t$ . The leakage rate is defined as

$$L_r(\%) = \frac{M_0 - M_t}{M_0} \times 100 \tag{4}$$

Although the increase of shell thickness can enhance leakage-prevention performance, it will weaken the encapsulation ratio simultaneously. Zhang et al. <sup>188</sup> proposed a GO-modified paraffin microcapsules with MF shell to enhance leakage-prevention performance with high encapsulation ratio. They stated that the added GO nanosheets were situated at the interface between the core and the shell and successfully served as a protective screen to prevent leakage of paraffin, as shown in Figure 21. Their measured results manifested that this structure of dual protective screens comprising GO layer and MF shell slowed down the leakage of paraffin and thus could lengthen the service life of paraffin microcapsules. Al-Shannaq et al. <sup>212</sup> used mass loss analysis to test the permeability of core RT21 through the PMMA shell of microcapsules and compare the leakage rates of core RT21 from microcapsules with and without nucleating agent, which was used to suppress supercooling. Their testing results indicated that the leakage rate of RT21 from the microcapsules significantly decreased after RT58 was added and the increase of RT58 concentration resulted in smaller leakage. They explained it by that the RT58 may form a protective layer between the core RT21 and the PMMA shell. This suggests that the nucleating agent RT58 does not only diminish supercooling, but could also enhance leakage-prevention performance of the RT21 microcapsules with PMMA shell.

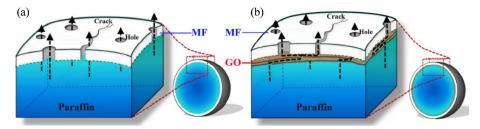


Figure 21 Schematic view for possible permeation through the shells of (a) MEPCM-00 and (b) MEPCMs with GO.

#### 3.3.3 Chemical properties

#### 3.3.3.1 Fourier transformation infrared spectroscopy (FT-IR)

The Fourier transformation infrared spectroscopy (FT-IR) was used to identify the functional groups in organic polymers, inorganic compounds and chemical characterization of the MPCMs. Almost all of the investigations listed in Table 4-7 had performed this analysis.

Normally, the chemical compositions of PCMs before and after microencapsulation were examined by FT-IR. The obtained spectra were compared to determine whether a change occurred in chemical structures during the microencapsulation process. For example, P(MMA-co-MA) shell with nano-Al<sub>2</sub>O<sub>3</sub> inlay microcapsules containing paraffin as core was synthesized through emulsion polymerization <sup>199</sup>. The FTIR spectra of nano-Al<sub>2</sub>O<sub>3</sub>, paraffin and P(MMA-co-MA) shell as well as microencapsulated paraffin modified with different percentages of nano-Al<sub>2</sub>O<sub>3</sub>

were shown in Figure 22. The results confirmed the successful encapsulation of paraffin within the P(MMA-co-MA) shell with no chemical interaction, and the paraffin microcapsules had been successfully modified with nano-Al<sub>2</sub>O3 as well.

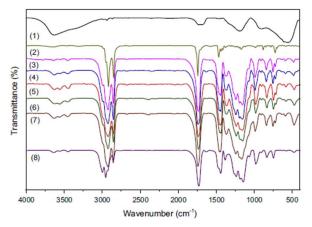


Figure 22 The FTIR spectra of nano-Al<sub>2</sub>O<sub>3</sub>, paraffin, copolymer shell and microcapsules modified with different amount of nano-Al<sub>2</sub>O<sub>3</sub>: (1) nano-Al<sub>2</sub>O<sub>3</sub>, (2) paraffin, (3) 0%, (4) 16%, (5) 27%, (6) 33%, (7) 38%, and (8) P(MMA-co-MA)<sup>199</sup>

## 3.3.3.2 X-ray diffraction (XRD)

The X-ray diffraction was used to determine the crystalline structures of microcapsules, which was typically suitable for the inorganic shell materials. For example, Zhang et al. <sup>155</sup> synthesized the microcapsules based on  $C_{20}$  core and silver/silica double-layered shell through interfacial polymerization. The XRD measurement was performed to investigate the crystalline structure of the silver/silica double-layered microcapsules, and the diffraction patterns are illustrated in Figure 23. The results suggested the sliver layer on the microcapsule surface retained good crystallinity and only an amorphous silica shell was fabricated onto the  $C_{20}$  core.

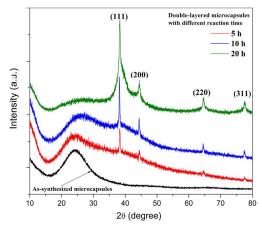


Figure 23 XRD patterns of the as-synthesized microcapsules and the silver/silica double-layered microcapsules obtained at different reaction time

#### 3.4 Summaries and discussions

When  $C_n$  and their blends microcapsules are prepared, the characterization of these microcapsules are required to examine their microencapsulation properties, in order to further determine their application ranges and propose improvement methods of their properties. The characterization is generally conducted from three aspects including

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thermal, physical and chemical properties to comprehensively evaluate the microcapsules. Multiple testing technologies such as DSC, LFA, TGA, SEM, AFM, FT-IR and XRD are used to explore these properties.

The main thermal properties are phase change temperature, latent heat, thermal conductivity and thermal stability. After PCM is microencapsulated, the shift of the phase change temperature occurs. Generally, the melting temperature slightly changes while the freezing temperature is notably decreased. The supercooling thus becomes a key barrier to the widespread application of microencapsulated  $C_n$ . In the literature, some methods to diminish or suppress the supercooling have been proposed, which can be classified into two sorts. One is to add nucleating agents into core to promote heterogeneous nucleation and another is to modify the composition and structure of shell to enable shell-induced heterogeneous nucleation. The effective latent heat in the first method will be reduced by the relatively large amount of additive and thus the second method is basically more advantageous from this point of view. It is inevitable that the latent heat decreases after microencapsulation of PCM because of shell existing. Utilization of the thinner or lighter shells can increase the latent heat of PCM microcapsules, but could cause more challenges in the synthesis process and material selection of shell. Types and dosage of shell materials and cross-linking agents should be precisely tailored to obtain the thinner or lighter shells. Due to its low thermal conductivities of the organic polymer shells, the PCM microcapsules with organic shells exhibit poor heat transfer property. The thermal conductivity of PCM microcapsules needs to be enhanced to enable a prompt response during the charging and discharging processes of thermal energy. The methods of elevating the thermal conductivity of PCM microcapsules proposed in the literature can also be classified two categories. One is to modify the organic shell using inorganic nanoparticles, such as Fe<sub>3</sub>O<sub>4</sub>, Al<sub>2</sub>O<sub>3</sub>, graphene, CNT, BN/TiO<sub>2</sub>. Another is to directly employ inorganic shells, such as TiO<sub>2</sub>, SiO<sub>2</sub>, CaCO<sub>3</sub>, ZrO<sub>2</sub> and Cu<sub>2</sub>O. It should be noted that a compromise should be made between the thermal conductivity and the latent heat. Thermal stability of PCM microcapsules includes thermal degradation behavior and thermal reliability. High thermal degradation temperature ensures the stable work of PCM microcapsules at a high temperature far above the melting point of core PCM and good thermal reliability enables long-term serving durability of PCM microcapsules. Suitable shell materials or more perfect shell structure is helpful for elevating thermal degradation temperature and achieving good thermal reliability.

The primary physical properties are microcapsule size distribution, efficiencies, microcapsule morphologies, mechanical strength, and leakage-prevention of PCM. Various microcapsule size distributions can be obtained by adjusting mass ratios of materials, shell compositions, process parameters and synthetic methods. The encapsulation efficiency and energy storage efficiency can be used to indicate the room for improvement in latent heat of PCM microcapsules. All the methods to elevate latent heat can be employed to augment the encapsulation efficiency and energy storage efficiency. The ideal morphologies of microcapsules should be spherical shape without agglomeration and without cracks, dents or defects on shell surface. Better morphologies of microcapsules can be achieved by adjusting types of emulsifiers, types of cross-linking agents and shell compositions. Excellent mechanical strength is required to maintain the integrity of microcapsules during repeated thermal charging-discharging cycling or repeatedly pumping in its usage as slurries. Additives like carbon nanofibers and adoption of shell materials with high flexibility and with glass transition temperature far away from phase change temperature is beneficial to the increase of mechanical strength. It should be noted that the mechanical strength will be decreased as PCM becomes liquid state. The leakage-prevention performance is closely related to the long term usability. A structure of dual protective screens formed by shell and additives like GO nanosheets can effectively slow down the leakage of PCM and thus lengthen the service life of PCM microcapsules.

The chemical properties are mainly chemical compositions or crystalline structures of PCM microcapsules. They can be used to indicate the chemical compatibility between core, shell and additives, and to check whether the shell has been successfully modified by nanoparticles or whether the multilayer shell has been successfully synthesized. They also can be used to aid the investigation of thermal reliability of PCM microcapsules.

Although lots of studies have been devoted to improvement of the properties of PCM microcapsules, there are still some key issues which need to be addressed: (1) Most of those prepared PCM microcapsules listed in Table 4 still have a high supercooling degree and low thermal conductivity. More effective methods are required to eliminate supercooling and increase thermal conductivity in the case of maintaining high latent heat for various PCM microcapsules. (2) The service life of PCM microcapsules need to be evaluated more precisely and be further prolonged. Thus more effective methods are required to prevent PCM in microcapsules from leaking. (3) MPCM slurry is a dominating application of PCM microcapsules, which undergoes repeatedly pumping in actual utilization. Therefore, the observed of morphologies and the measurements of mechanical strength of PCM microcapsules should be performed in repeatedly pumping conditions. (4) The microencapsulated pure  $C_n$  which can be found in the literature only refer to C12 to C32 as shown in Table 4, whereas the Cn with lower melting points such as C8~C11 and higher melting points such as C33~C50 as shown in Figure 1 have not yet been involved in the microencapsulation study or application. Table 2 and Table 3 summarize lots of binary mixtures and ternary mixtures of  $C_n$ , whose melting points are different from the corresponding pure  $C_n$ . These mixtures thus enrich the melting points of optional PCM and enable more precise solution of melting points. However, it can be found that most of these mixtures have not yet involved in the microencapsulation study or application by comparison with Table 6. Therefore, more studies should be conducted on microencapsulation of those Cn and their mixtures mentioned above.

#### **4** Applications

### 4.1 Slurry

When the PCM microcapsules are dispersed into a carrier fluid (e.g. water) at the assistance of an appropriate amount of surfactant, MPCM slurry is formed. As they combine the latent heat of the PCM microcapsules and sensible heats of both the liquid and PCM microcapsules, MPCM slurry has high thermal storage capacity and strong heat transfer capacity. MPCM slurry is a multifunctional solid/liquid mixture, which can serve as both heat transfer fluids (HTFs) and thermal storage medium (TSM). MPCM slurry has various potential applications, such as cooling storage <sup>227</sup>, solar thermal collector and storage <sup>191, 228</sup> and microchannel heat exchangers <sup>229</sup>. There are different levels of the scientific and technological issues which need to be addressed before realistic applications of MPCM slurry as HTFs and TSM.

At a material level, the thermophysical properties of MPCM slurry need to be clearly identified and predicted, such as thermal conductivity, specific heat, viscosity and density. Zhang et al. <sup>223</sup> studied the thermal and rheological properties of a series of MPCM slurries at low concentration of microcapsules. They measured the thermal conductivity and specific heat of MPCM slurry by the Hot Disk and the viscosity by a rheometer. Their study indicated that the predicted values of thermal conductivity and specific heat using those models adopted by Goel et al. <sup>230</sup> agreed well with the experimental data. The models for predicting the thermal and rheological properties of MPCM slurries are summarized and analyzed by Chen et al. <sup>231</sup>. These models have been widely employed as the basis of the experimental or numerical studies on heat transfer performance of MPCM slurries <sup>224, 232-233</sup>. There are also some studies devoted to the thermal performance improvement of MPCM slurries or development of novel PMCM slurries with excellent performances. Liu et al. <sup>191</sup> dispersed the paraffin@MF/graphite microcapsules into an ionic liquid to form a novel HTF. They found that this new kind of HTF exhibited an enhancement of 13% in thermal conductivity as the mass fraction of paraffin@MF/graphite was 20% and an increase by double in thermal storage capacity as compared to the base fluid.

At a component level, the heat transfer and hydrodynamic properties of MPCM slurry in ducts or channels and the thermal storage characteristics in a tank or container need to be figured out. A review on studies of heat transfer and hydrodynamic properties of MPCM slurry was conducted by Chen et al. <sup>231</sup>. They pointed out that wall temperature, heat transfer coefficient, Nusselt number are uesed to reflect the heat transfer properties of MPCM slurry indirectly or directly, while pressure drop and pumping power are used to estimate the degree of hydrodynamic challenge caused by high viscosity of MPCM slurry. Qiu et al. 234 reviewed the heat ransfer enhancement mechanism of MPCM slurry, which consists of microconvection caused by microencapsules, migration of microcapsules within the boudnary layer, and phase change heat latent. They also collocated and evluated the parameters that have impact on the heat transfer properties of MPCM slurry under the condition of laminar and turbulent flow, mainly including concentration of microcapslues, size of microcapsules, Stephan number. Peclet number. Revnolds number as well as Prandtl number. Song et al.<sup>235</sup> carried out experimental studies on laminar heat transfer of MPCM slurry using low-melting-point liqud metal as a carrier fluid. They reported that the heat transfer coefficient increases with increasing volume concentration of microcapsules and Reynolds number. Kong et al. <sup>236</sup> conducted pressure drop and heat transfer experiments for MPCM slurries in a helically coiled tube under turbulent flow conditions. They found that a helically coiled tube was more suitable than a straight tube for convection heat transfer of MPCM slurry, although the heat transfer enhancement was restricted by high viscosity.

Zhang et al. <sup>237</sup> compared the thermal storage characterisites of MPCM slurry storage device (coil-in-tank) and stratified water storage tank (SWST). They observed that although the thermal storage capacity of MPCM slurry was much higher than that of water, the overall charging/dischanging rates of the slurry storage device were much lower than the idealized SWST, implying that an optimized design for MPCM slurry thermal storage device was further required.

At a system level, the compatibility of selected MPCM slurry with a heat exchange system or thermal energy system and the integrated system performnce should be carefully considered. Zhang et al. <sup>227</sup> experimentally investigated the phase transition of MPCM slurry running in a thermal storage test system. They found that the extraction of latent heat of MPCM slurry was not entirely complete due to supercooling in a practical air conditioning system integrated with thermal storage. Therefore supercooling would lower the partical storage capacity of MPCM slurry at a limited cooling temperature or the efficiency of a cooling storage system. Qiu et al. <sup>238</sup> conducted an experimental study concerning the overall performance of a novel PV/T thermal and power system ultilizing MPCM slurry. It was presented that the effects of various solar radiations, Reynolds numbers and concentrations of microcapsules on the performances of the PV/T system. At their recommended operational conditions, the net overall solar efficiencies of the system could achieve up to 80.8–83.9%. Kong et al. <sup>239</sup> performed field evaluation of ground source heat pump systems (GSHP) employing MPCM slurries as working fluids. They reported that the performance coefficient of the GSHP system was elevated by up to 4.9% due to higher heat capacity of MPCM slurries and progressive cavity pumps were more beneficial to durability of MPCM slurries than centrifugal pumps.

#### 4.2 Buildings

For the building applications, MPCMs are always embedded into concrete mixes, cement mortar, wallboards, gypsum plasters, sandwich panels, slabs, among others, which act to increase the thermal inertia for the same mass of buildings<sup>20</sup>. Actually, the concrete is one of the most useful materials in buildings, and most of researchers are focused on the embedment of MPCMs into concrete to enhance the thermal and acoustic insulation of walls in recent years. However, from an economic point of view, only the lower cost of the synthesized MPCMs has potential for a pilot application.

Cabeza et al. <sup>240</sup> studied a new concrete with paraffin microcapsules on thermal aspects. They found that the energy storage in the walls containing paraffin microcapsules were contributed to an improved thermal inertia and smoother fluctuations of temperature, which demonstrated a commendable opportunity in energy saving for buildings. Giro-Paloma et al. <sup>201</sup> synthesized the microencapsulated RT21, and tested their mechanical properties like elastic modulus, load at maximum displacement, displacement at maximum load by nano-indentation technique. In addition to this, an important parameter for considering use in building, the release of volatile organic compounds (VOCs), were studied. The results indicated that the RT21 microcapsules had better mechanical resistance and stiffness, and showed better stability with less short-term emission of VOCs as well. Aguayo et al. <sup>241</sup> proposed a new application of paraffin microcapsules in infrastructural concrete for mitigating early-age cracking and freeze-and-thaw induced damage. Figure 24 depicted the microstructure of cement pastes incorporating MPCMs. The results ascertained that the compressive strength of cement mortars with MPCMs was noted to be strongly dependent on the encapsulation properties. Cao et al. <sup>242</sup> fabricated the concretes by mixing the microencapsulated RT27 into Portland cement concrete (PCC) and geopolymer concrete (GPC), it was found that the thermal performance of concrete was improved significantly by adding the microcapsules, simultaneously, the significant

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loss in compressive strength was observed. However, the compressive strength still satisfied the mechanical European regulation for concrete applications. Sant et al. <sup>243-244</sup> synthesized the paraffin microcapsules, and applied them into cement-based composites. The results showed that the existence of MPCMs would not affect the drying shrinkage of cementitious composites, but in specific cases, it may slightly improve the durability of cementitious composites. Beyond that, the effect of MPCMs on the thermal deformation behavior was examined. The thermal deformation coefficient of microcapsules was similar to the shell materials. Finally, a rule was presented for designing the mortar composites with MPCMs which find use in built environment.

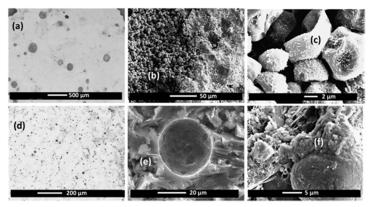


Figure 24 Microstructure of cement pastes incorporating MPCMs (a) PCM-M dispersed in cement paste, (b) breakage of PCM-M agglomerates into individual nodules in the cement paste, (c) cement hydration products on individual PCM-M nodules, (d) PCM-E dispersed in cement paste, (e) intact PCM-E microcapsule with hydration products around, and (f) dense reaction product around a PCM-E particle.<sup>241</sup>

#### 4.3 Textiles

Application of microencapsulated  $C_n$  and  $C_n$ 's blends in the textile industries was an old topic but had continually growing interest in recent years. Many studies have been done on microencapsulated  $C_n$  textiles materials.

As Nelson <sup>245</sup> reported, microcapsules can be coated on the surface of fabric or embedded within fiber. Sarier et al. <sup>81,94</sup> reported that the thermal enhancement of the fabrics could be achieved by incorporating  $C_{16}$ ,  $C_{18}$  and  $C_{19}$  microcapsules through coating. The energy storage capacities of the fabrics with microcapsules were found to be 2.5~4.5 times enhanced compared to the reference fabrics for particular temperature intervals. Later on, They indicated that the microencapsulated  $C_{16}$  and  $C_{18}$  with silver nanoparticles have very high thermal storage capacities, good durability, thermal stability and improved thermal conductivity, which are fairly appropriate for industrial applications in the field of textiles like sportswear and protective clothing, medical textiles and automotive and agriculture textiles <sup>88</sup>. Alay et al. <sup>82-83</sup> fabricated the  $C_{16}$  microcapsules and added to woven fabrics by cad-cure method. The results showed that the cotton, cotton/polyester, and microfiber polyester fabrics treated with microcapsules at the same concentration were capable of heat absorbing 4.95 J/g, 10.02 J/g, and 8.38 J/g, respectively. These discrepancies were attributed to the chemical compatibility of the fabric material and shell material of microcapsules. Moghadam et al. <sup>140-141</sup> prepared microencapsulated  $C_{19}$  for textiles application, and they found that that  $C_{19}$  microcapsules had a high energy-storing density (>137.83 J/g) and proper temperature of solid–liquid change (30~31°C), which were suitable for thermo-regulating textile. Most recently, Aksoy et al. <sup>89,133.</sup>

property of the textiles. SEM images demonstrated that the microcapsules could be distributed onto textile substrates homogeneously and durable to repeated washings (as shown in Figure 25). Meanwhile, thermo-regulating properties of the fabrics with microcapsules were proved via thermal history measurement results. Sun and Iqbal <sup>210</sup> synthesized the nanocapsules with  $C_{18}$  and  $C_{20}$  mixture as the core materials, and applied them on a cotton fabric via a pad-dry-cure process. The results indicated that nanocapsules have better durability on cotton fabric than MPCMs. The latent heat was decreasing faster for MPCM than nanoencapsulated PCM after washing.

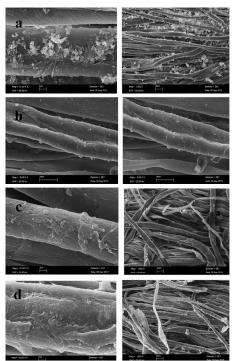


Figure 25 SEM images of the fabrics treated with P(MMA-co-MAA)/n-octadecane-3 microcapsule using Fixapret F-ECO resin (a) rubbing test applied, (b) 5 cycles washed, (c) 10 cycles washed, and (d) 20 cycles washed <sup>133</sup>

## 4.4 Foam

Integration of MPCMs into foams can improve their thermal performances, especially in thermal-insulating ability. Polyurethane, polystryrene foams with MPCMs can be applied in areas like automotive interiors, medical products, among others.

You et al. <sup>246</sup> fabricated the polyurethane foams containing  $C_{18}$  microcapsules. They found that the enthalpy of the foam increased with the increase of the content of MPCMs, and the maximum value of 12 J/g was achieved when the weight ratio of MPCMs/Polyurethane foam is 12.59%. Borreguero et al. <sup>247-248</sup> produced polyurethane foams incorporating different percentages of RT27 microcapsules. It was observed that the foam with 18 wt% of microcapsules can improve the TES capacity and hold the mechanical properties of the foam without fillers. 21 wt% of microcapsules resulted in a reduction in mechanical properties but with compressive strength and modulus higher than those exhibited by the foams containing 11 wt%. Then, 18 wt% of two types microcapsules (with different shell materials) were synthesized and added to the polyurethane foams <sup>249</sup>, and Figure 26 illustrated the SEM images of polyurethane foams containing 18 wt % of mSP-(PS-RT27). The results indicated that the microcapsules with highest particle size from PS and the agglomeration of the microcapsules from PMMA, led to the strut rupture, damaging the final mechanical performance. Three years later, they successfully produced rigid polyurethane foams

containing up to a 40 wt% content of mSD-(LDPE-EVA-RT27) <sup>250</sup>. These foams as temperature-regulating materials have a latent heat of 34.4 J/g which is higher than that reported value in literature for similar materials. Qiu et al. <sup>77, 118, 182, 196</sup> formed the polystyrene foams containing  $C_{14}$ ,  $C_{18}$  and paraffin microcapsules, and all the experimental results demonstrated that the foam treated by microcapsules had a better thermoregulatory property than the raw foam.

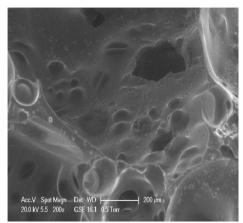


Figure 26 SEM images with 200× magnification of PU foams containing 18 wt % of mSP-(PS-RT27)<sup>249</sup>

#### **5** Conclusions and outlook

A main line from materials to their microcapsules ( $C_n$  and  $C_n$ 's blends to their microcapsules) as PCMs for TES systems was presented in this review. At first, PCM-interesting characteristics (transition temperatures and enthalpies) of  $C_n$ , multinary  $C_n$  and paraffins were listed, while the phase equilibrium evaluations of binary  $C_n$  were elaborated. Then, the microencapsulated  $C_n$  and  $C_n$ 's blends with respect to the synthesis methods, physical properties, thermal properties and chemical properties were presented and analyzed. Finally, the practical applications of microencapsulated  $C_n$  and their blends were reported.

In this review, the temperature range of the summarized  $C_n$  and  $C_n$ 's blends is from 211K to 366K (-62°C~93°C), while the temperature range of the summarized microencapsulated  $C_n$  and  $C_n$ 's blends is from 244K to 354K (-29°C ~81°C).

Review demonstrated that:

(1) The fixed melting points of  $C_n$  limit their practical applications; however, the  $C_n$ 's blends have proved the greater value as tunable PCMs because the temperature range are substantially enlarged and enriched. To employ  $C_n$ 's blends as PCM with robust performances, a narrow thermal window with no phase separation is the properties pursued. The phase change behaviors of  $C_n$ 's blends are close related to the phase equilibrium. Various types of phase change characteristics are elaborated through phase diagrams, and it is admitted that the eutectics and peritectics have been considered largely from a PCM selection perspective.

(2) The supercooling is prevalent for PCM microcapsules, which can be suppressed or eliminated by adding nucleating agents or modify the composition and structure of shell to induce heterogeneous nucleation. The thermal conductivity of PCM microcapsules can be elevated by modifying the organic shell using inorganic nanoparticles or directly employing inorganic shells. A compromise should be made between the thermal conductivity and the latent heat. Suitable shell materials or more perfect shell structure is helpful for elevating thermal degradation temperature. Better morphologies of microcapsules can be achieved by adjusting types of emulsifiers, types of cross-linking

agents and shell compositions. Suitable additives in shell or adoption of shell materials with high flexibility and glass transition temperature far away from phase change is beneficial to the increase of the mechanical strength. A structure of dual protective screens formed by shell and additives can effectively slow down the leakage of PCM and thus lengthen the service life of PCM microcapsules. The chemical compositions and crystalline structures of PCM microcapsules should be tested to certify the chemical compatibility between materials and success of shell modification or hybrid shell synthesis.

Outlook:

(1) For materials ( $C_n$  and  $C_n$ 's blends) level: Firstly, the published studies indicated that the binary system with a large discrepancy in chain length ( $\Delta n_c \ge 6$ ) still showed a eutectic characteristic, which does not respect the basic thermodynamic and miscible laws. Therefore, a huge amount of new combinations can be created, and deserve further investigations. Secondly, ternary systems are the neglected category in the PCM-context (few works published), but are promising for exploration in the future. Finally, a comprehensive phase equilibrium analysis is a fundamental way to indentify the phase change characteristics of  $C_n$ 's blends, but now it is still insufficient, the relative studies are worth improving.

(2) For microcapsules level: Firstly, more effective methods are required to eliminate supercooling and increase thermal conductivity in the case of maintaining high latent heat for various PCM microcapsules. Secondly, the service life of PCM microcapsules need to be evaluated more precisely and be further prolonged. Thirdly, the observed of morphologies and the measurements of mechanical strength of PCM microcapsules should be performed in repeatedly pumping conditions for slurry application. Finally, microencapsulation of more  $C_n$  and their mixtures which are not involved in the literature should be studies to enrich the optional range or values of melting points of PCM microcapsules. Except for the application areas in slurry, building, textiles and foam, the PCM microcapsules may also have the potential to be applied in solar air heater, refrigeration, liquid air thermal energy storage systems, among others.

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